



**Plant History**

Innovations and Future Trends





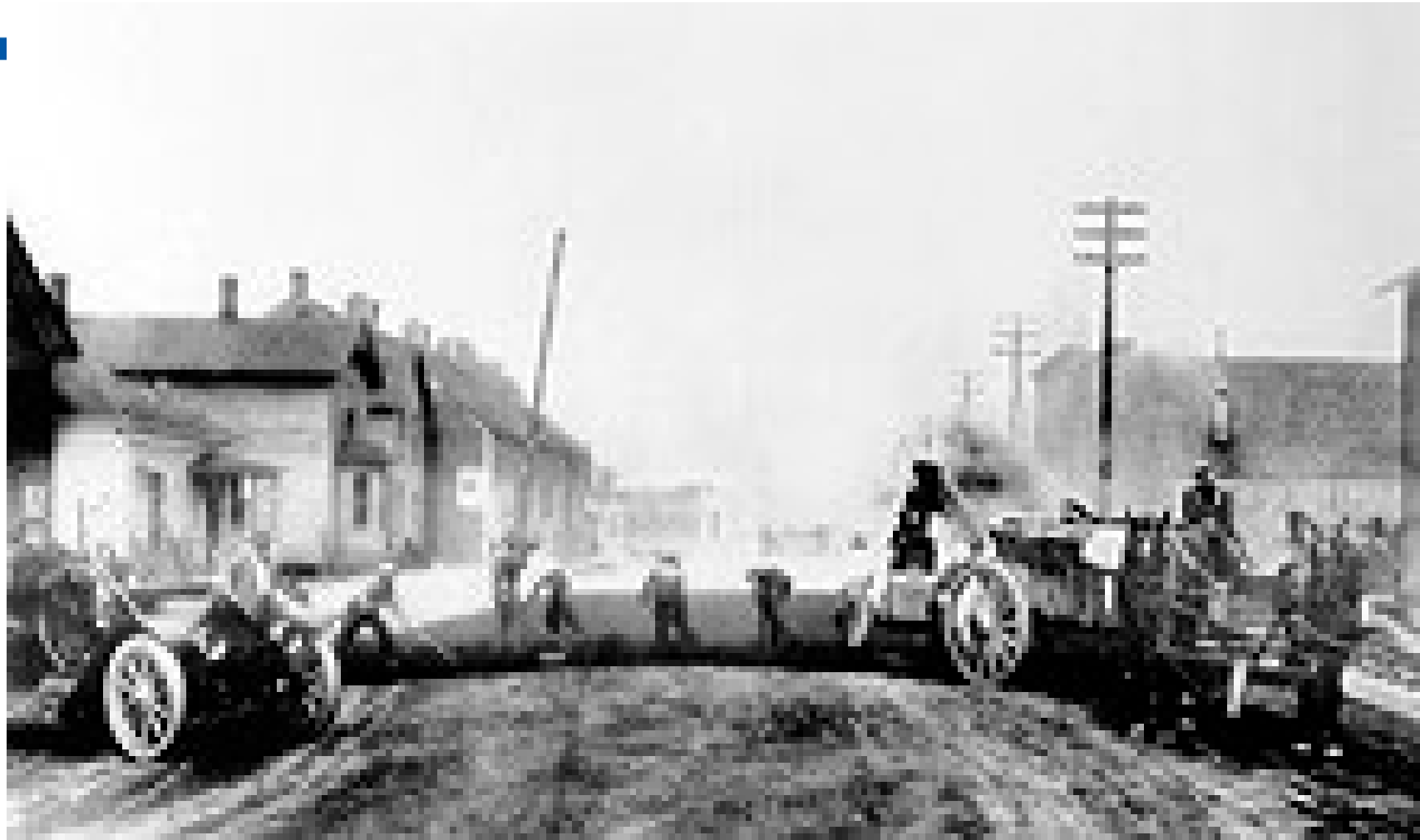
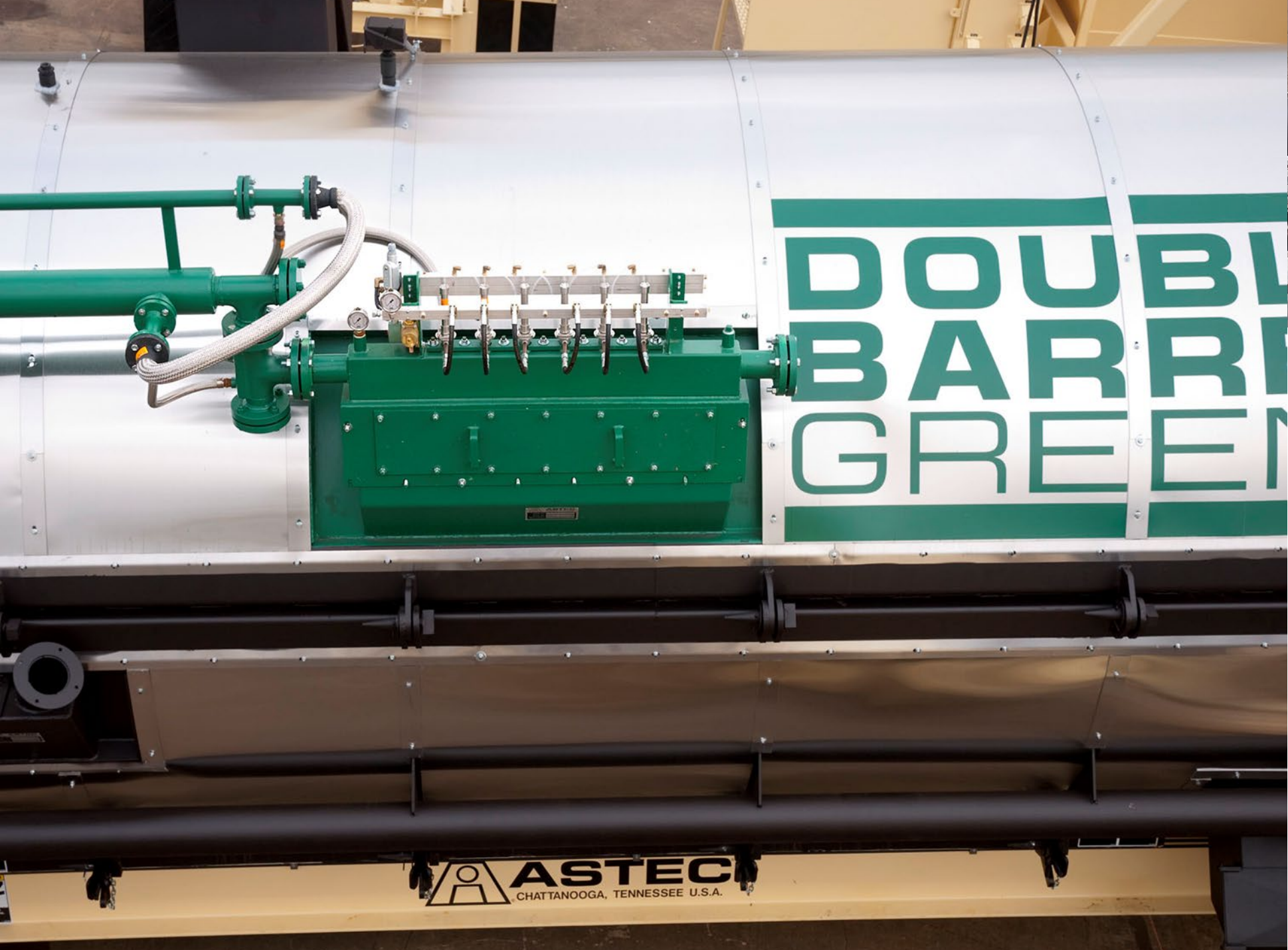






PHOTO OF BOTHELL ROAD  
TAKEN MAY 6, 1912  
BY O. S. SEATTLE, W. N.





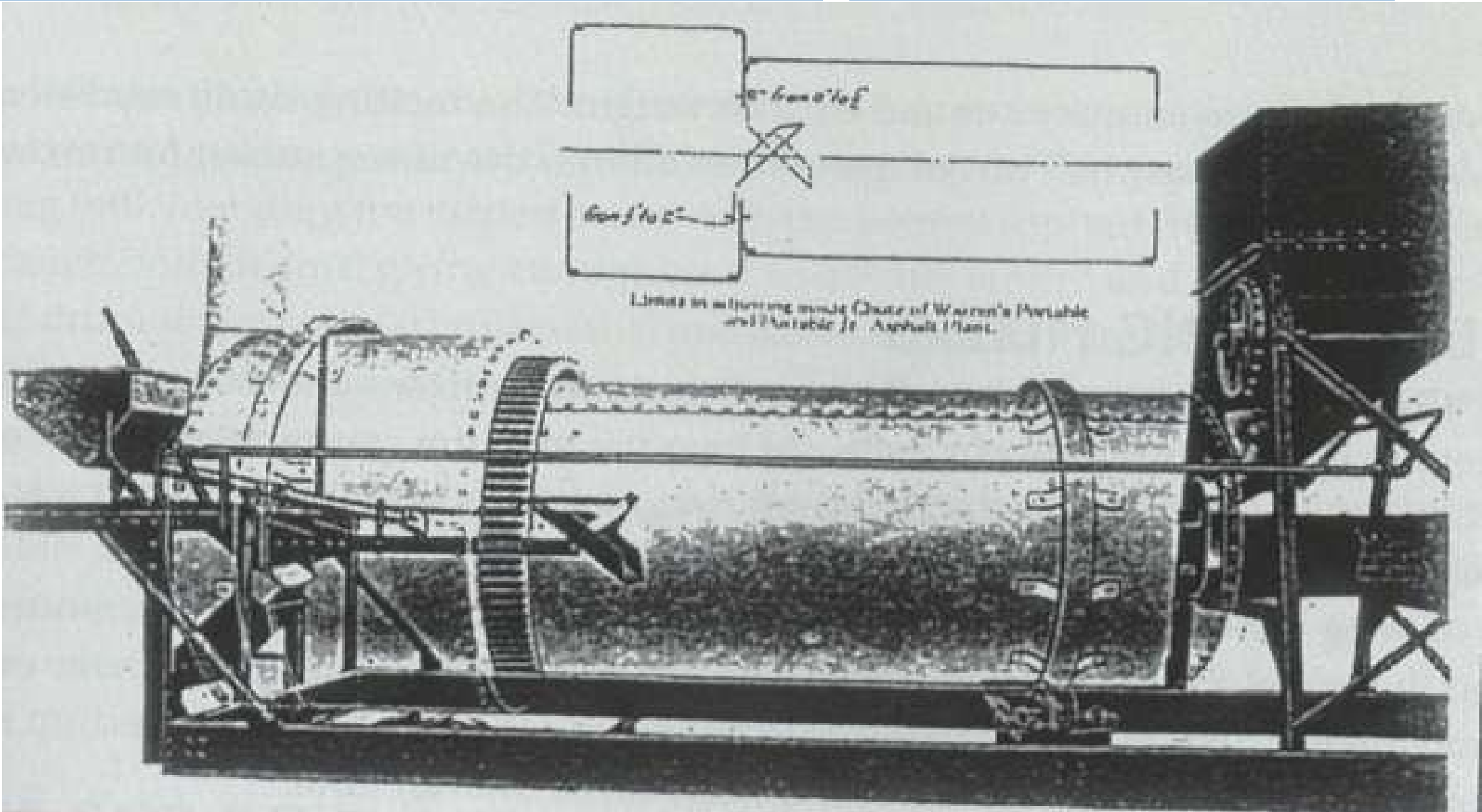
# DOUBLE BARREL XHR®

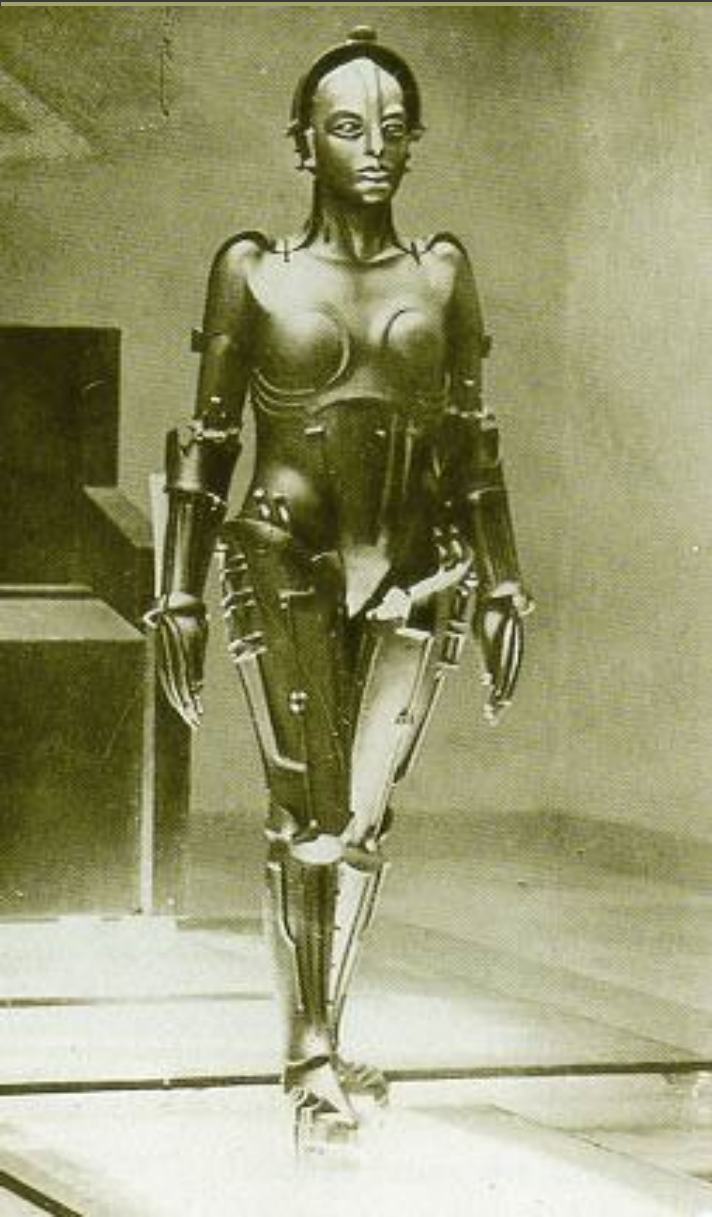


**It's not EVOLUTION.**



# Warren Brothers Portable





**It's INNOVATION.**



# Innovation Drivers

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**MIX DEMAND, ECONOMICS, MIX DESIGN,  
REGULATION, COMPETITION**

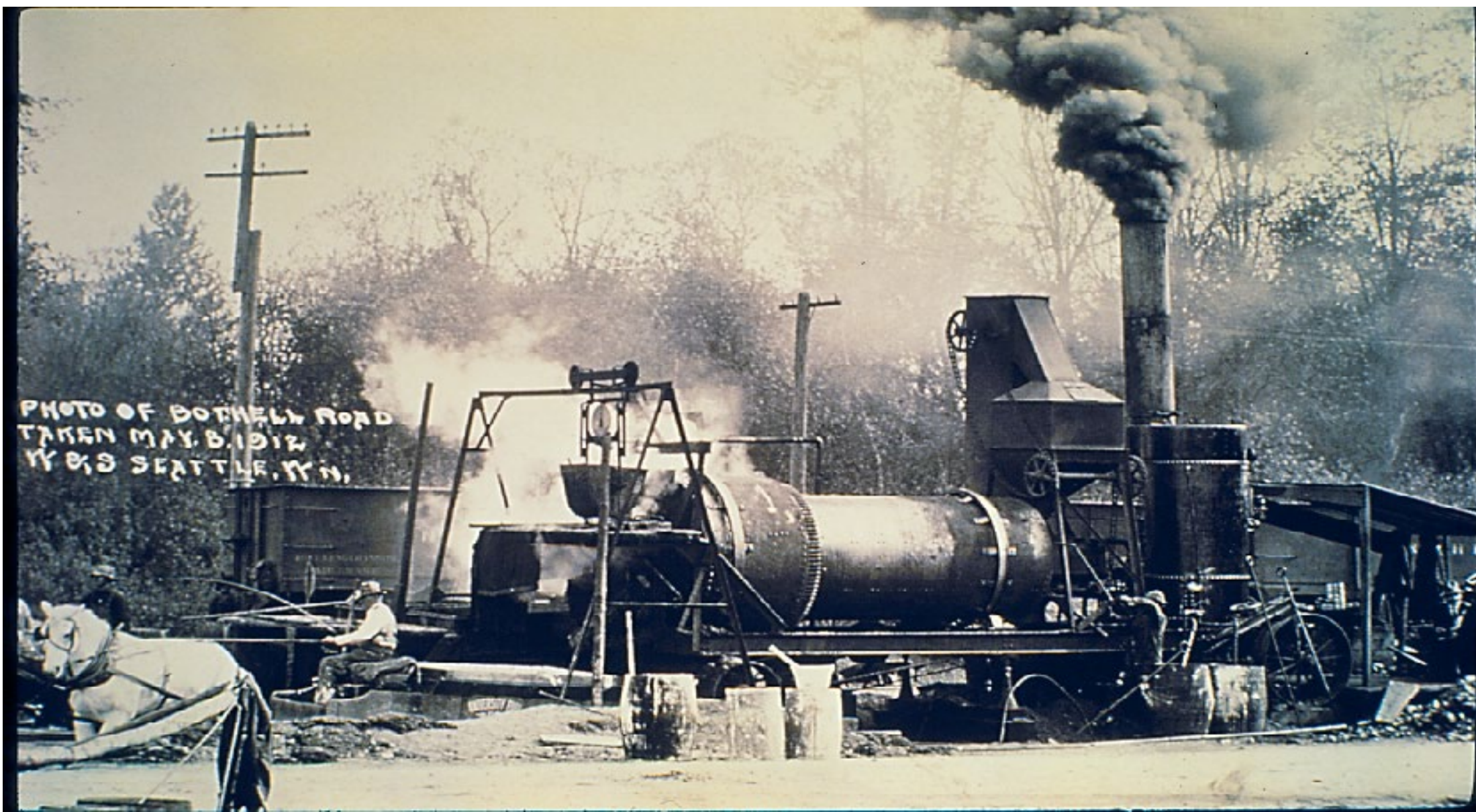
**CREATES NEED**

**“AVAILABLE” TECHNOLOGY**

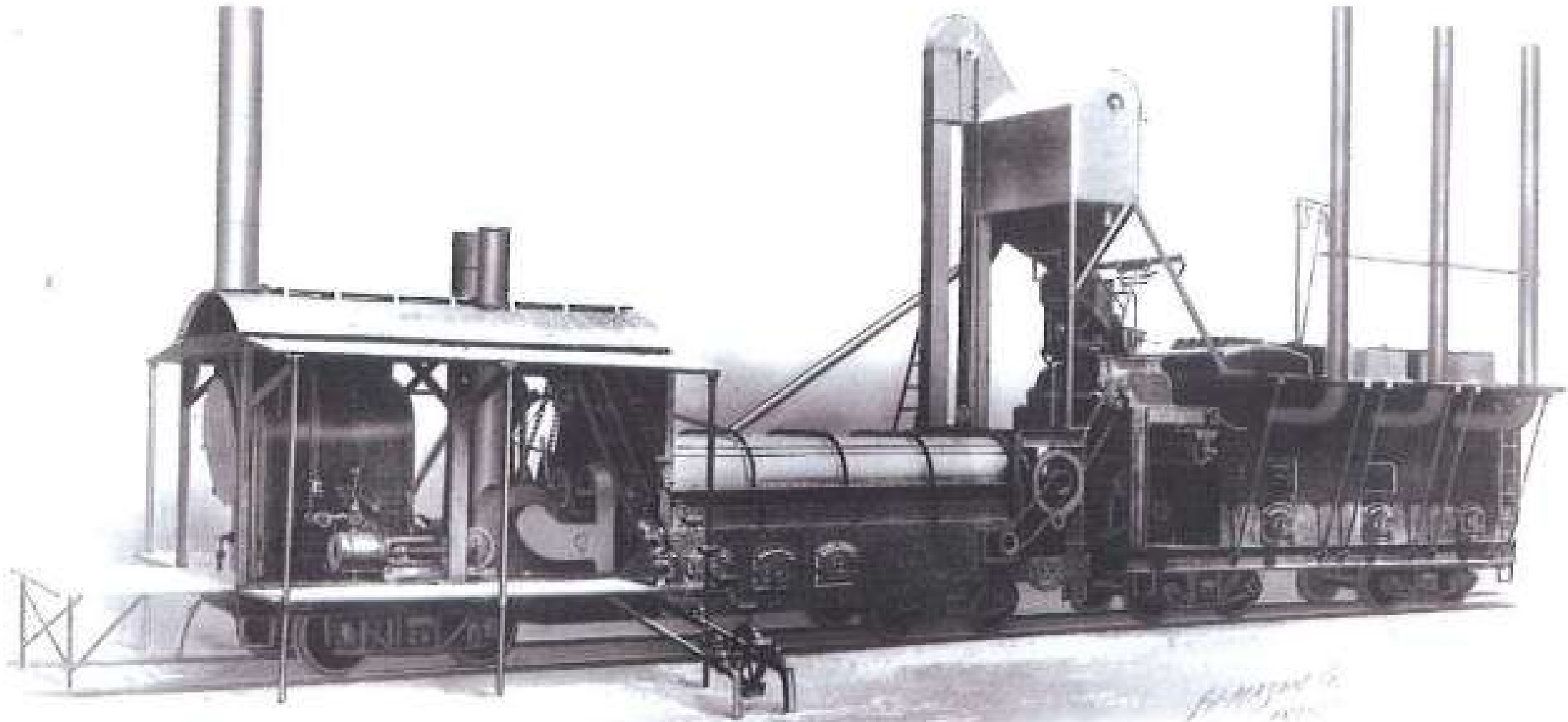
**ADAPT, INNOVATE**



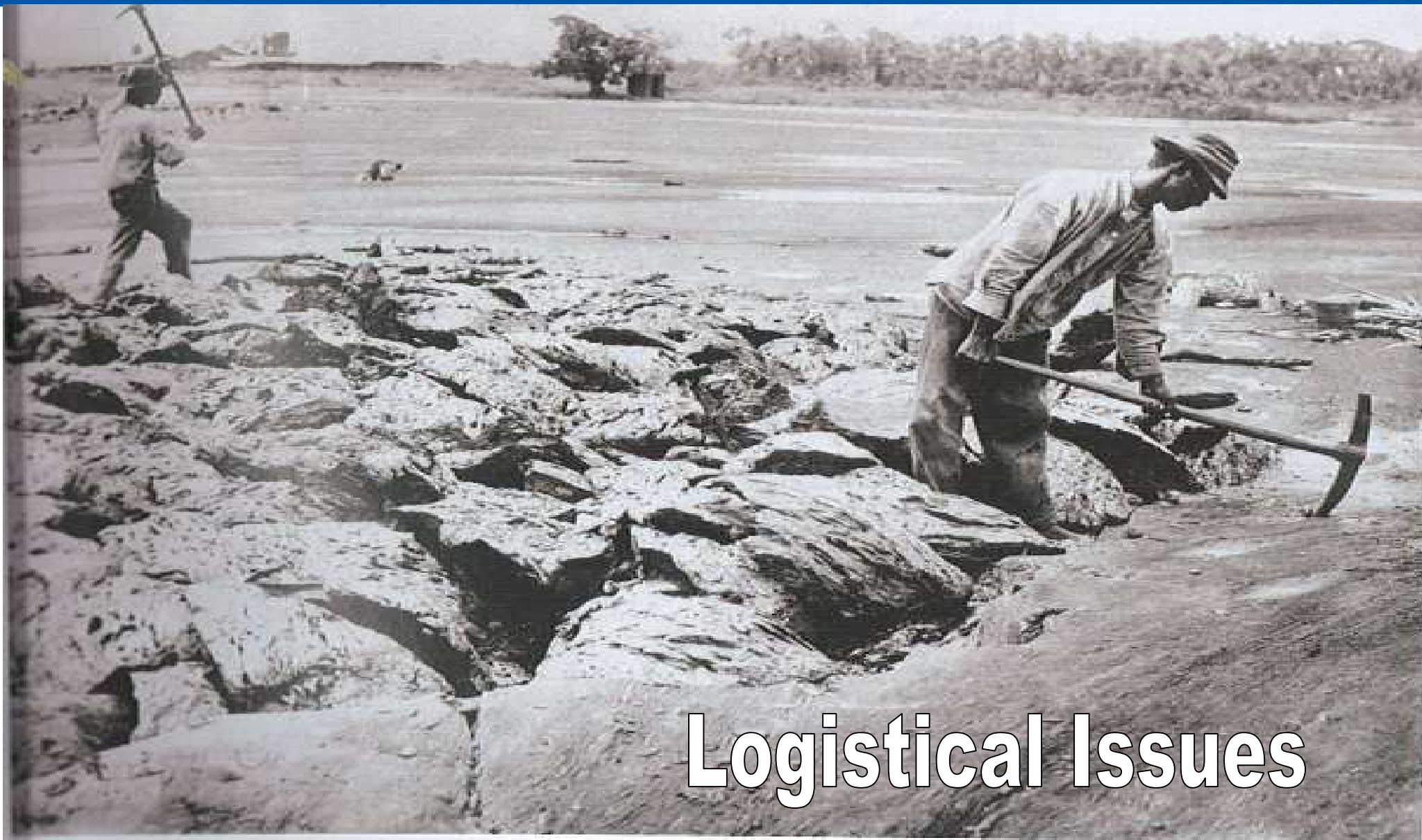
# Warren Brothers Plant Operating Outside Seattle, 1912



# Hetherington & Berner Railcar Portable, 1908



# Liquid Asphalt Harvesting from Trinidad Lake



**Logistical Issues**

# Liquid Asphalt Harvesting from Trinidad Lake

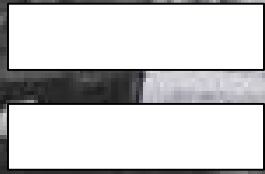


# Liquid Asphalt Harvesting from Trinidad Lake

High-quality material

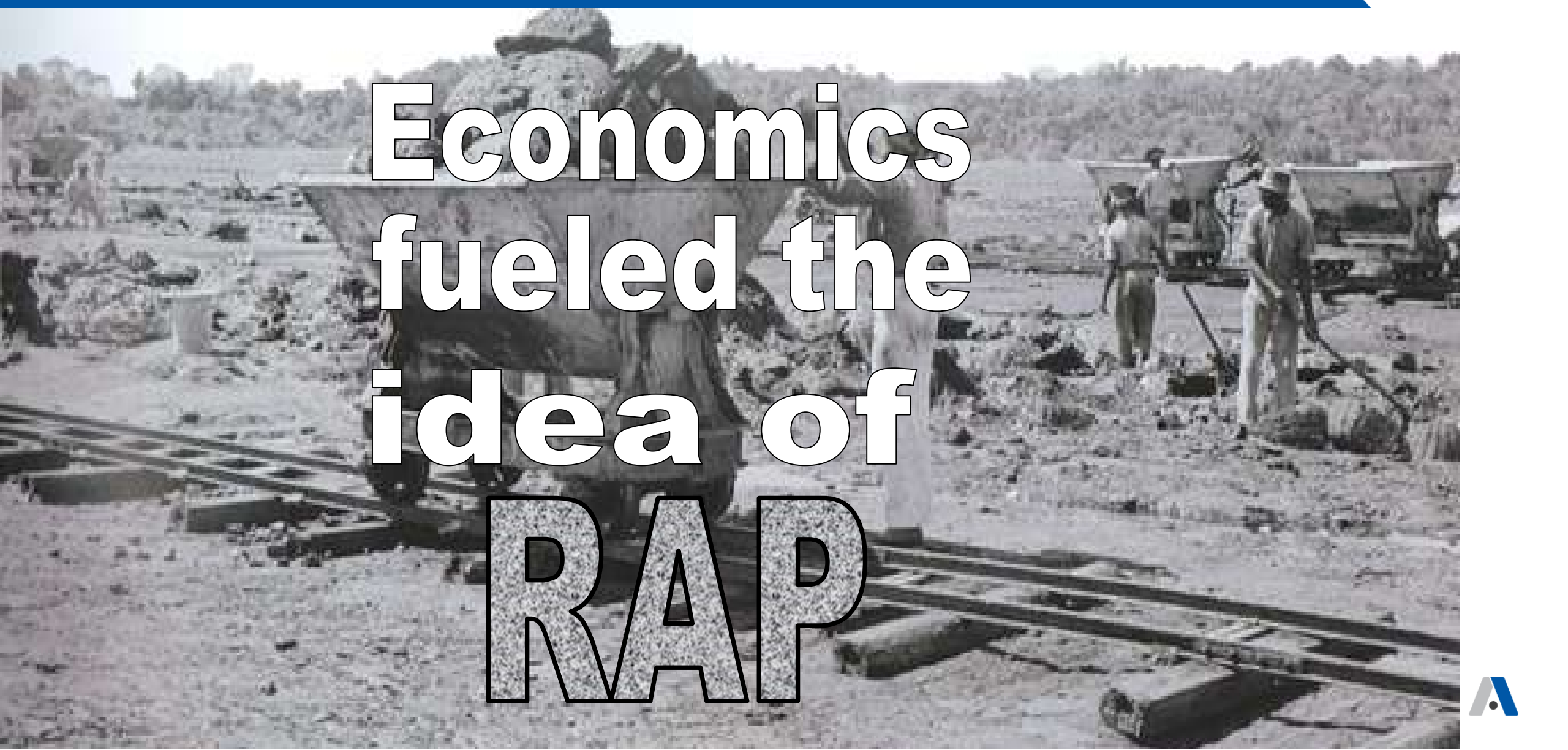
Distant Source

Political Instability



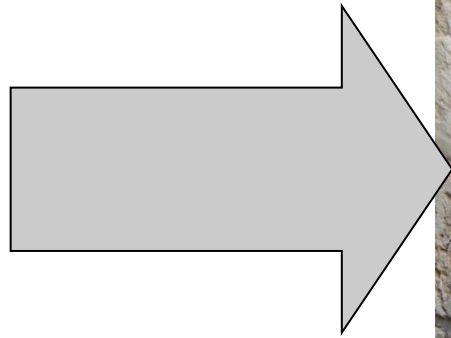
**Expensive**

## Economics a Major Driver

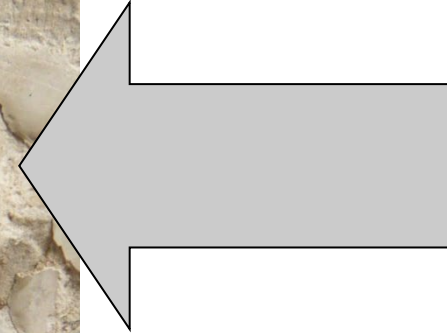


Economics  
fueled the  
idea of  
RAP

# Economics is Always a Driver



Jerusalem,  
March 2011



**Why shouldn't it?**

# Supply Change Drives Economics...

## History intervenes...

- January 10, 1901 near Beaumont, Texas
- Lucas Gusher -- took 9 days to cap
- Lost 850,000 barrels
- Oil price plummeted -- \$2/bbl to 3¢/bbl
- \$100/bbl to \$1.50/bbl

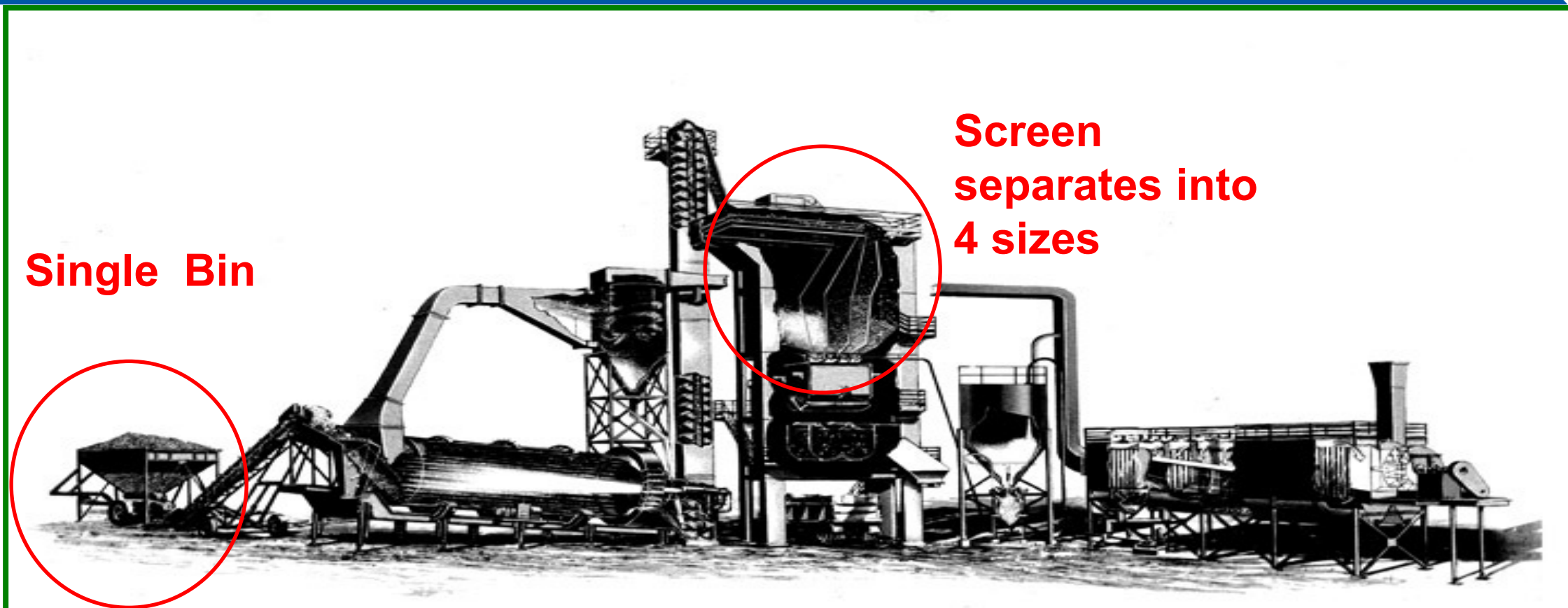
*photo courtesy of the American Petroleum Institute*





**28 months later...**

# Typical Plant Design from 1920's until 1950's

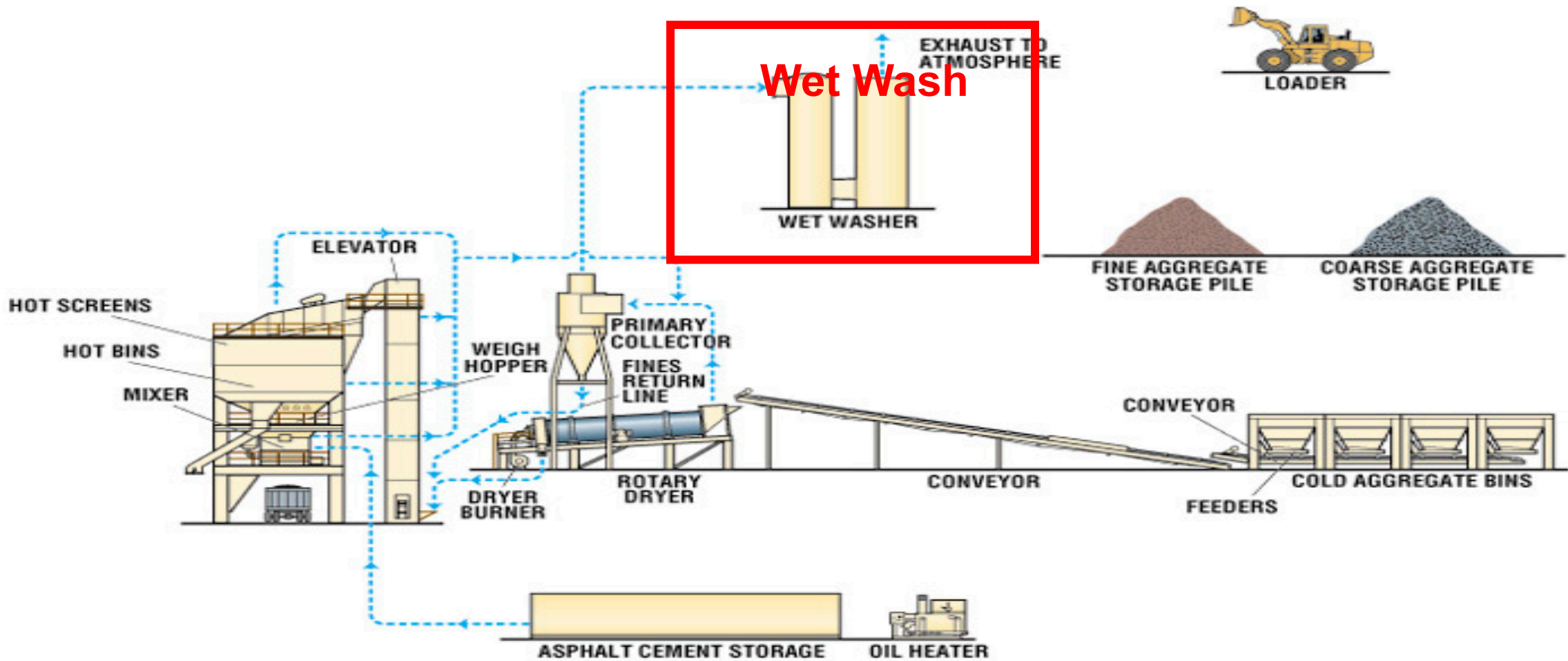


Single Bin

Screen separates into 4 sizes

**BATCH PLANT**  
ONE BIN COLD FEED

# 1960'S

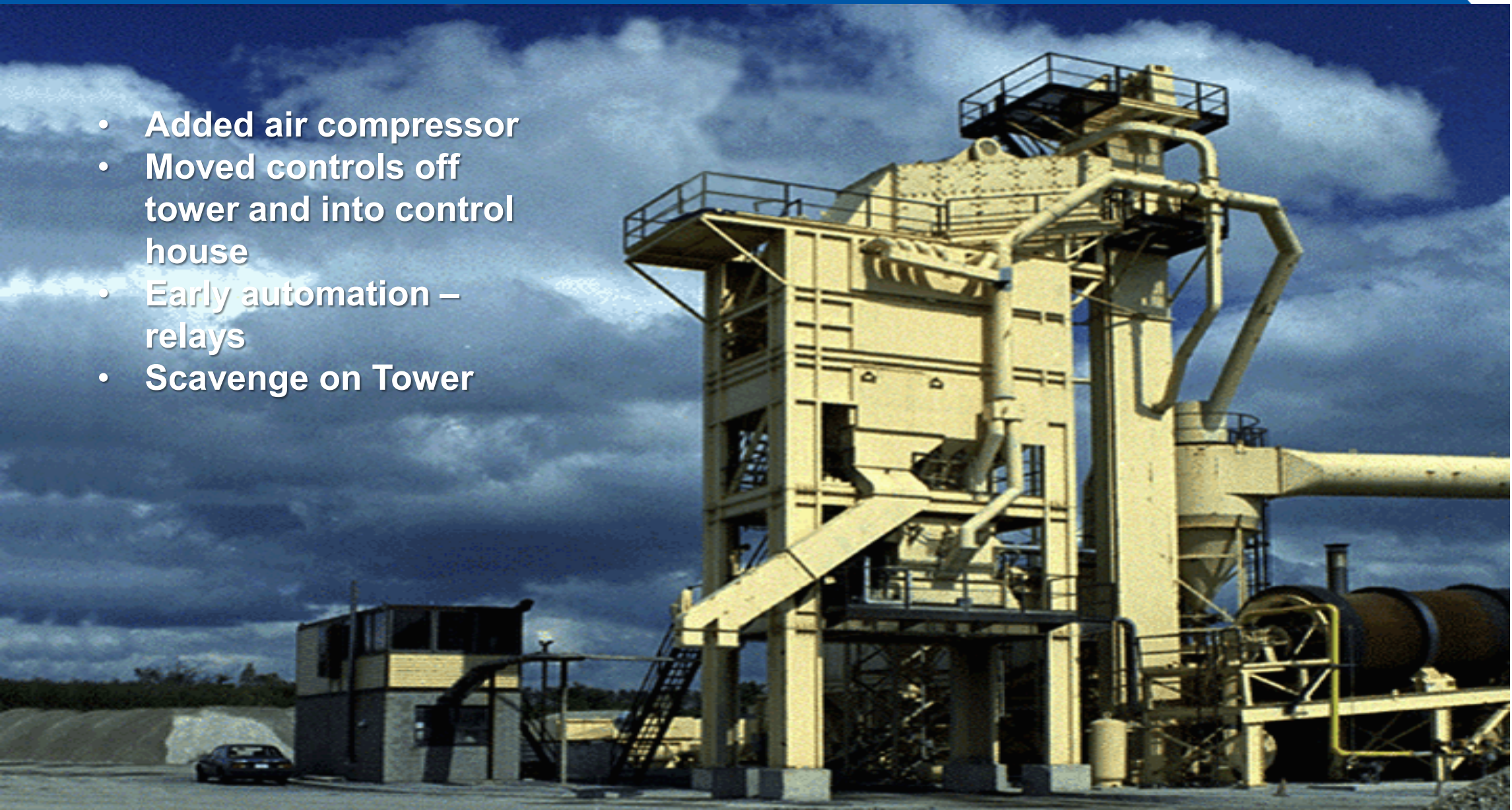


**PROCESS FLOW DIAGRAM FOR BATCH MIX ASPHALT PAVING PLANTS**



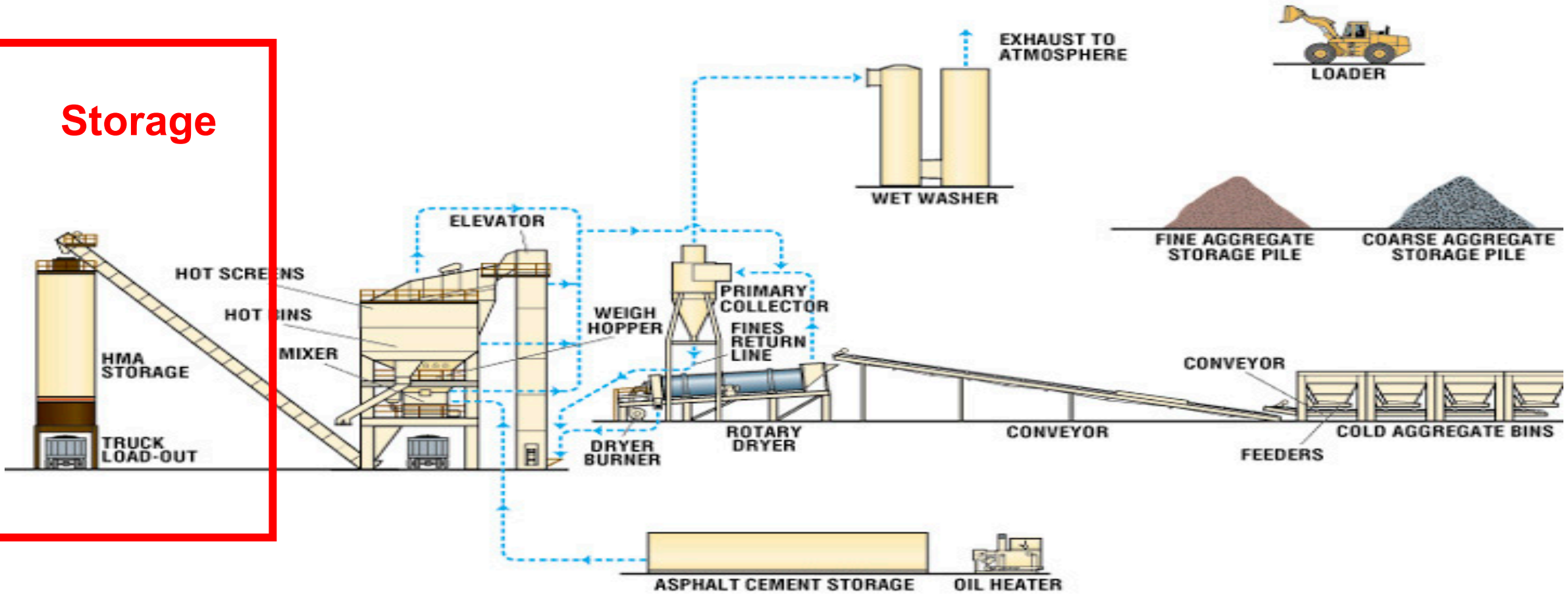
# 1960'S

- Added air compressor
- Moved controls off tower and into control house
- Early automation – relays
- Scavenge on Tower



# 1966

Storage

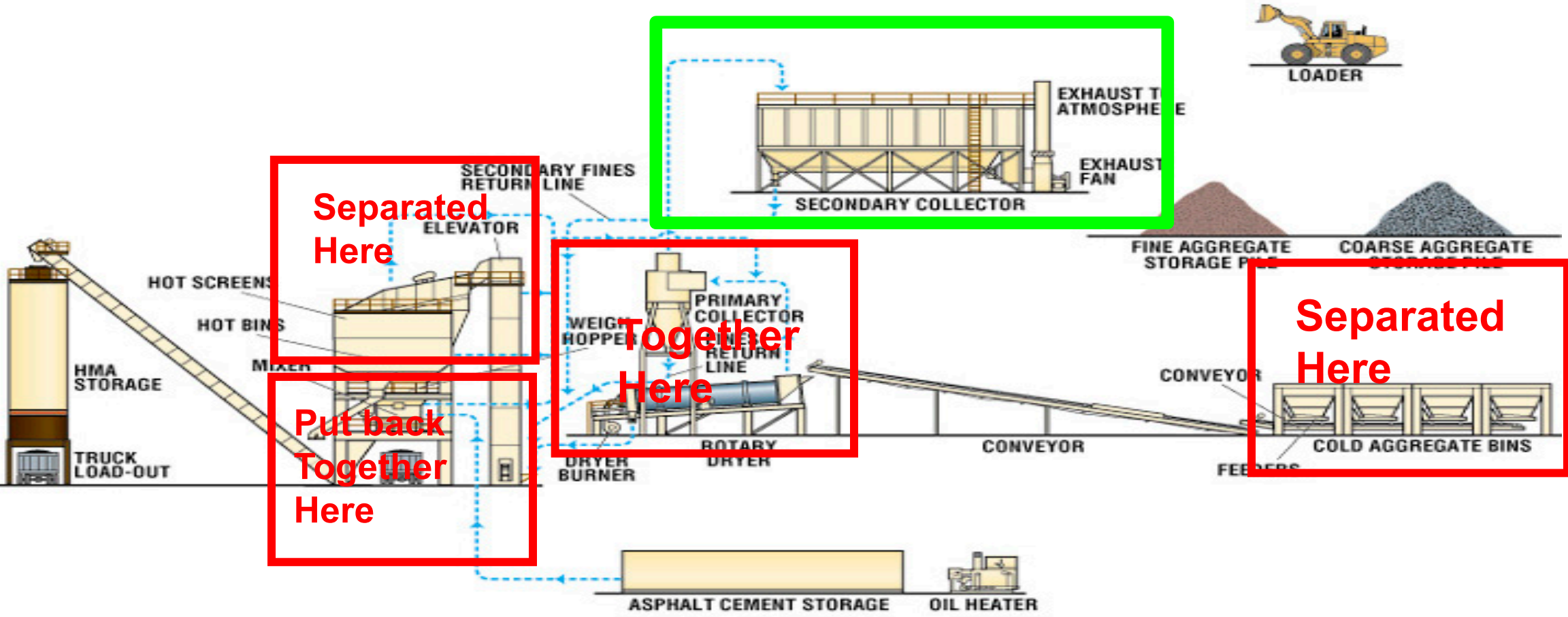


**PROCESS FLOW DIAGRAM FOR BATCH MIX ASPHALT PAVING PLANTS**



# Much Material Handling...

## Clean Air Act of 1970



**PROCESS FLOW DIAGRAM FOR BATCH MIX ASPHALT PAVING PLANTS**



# World Events Shape Economics...



History intervenes...again.

# World Events Shape Economics...



- **October 1973 Embargo begins.**
- **Oil price jumps from \$3/bbl to \$12/bbl.**


# Many Factors Come into Play

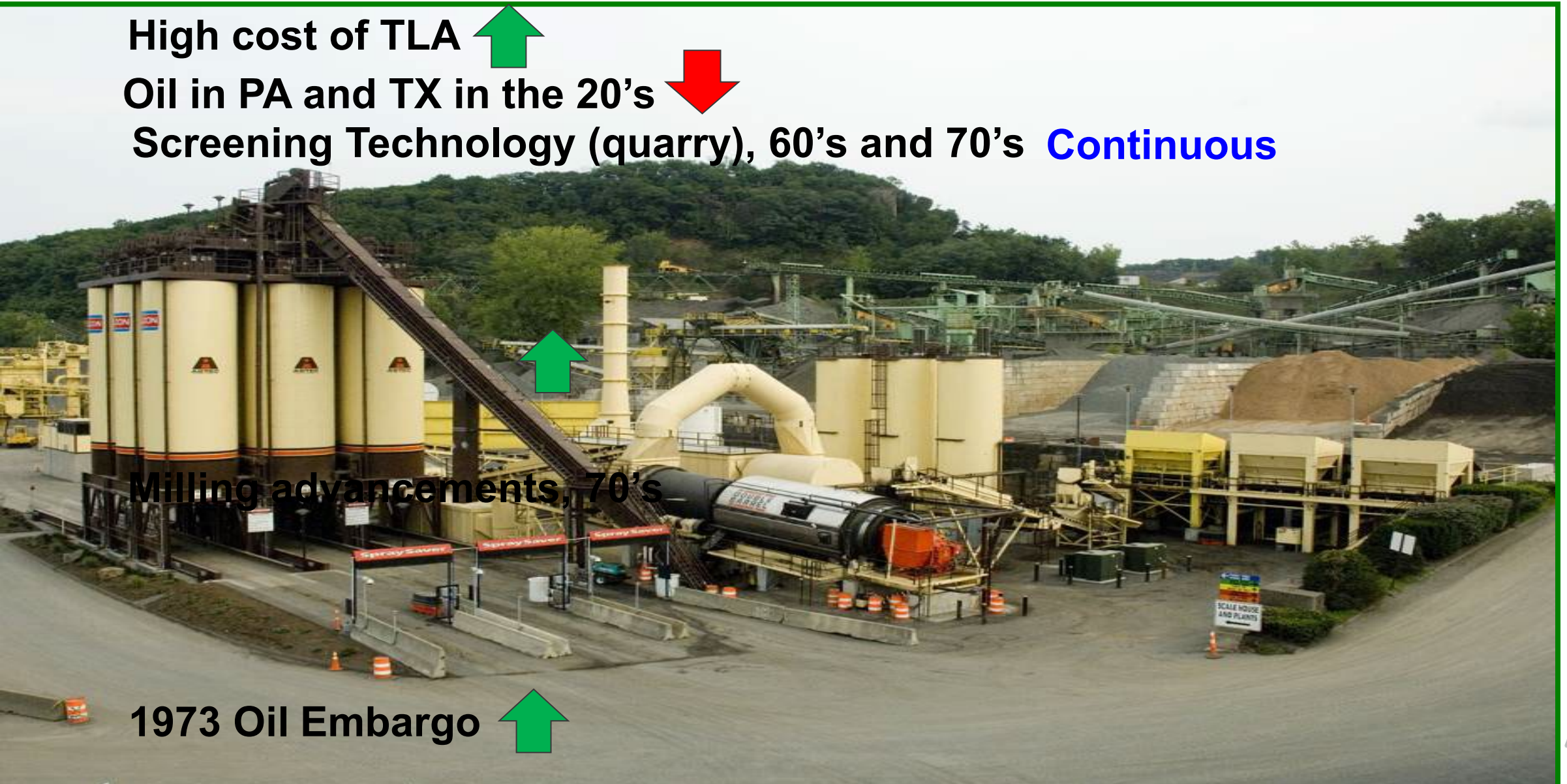
High cost of TLA 

Oil in PA and TX in the 20's 

Screening Technology (quarry), 60's and 70's **Continuous**

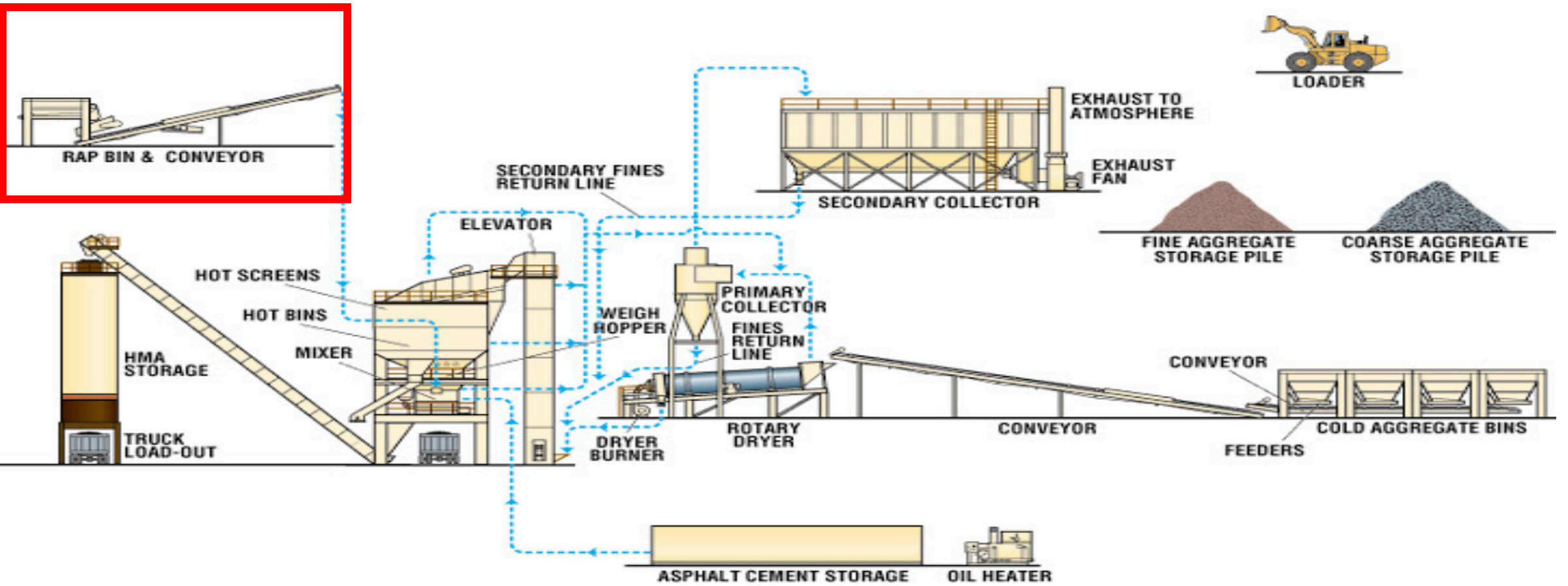
Milling advancements, 70's 

1973 Oil Embargo 



# Need to add RAP? Add a bin!

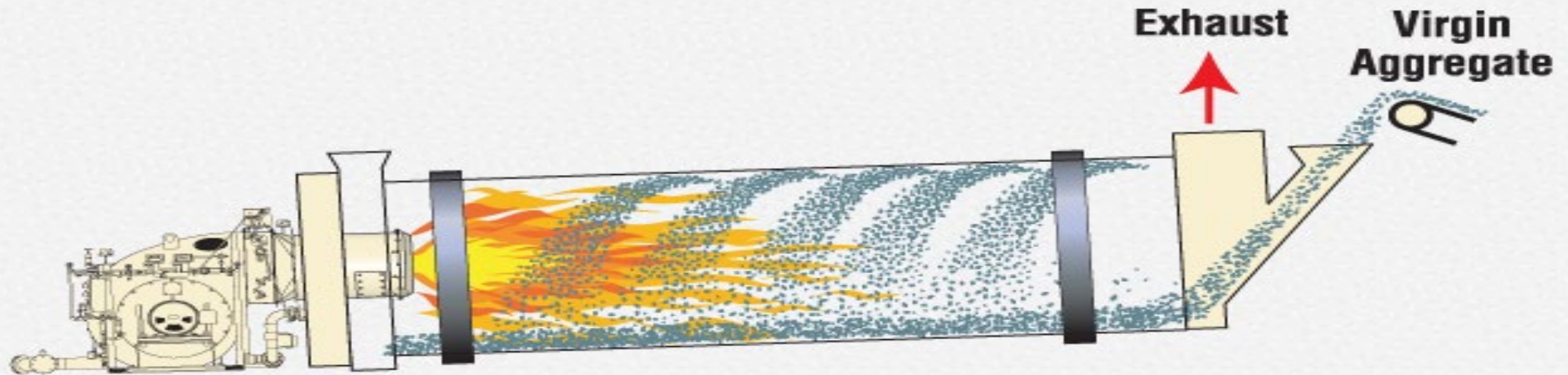
## RECYCLE BINS ADDED IN LATE 1970'S EARLY 1980'S



**PROCESS FLOW DIAGRAM FOR BATCH MIX ASPHALT PAVING PLANTS**



Batch plants use an efficient dryer, but...



Historically don't do well with high levels of recycle (indirect).

**Counterflow Drying Drum**



# Running RAP is like...

**Cold  
Water**



**RAP**

(Ambient Temperature)

**+**

**Hot  
Water**



**Virgin  
Aggregate**

(Superheated Temperature)

**=**

**Warm  
Water**



**Mix**

(Mix Temperature)

# Steam “Explosion”



# Aggregate Temperature

All stored aggregate superheated when running RAP.



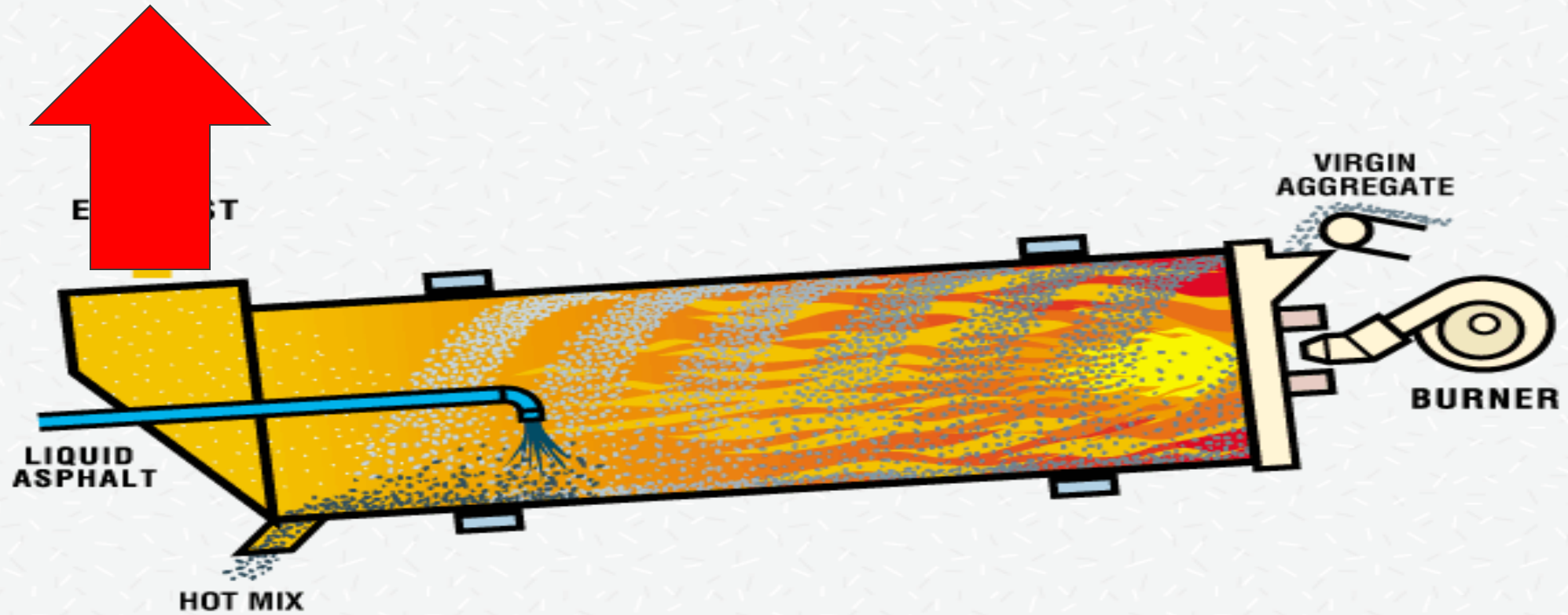
# Answer: Continuous Production

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- Ability to change (RAP-Virgin-RAP) quickly
- No more steam explosion.
- Solves stored “super hot rock”
- Gradation control in coldfeed bins



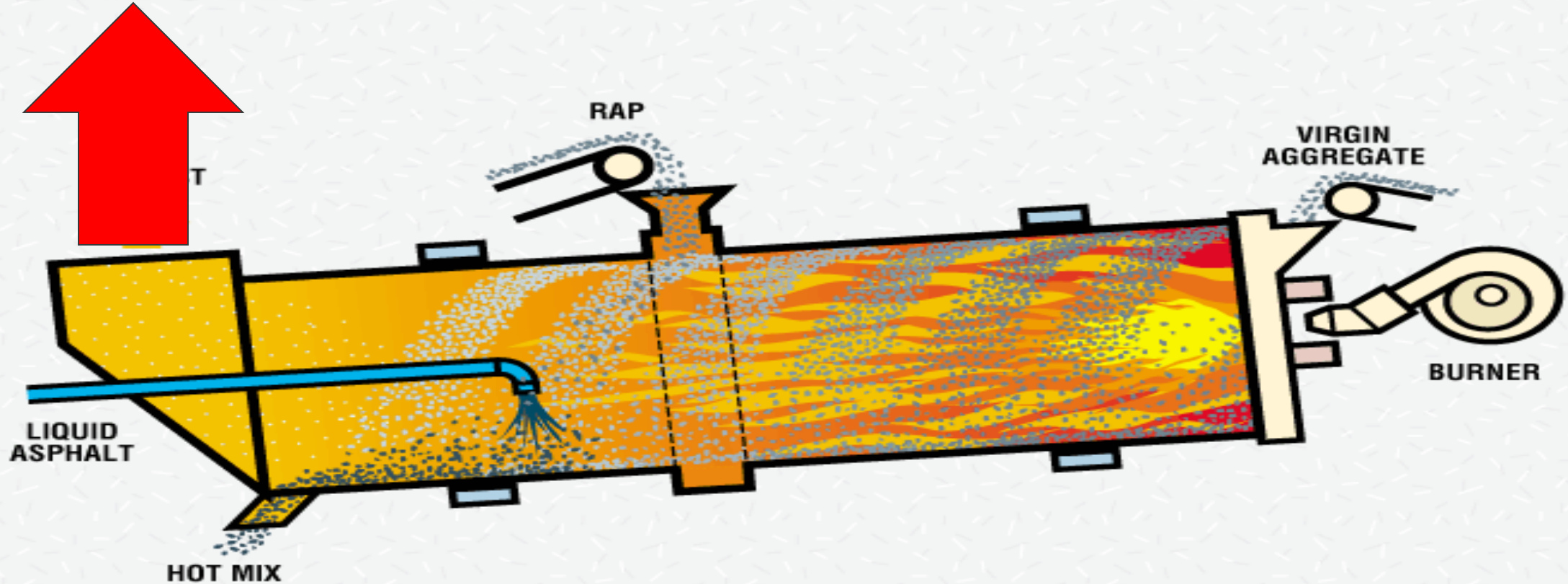
# Parallel Flow Continuous HMA Plant



**ORIGINAL PARALLEL-FLOW DRUM MIXER**

# Parallel Flow Continuous HMA Plant with RAP

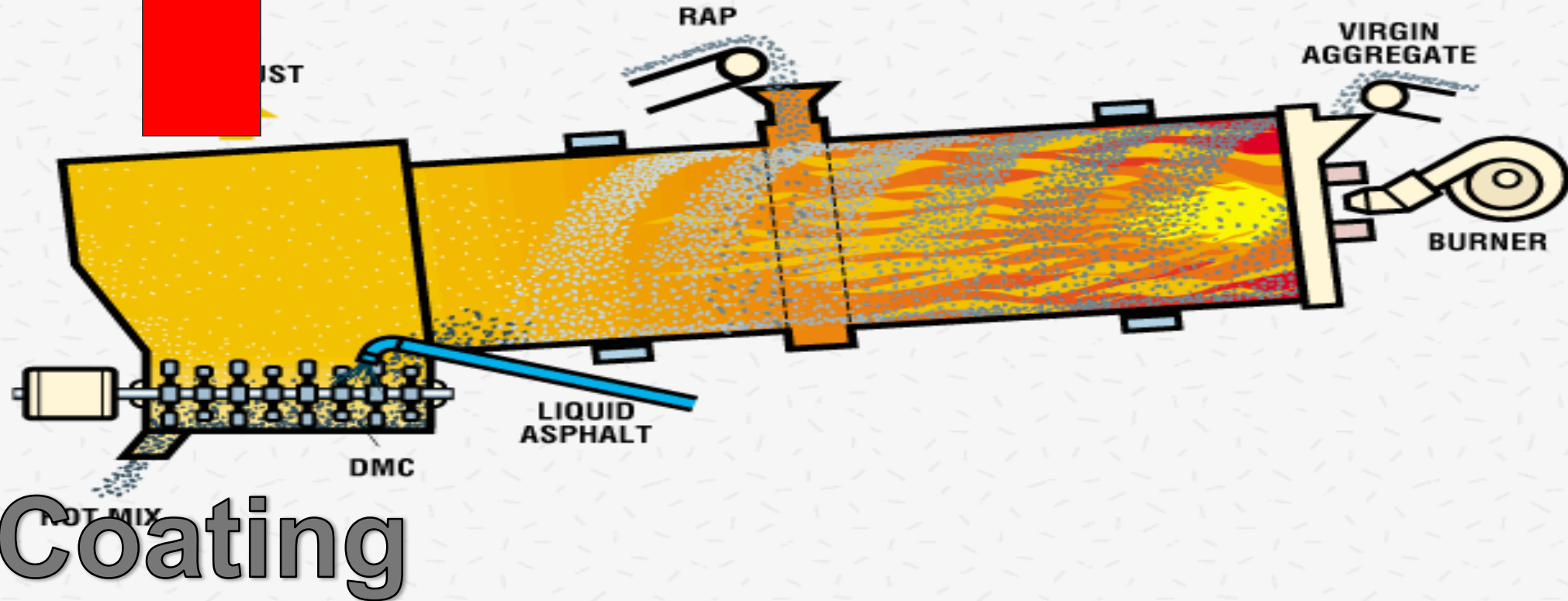
Smoke



**DRUM MIXER WITH CENTER INLET**

# Parallel Flow Drum Mix Coater I

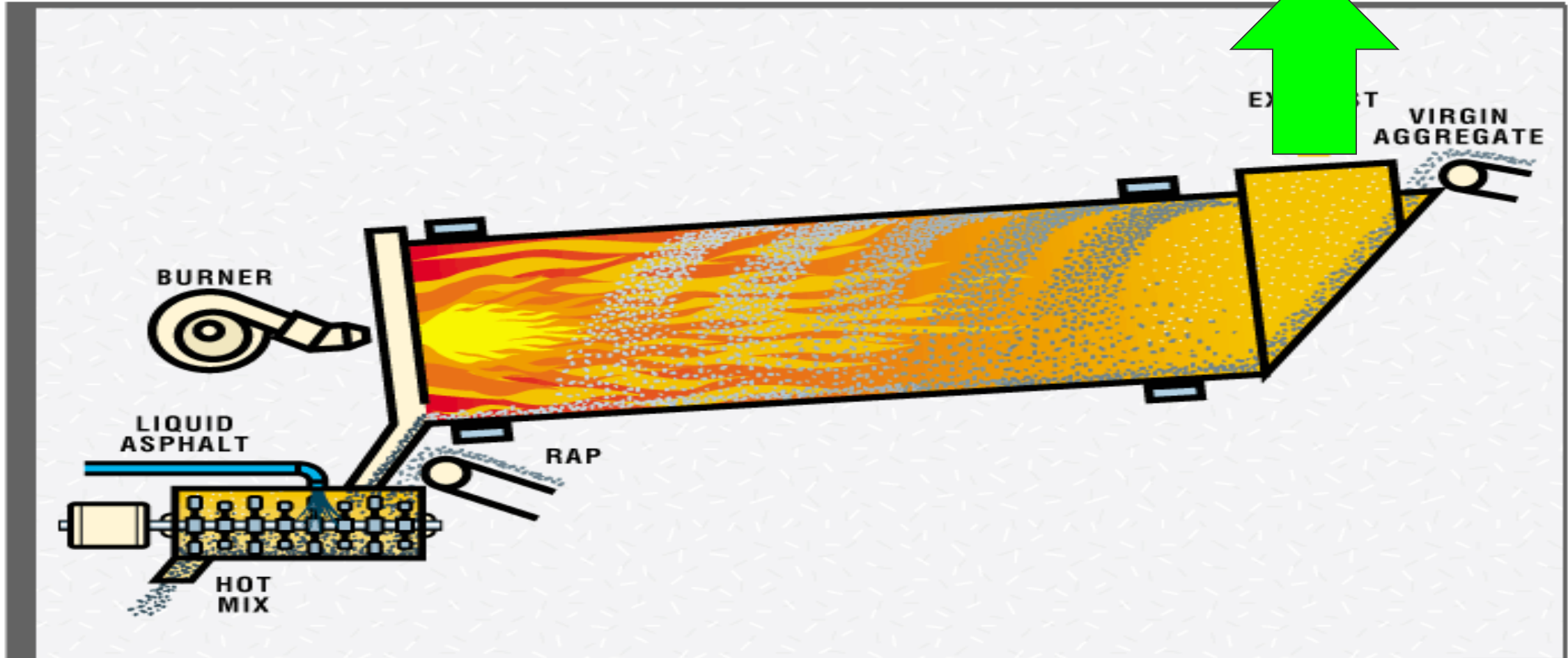
Smoke



Coating

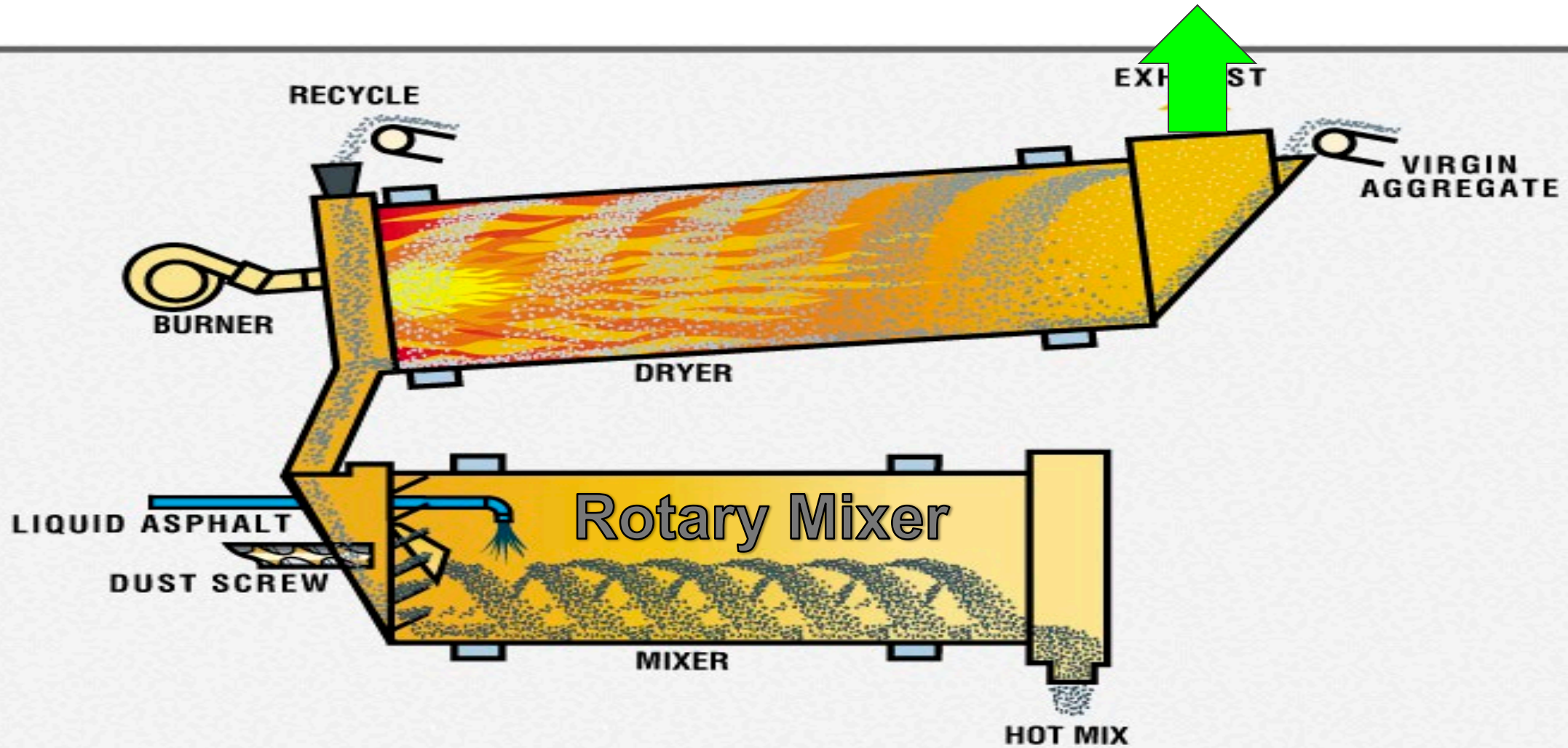
**DRUM MIX COATER-I (DMC-I)**

# Counterflow Drum Mix Coater II



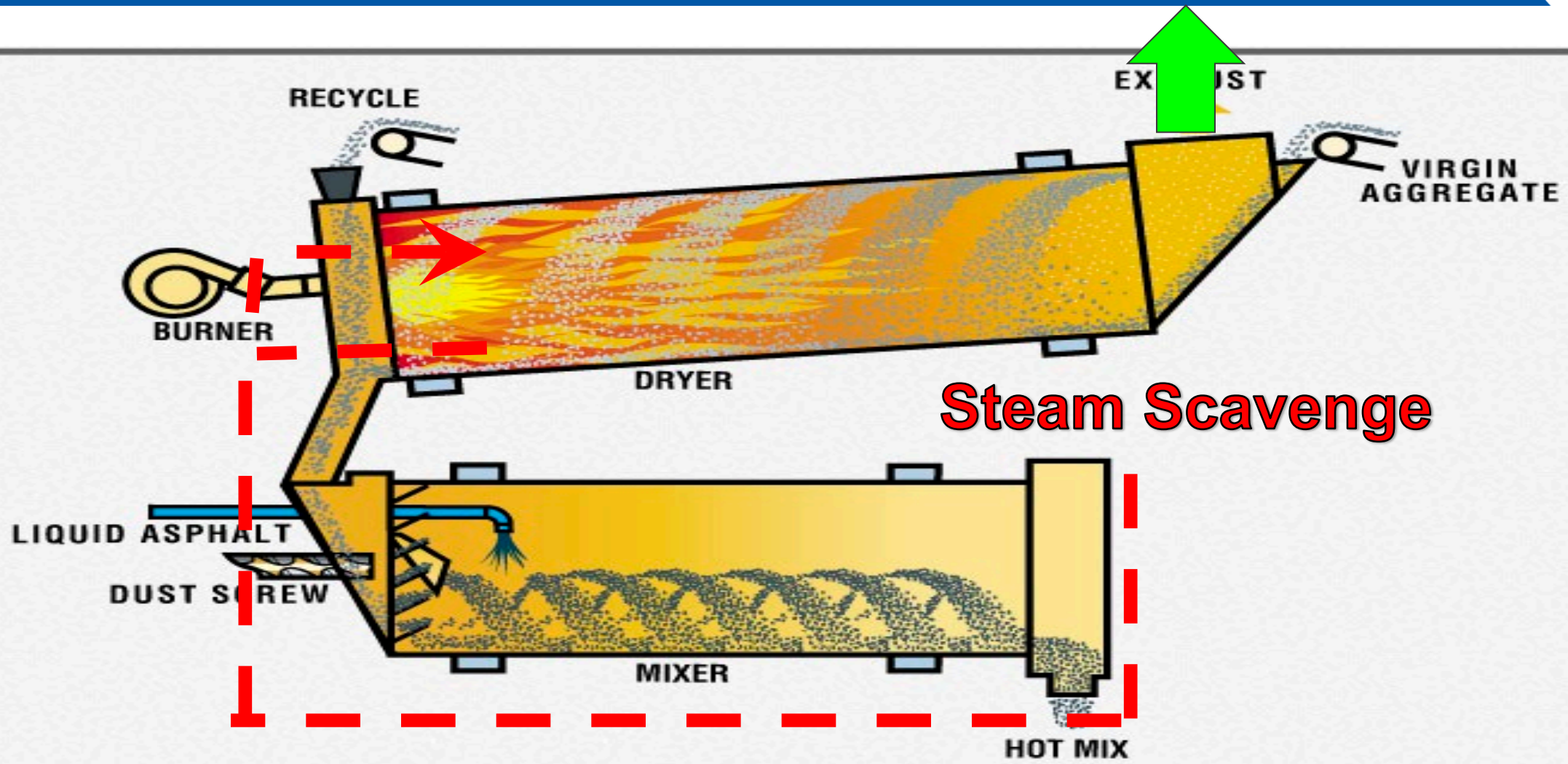
**DRUM MIX COATER-II (DMC-II)**

# Counterflow Drum Mix Coater II Alternative – “Double Drum”



**COUNTER FLOW DRYER AND ROTARY MIXER**

# Managing RAP Steam: Problematic



**COUNTER FLOW DRYER AND ROTARY MIXER**

# Managing RAP Steam: Examples



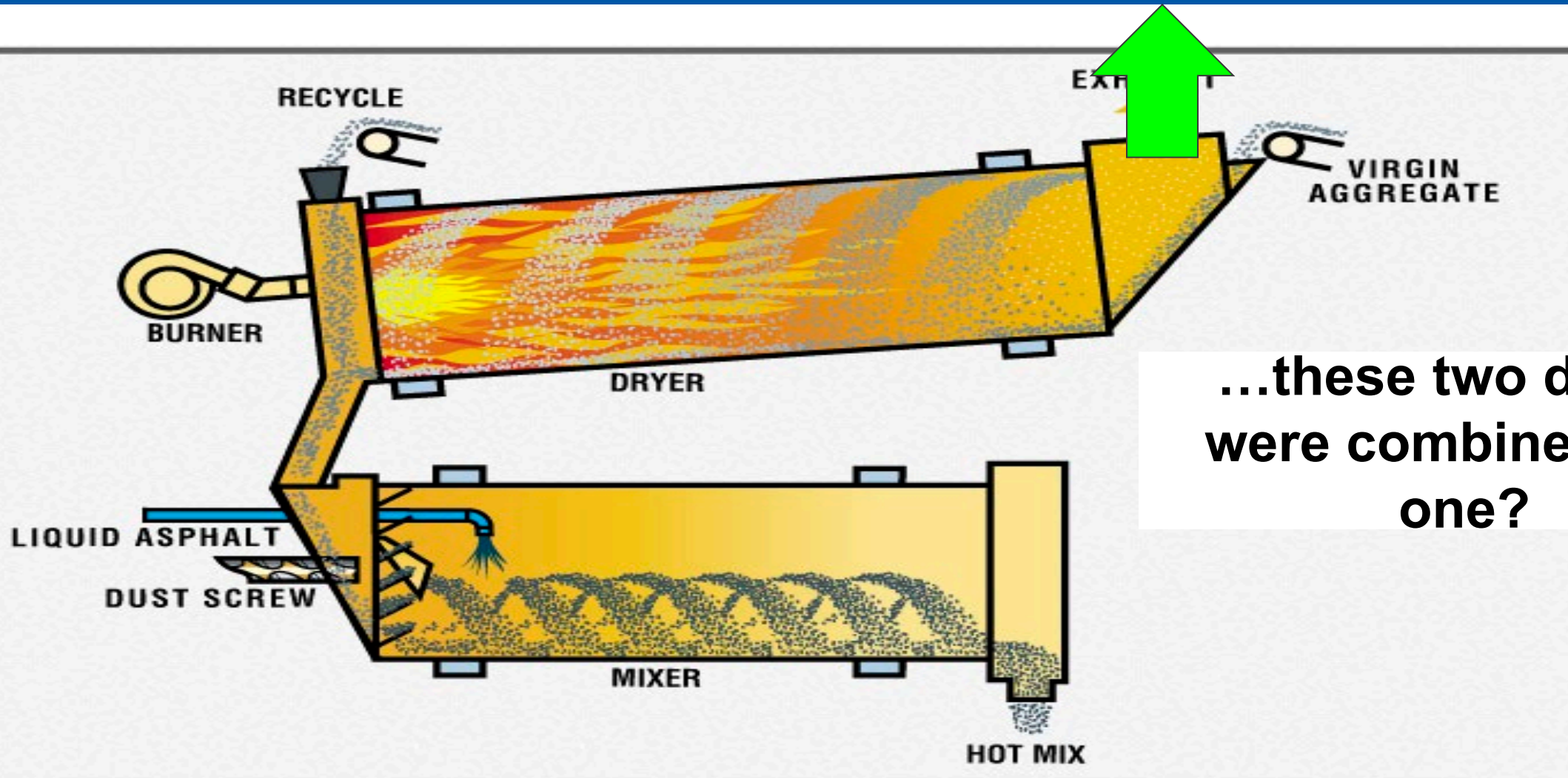
Non-Astec Double Drum, North Carolina, 2013;  
Steam Scavenge Retrofit (Before)

# Managing RAP Steam: Examples



Non-Astec Double Drum, North Carolina, 2013;  
Steam Scavenge Retrofit (After)

# Going back to this diagram.... What if...

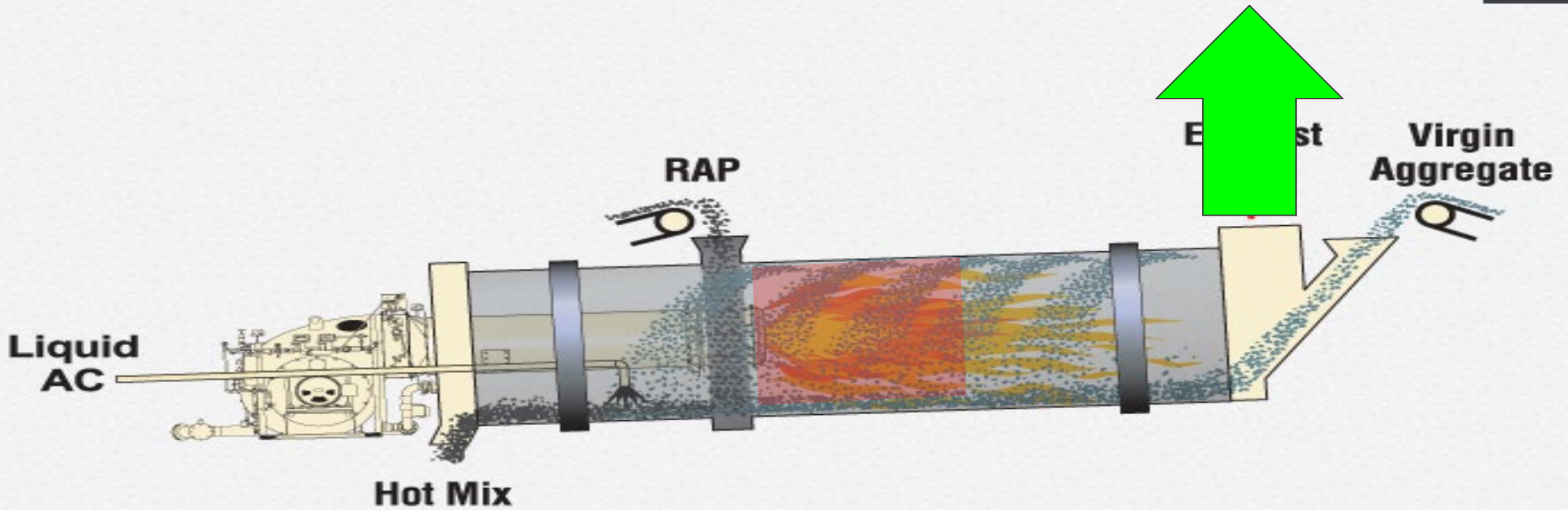


...these two drums were combined into one?

**COUNTER FLOW DRYER AND ROTARY MIXER**

# The “Unified” Drum: Counterflow Drum Mixer

F37



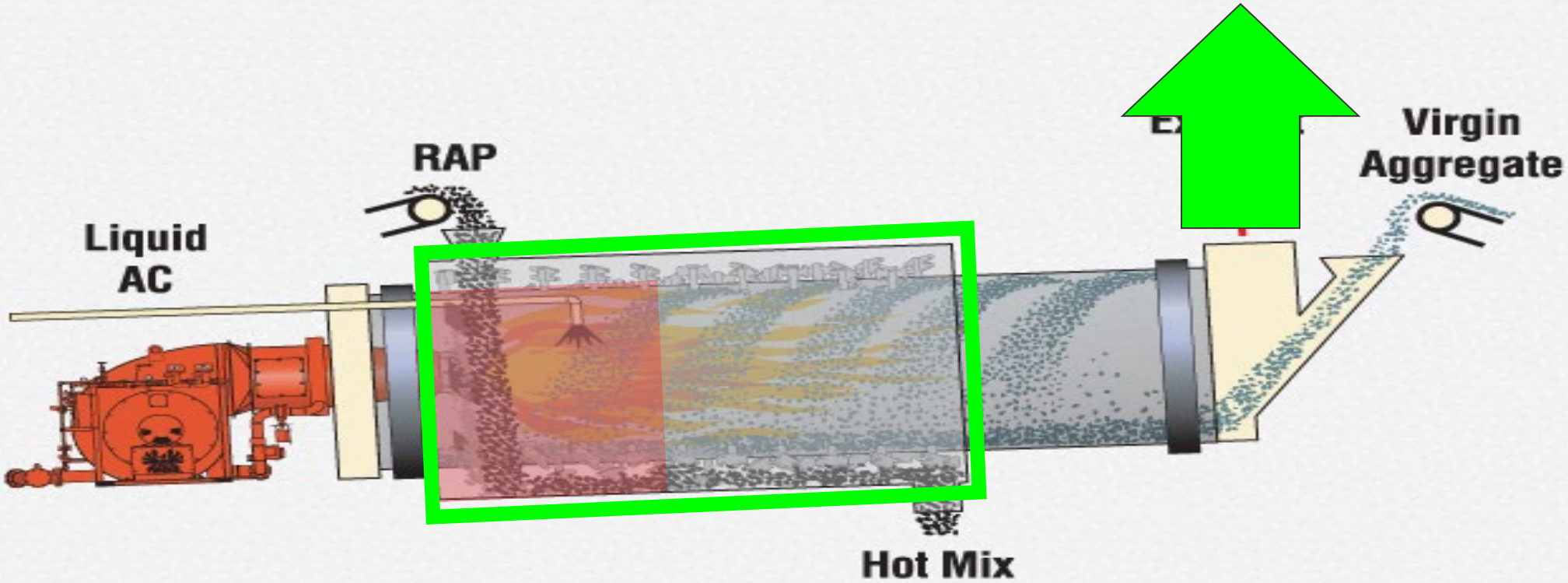
Mike Hawkins, Stansteel

Counterflow Drum Mixer



# Astec Double Barrel

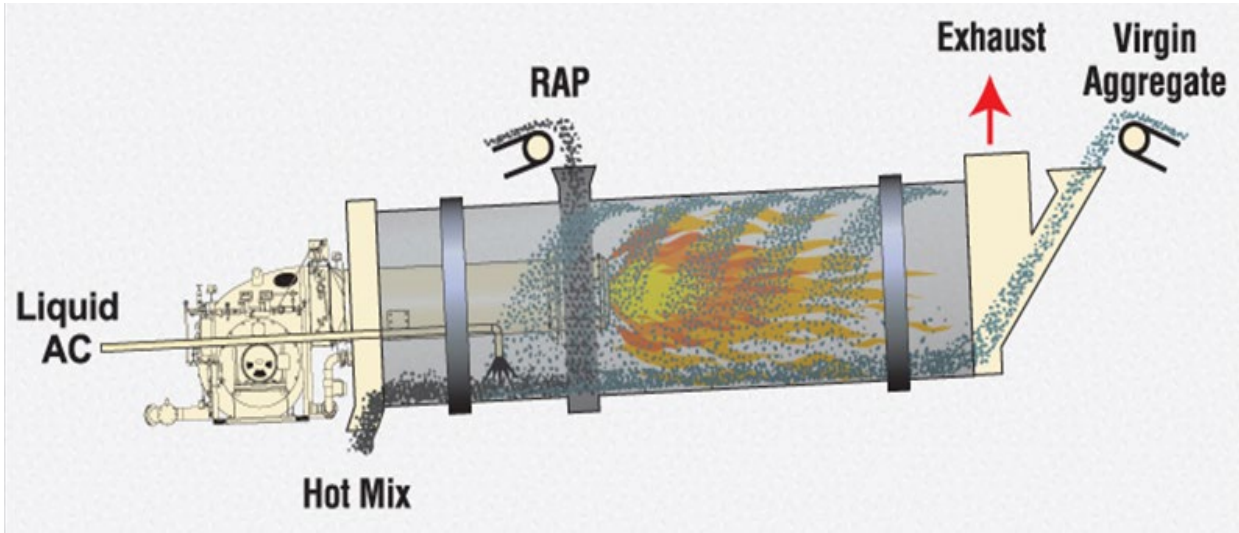
F38



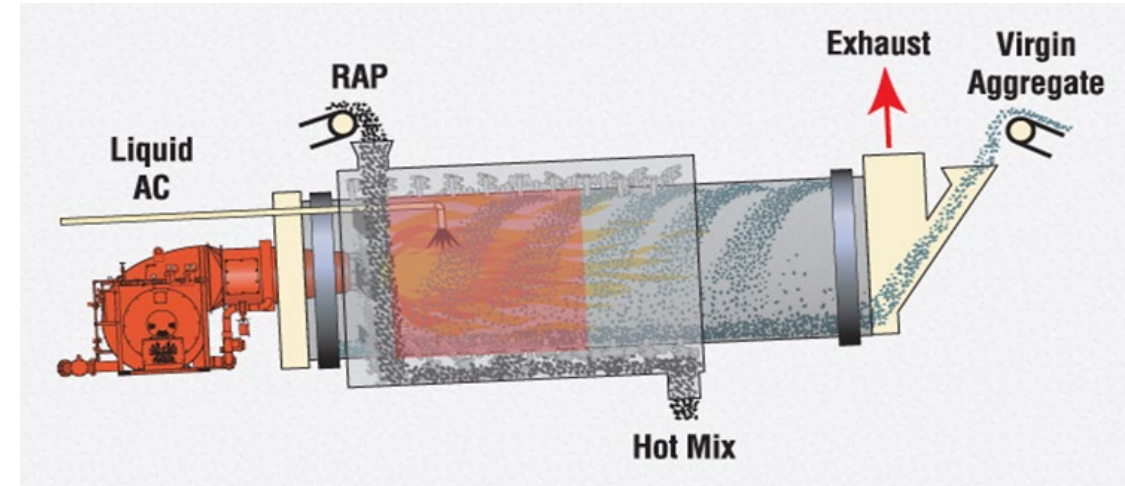
**Double Barrel® Combination Dryer/Mixer**



# Computer Analogy

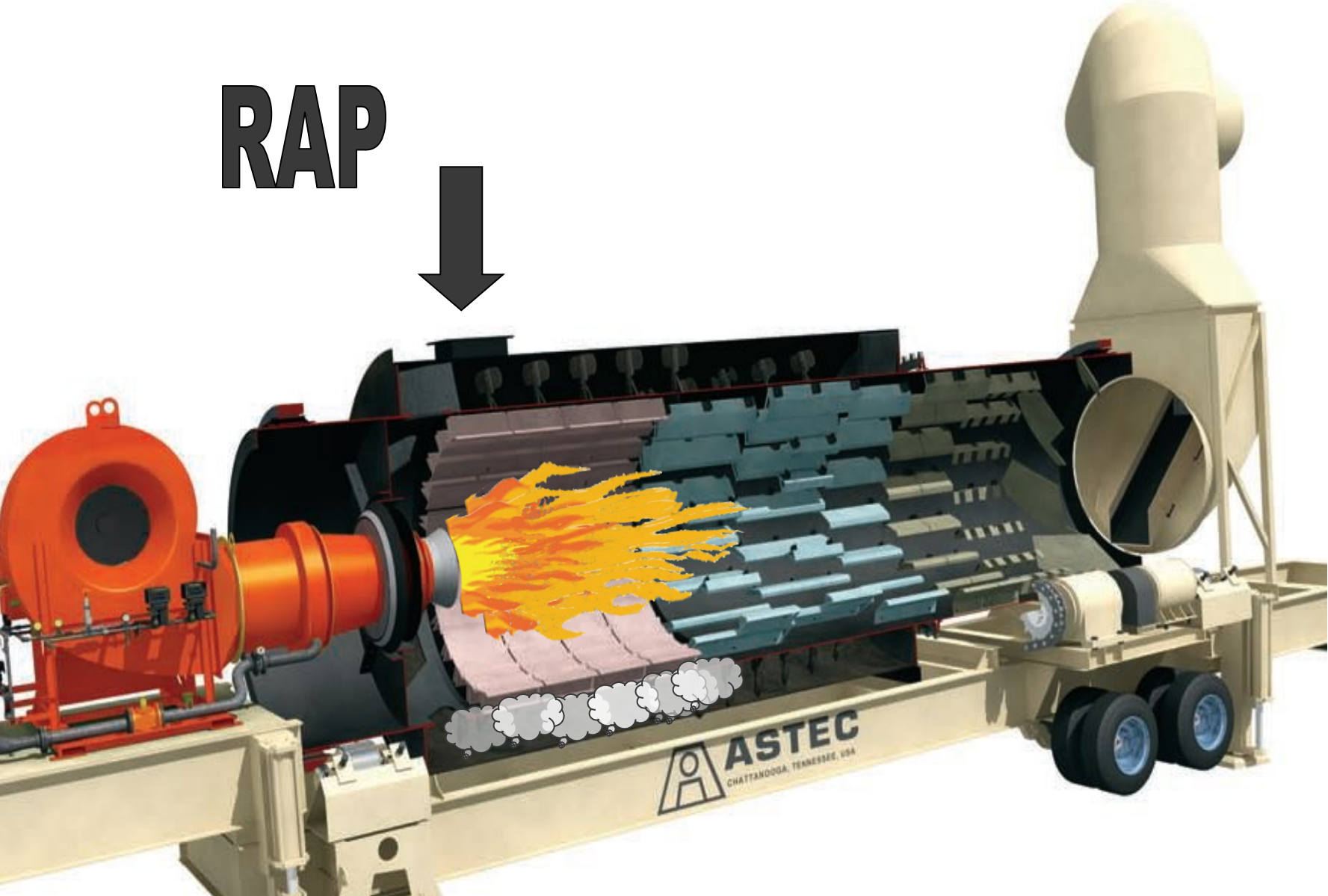


**PC**



# Advantage of Continuous Production: RAP Processing

RAP



# Advantage of Continuous Production: Emissions Mitigation

Fines  
↓ AC  
RAP ↓ ↓



**Rebranded a few years ago...**



**DBX**

**Double Barrel®**

**External Mixer**



# Astec Double Barrel XHR (2014)



# Astec Double Barrel XHR (2015)



# Remember the Innovation Drivers?

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**MIX DEMAND, ECONOMICS, MIX DESIGN,  
REGULATION, COMPETITION**

**CREATES NEED**

**“AVAILABLE” TECHNOLOGY**

**ADAPT, INNOVATE**



Here is where the challenges appear...

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**“AVAILABLE” TECHNOLOGY**

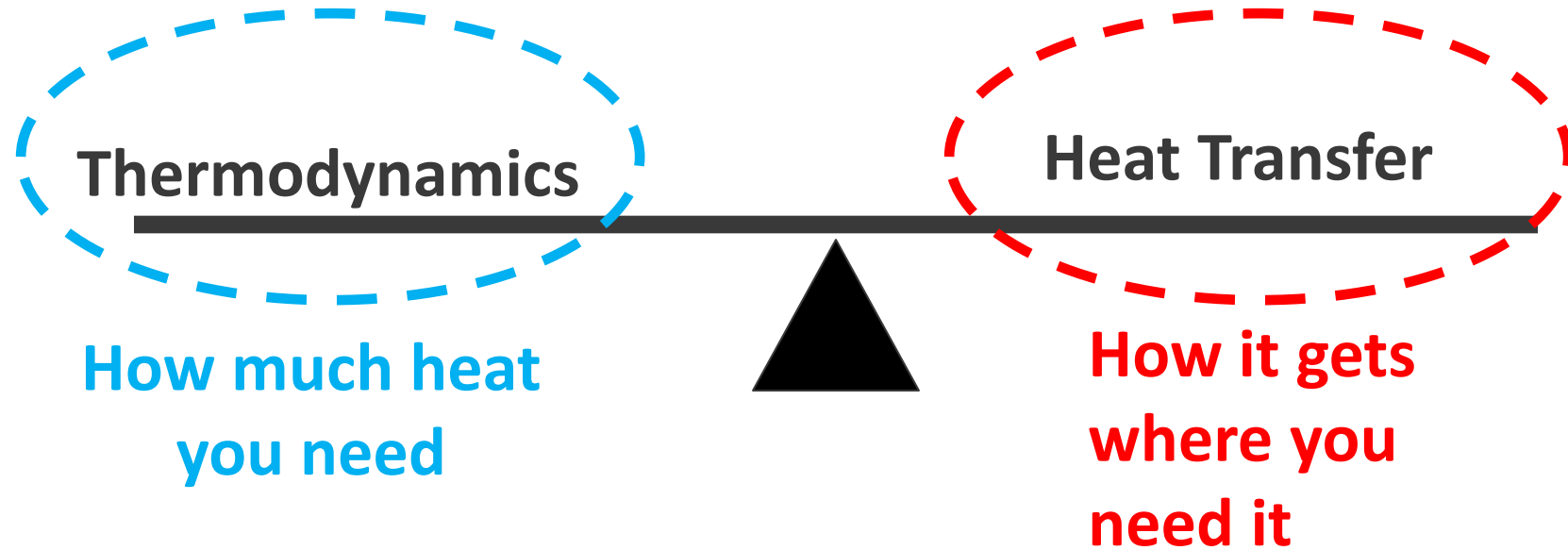
**CHALLENGES**

**ADAPT, INNOVATE**

What are the challenges?

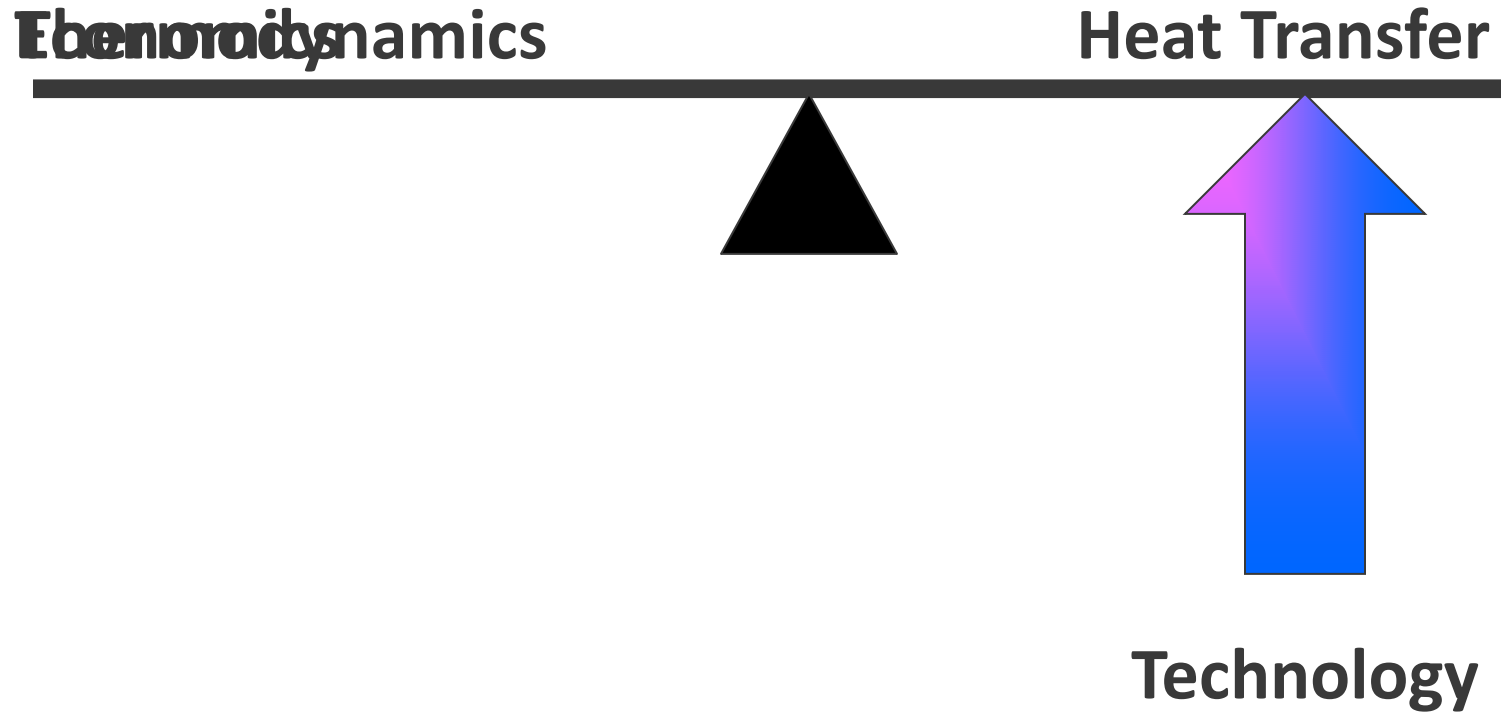


# Big Challenge: Balance “Thermo” and “Heat Transfer”



**Heat transfer ALWAYS wins...**  
**And its NOT in our favor.**

# Technology Drives the Balancing Effort

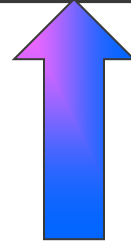
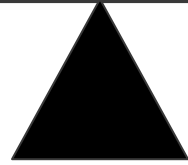


Helping heat transfer through technology

# First Technology... Flying

Economics

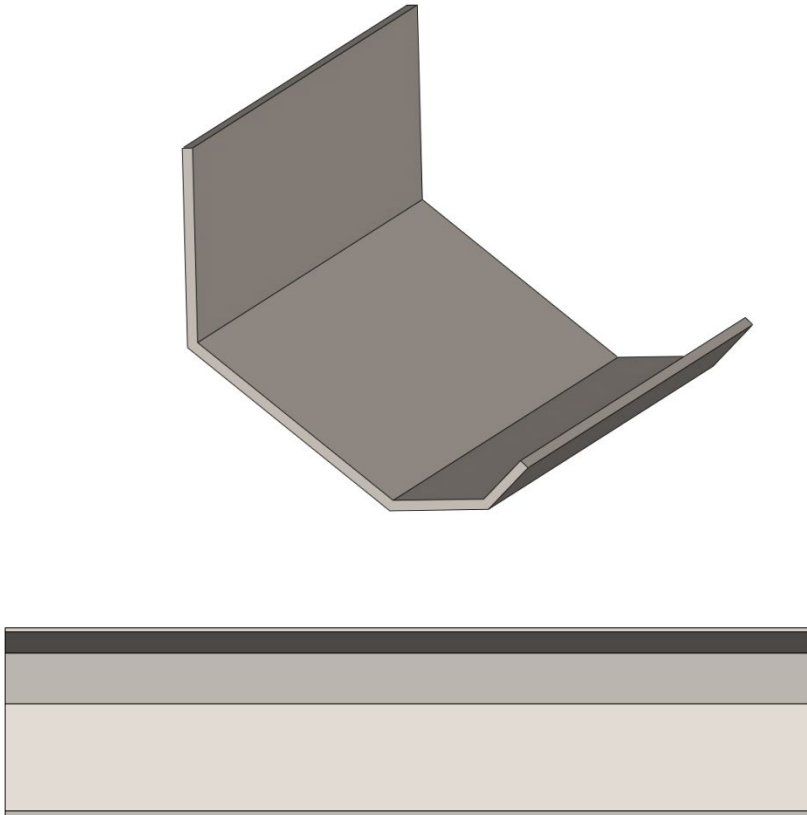
Heat Transfer



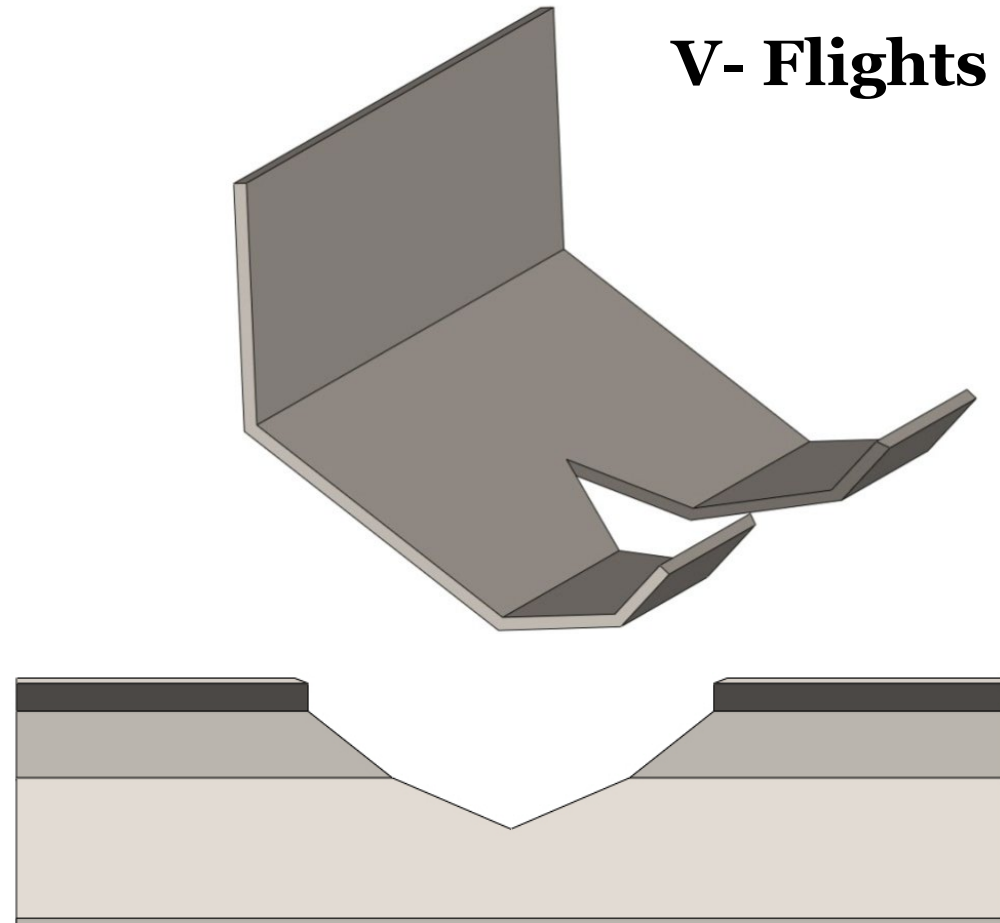
V-flights

# Flighting – Improving Heat Transfer in the Dryer

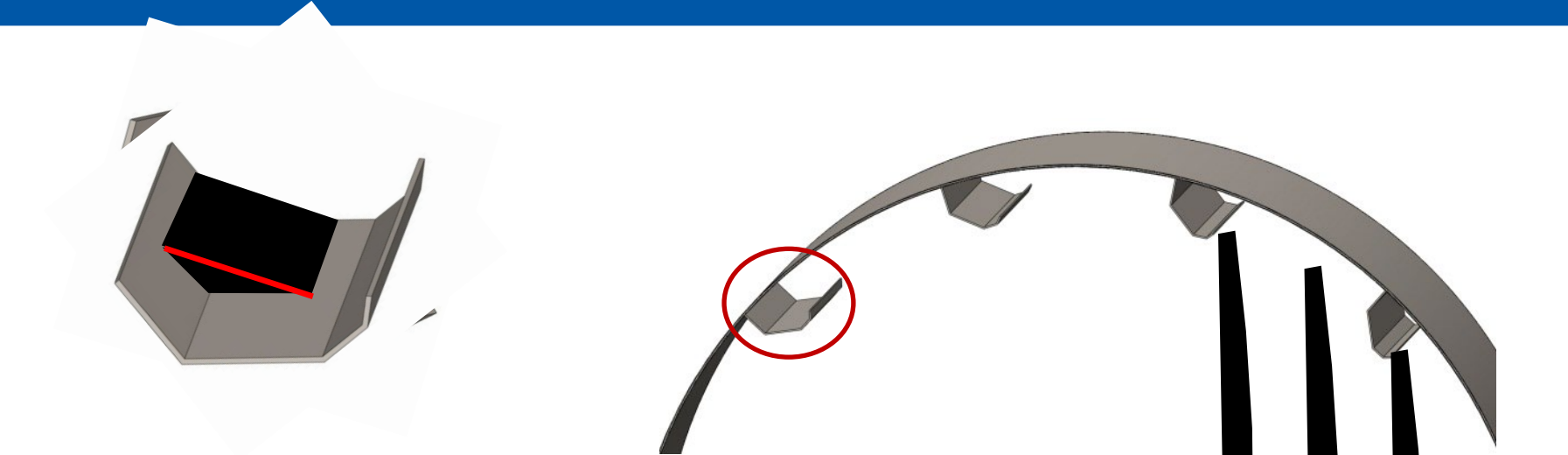
**Standard Flights**



**V- Flights**



# Flighting – Traditional Flights, Traditional Issues



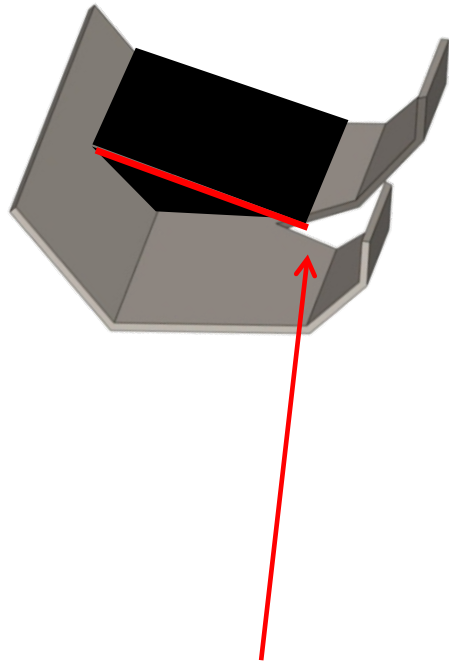
**Flight must rotate further before angle of repose reaches tip of flight**

**Hot gas bypassing occurs on this side of drum**

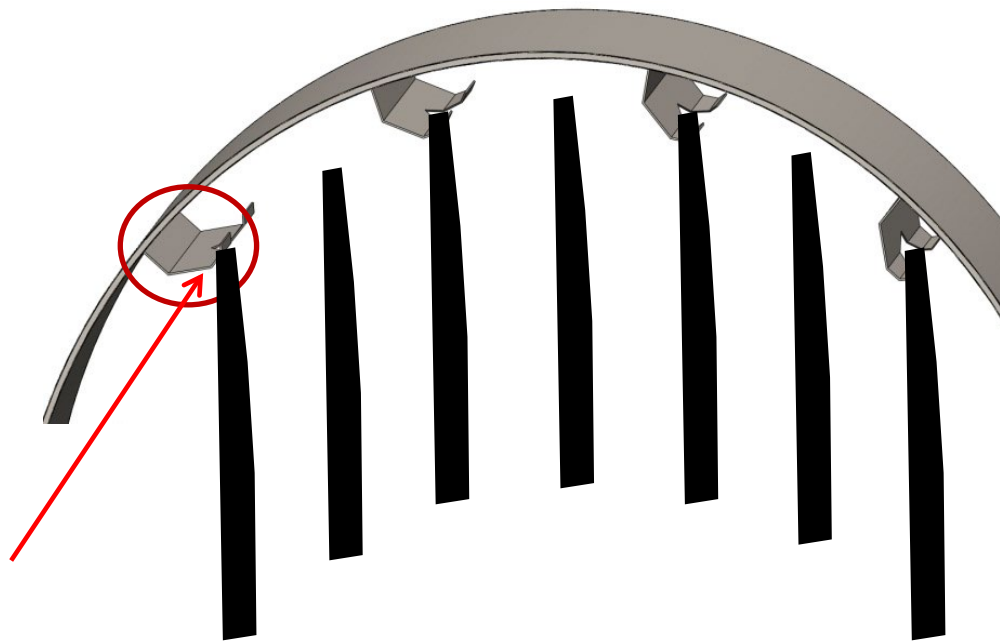
**Previous Flights – Tendency for Hot Spots**



# Flighting – Advanced Flights, Mitigate Issues



**Veiling through notch**



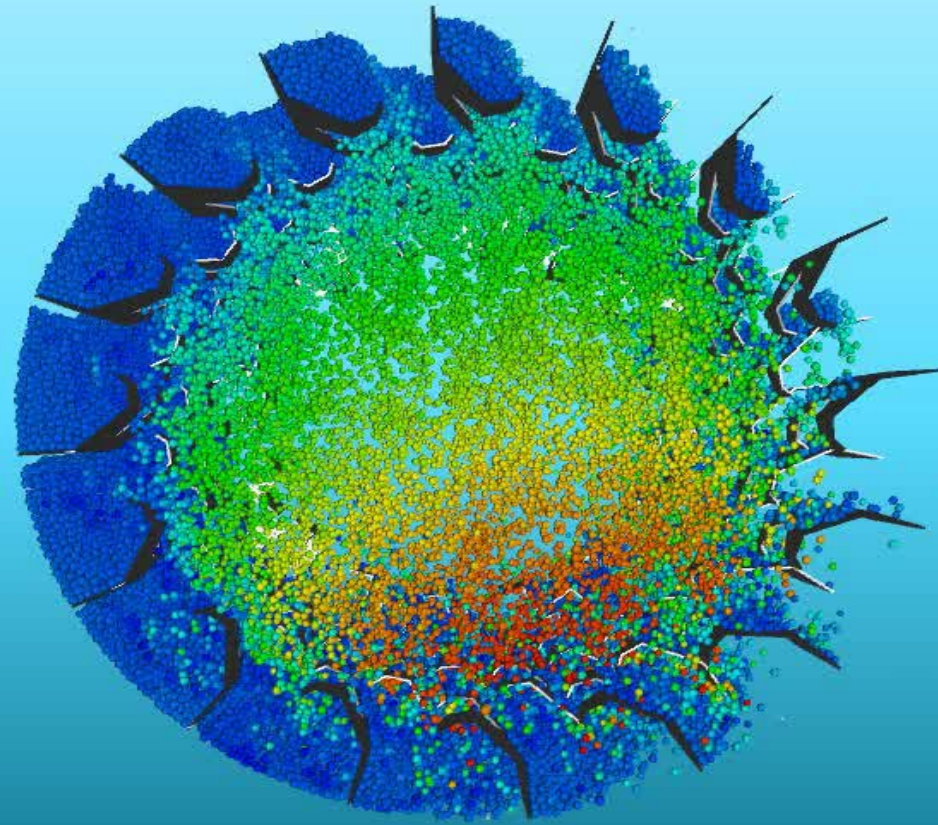
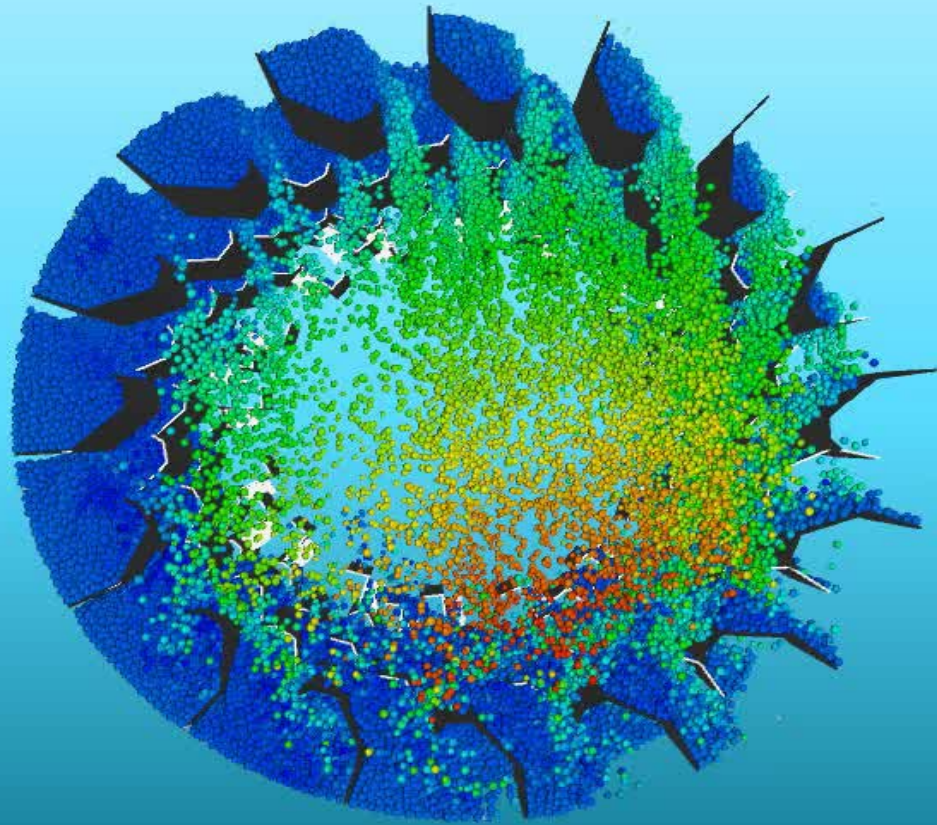
**Hot gas bypassing is eliminated**

**V-Flights – Minimize Hot Spots**

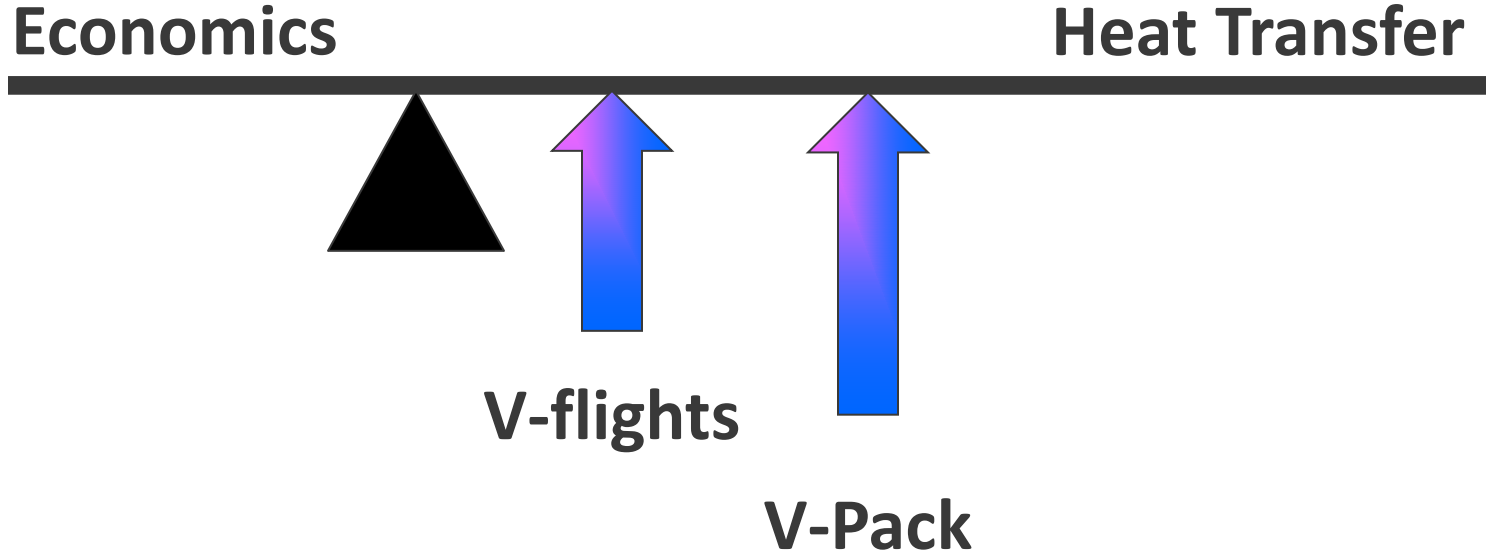


# Previous Flights

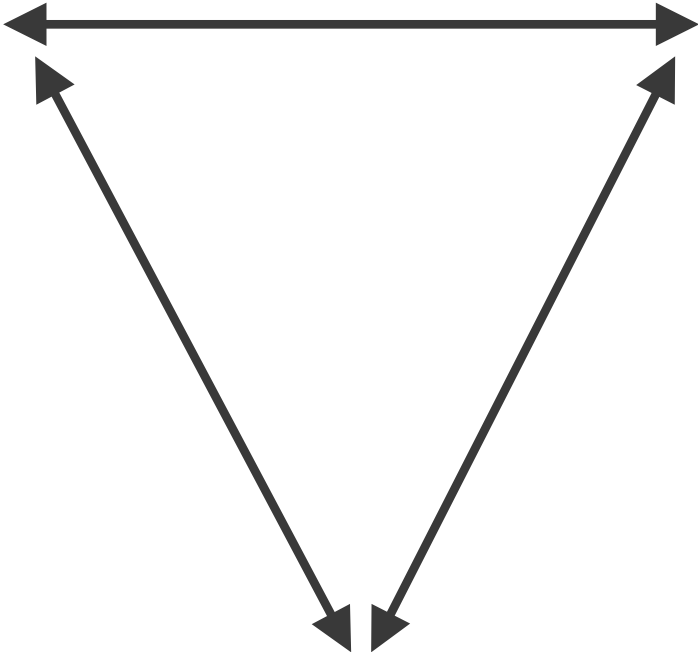
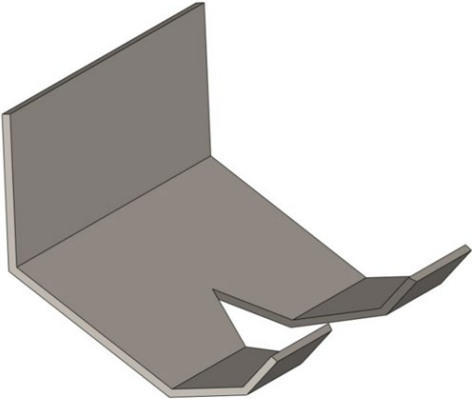
# V-Flights



# Second Technology... Drum VFD

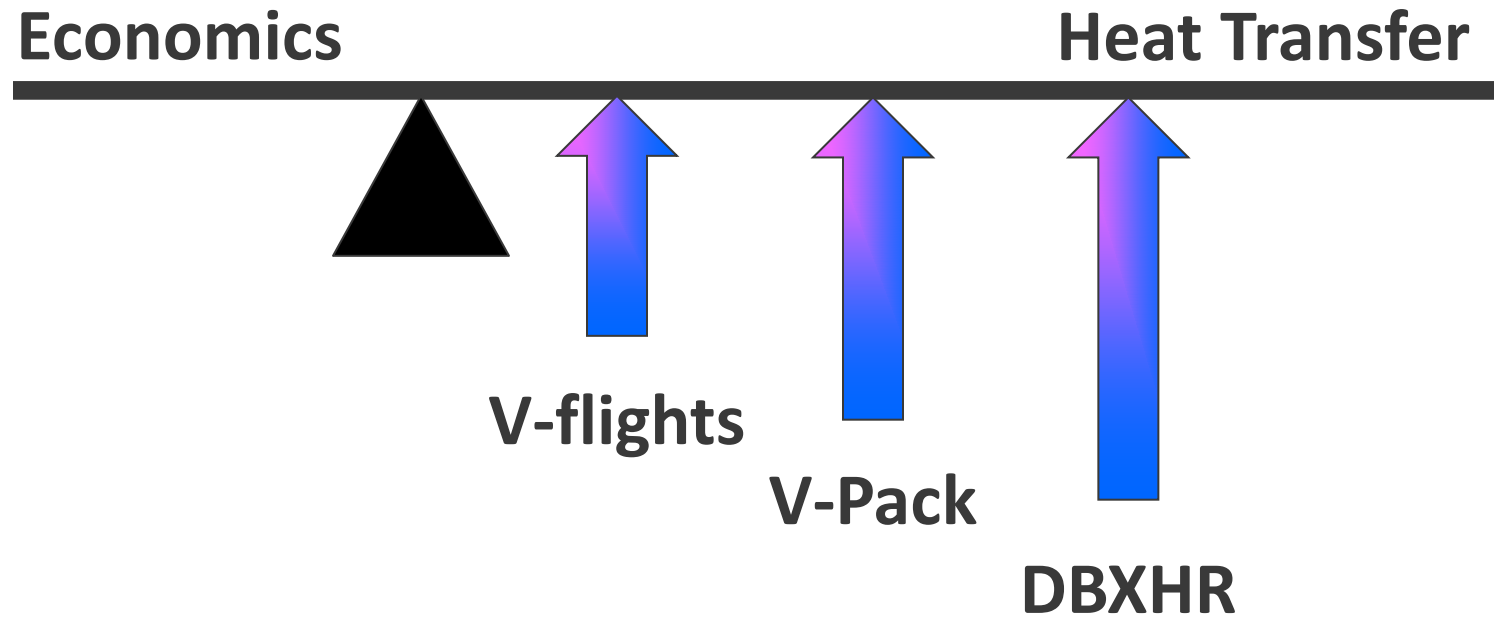


# V-Pac™ Stack Temperature Control

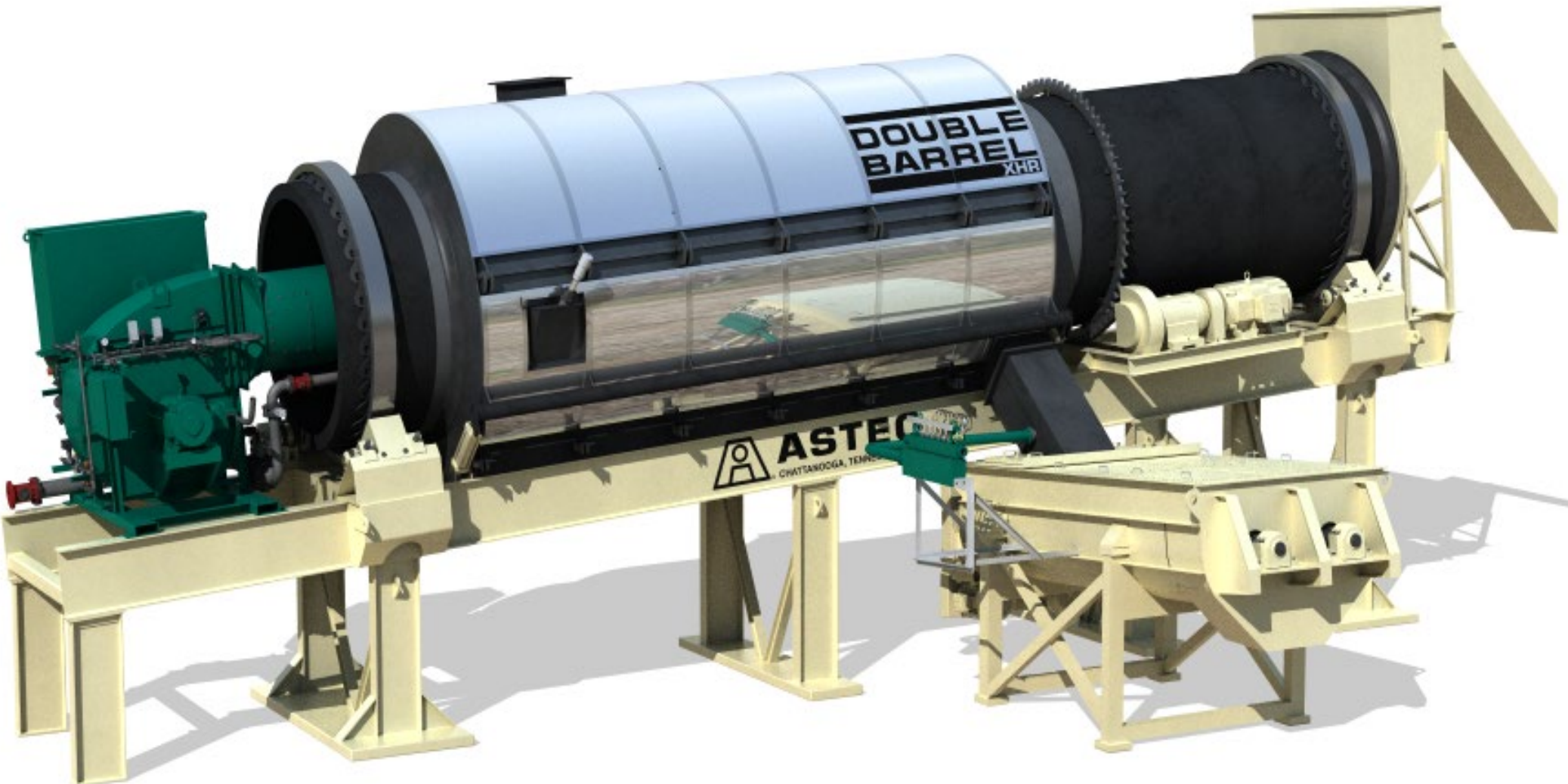


**Control Logic**

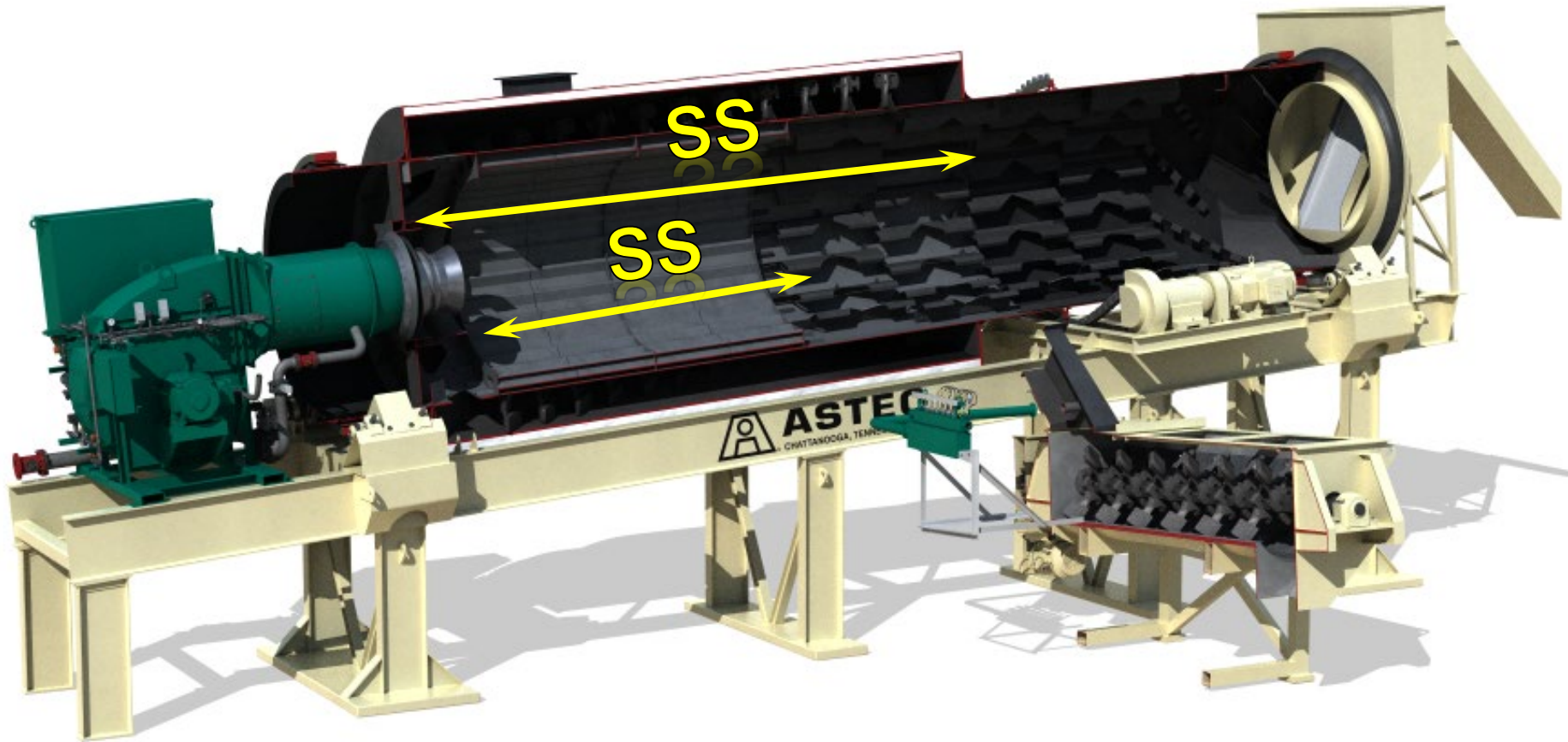
# Third Technology... Double Barrel XHR



# Double Barrel XHR



# Double Barrel XHR Key Features



**Shell and flights typically Corten, 1100°F (593°C)**

**Stainless, 1800°F (982°C) minimal oxidation**



# Predicting the Future?

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What MIGHT the HMA Plant of the Future be like?

Who knows the future?



# World Events and Trends Drive Design

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# Certainty: Increased Expectation of Sustainability



**Green**

**Less HMA. More WMA.**

**Recycle, Recycle, Recycle**

# Certainty: Increased RAP: NORM rather than EXCEPTION



## What MIGHT the HMA/WMA Plant of the Future be like?

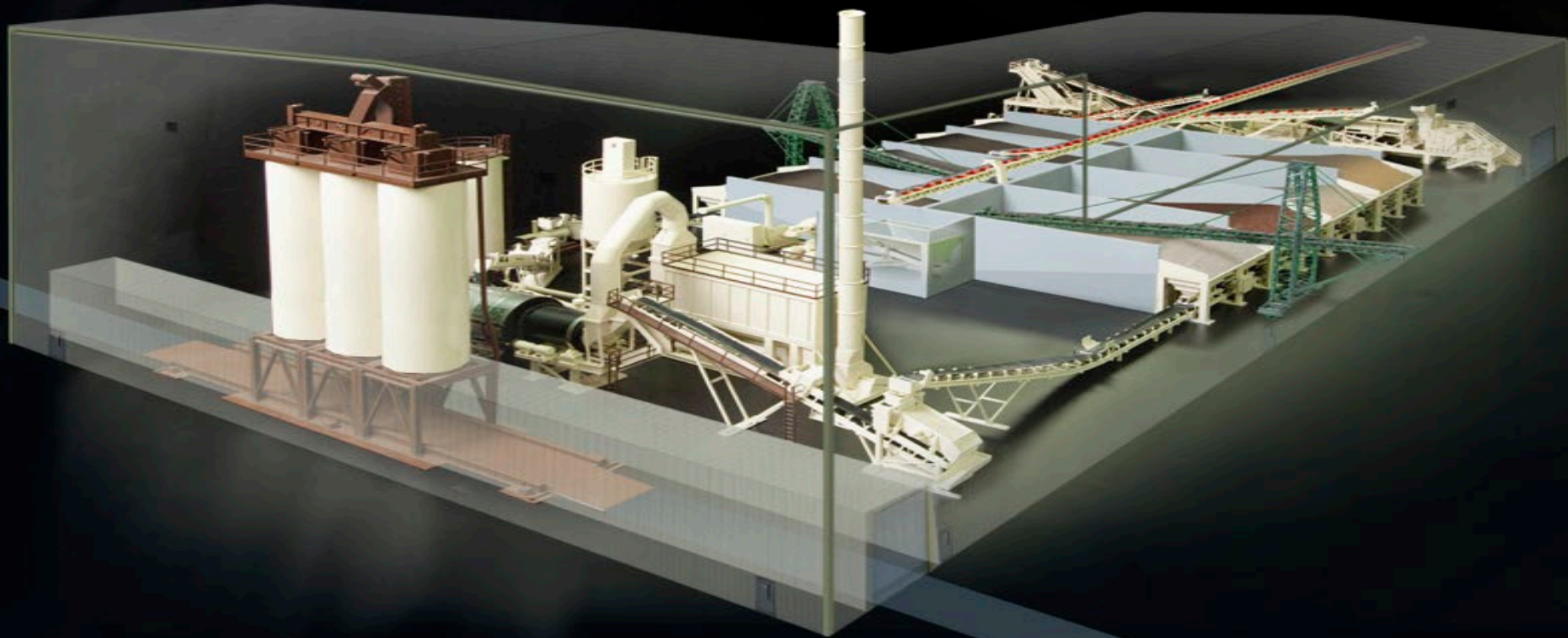
- Well-planned and landscaped industrial facility.
- Barely audible, if at all, to neighbors (Quiet)
- Most emissions greatly reduced or eliminated...
- More fuel efficient, less effective greenhouse gas emissions.

**Less impact...**

**Better neighbor.**



# Covered, Indoor Facilities?



# Covered, Indoor Facility (2013)



05/17/2013



# Covered, Indoor Facility (2013)



05/17/2013

# Interface to Outdoor Storage (Feed Bins)



# Interface to Outdoor Storage (Storage Bins)



05/17/2013



# What's Next?



We can safely predict...



**Less impact!!!**

**Better neighbor.**

**ALTERNATIVE FUELS  
EVEN HIGHER RECYCLE**

**PROCESS HEAT RECOVERY**

**HIGH RECYCLE**

**WHITE BINS, BLACK BINS**

**TECHNOLOGY APPLICATION**



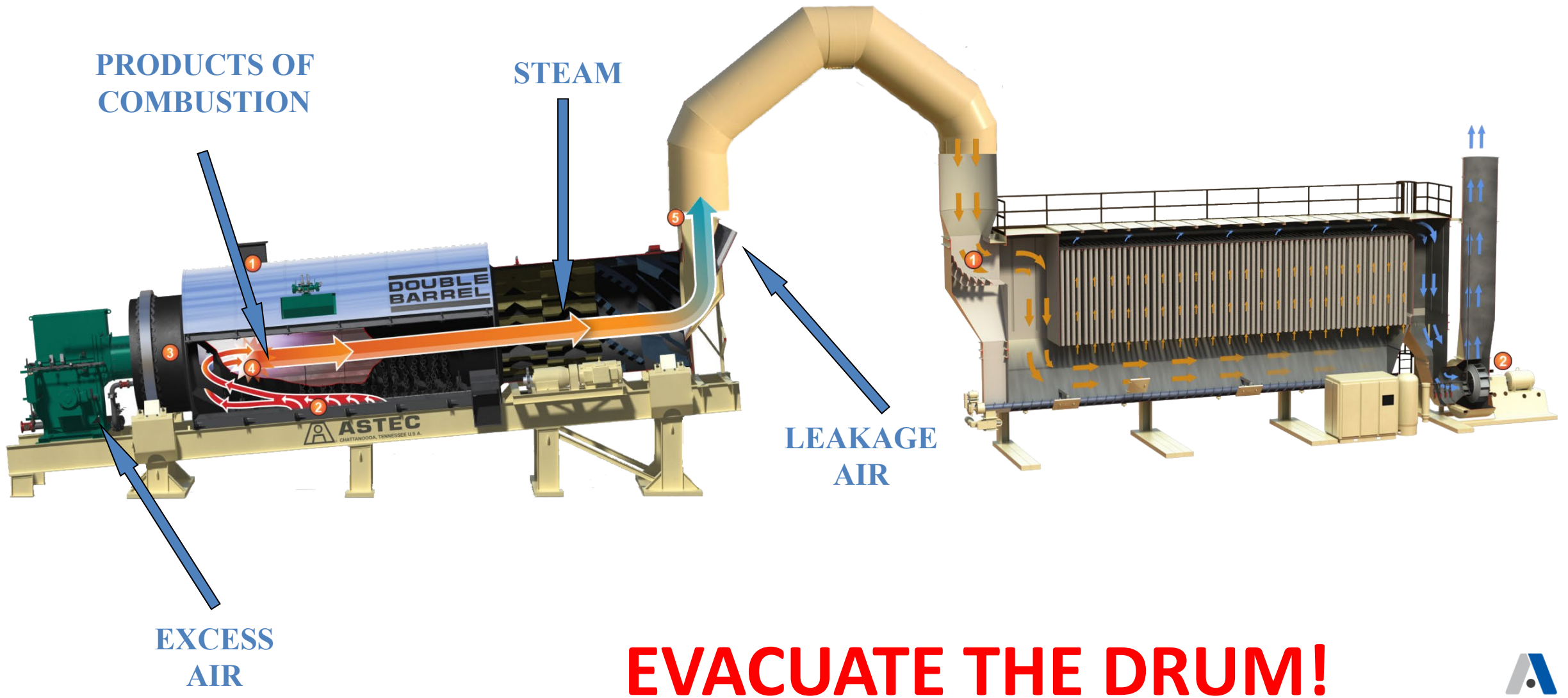


**PARTICULATE CONTROL  
& AIRFLOW**

# I THINK WHAT WE NEED IS A BAGHOUSE...



# What is the function of the exhaust system?



# Common Terms

**AIR-TO-CLOTH RATIO: GAS VELOCITY THROUGH THE BAG FABRIC**

**BLINDED: CONDITION OF REDUCED BAG PERMEABILITY**

**CAN VELOCITY: UPWARD GAS VELOCITY IN THE HOPPER BELOW THE BAGS**

**DIFFERENTIAL PRESSURE: DIFFERENCE IN PRESSURE BETWEEN TWO POINTS IN SYSTEM; A.K.A. "PRESSURE DROP"; CAN BE MEASURED IN inWC OR mmHG**

**DUST CAKE: BUILDUP OF PARTICULATE MATTER ON OUTSIDE OF BAGS**

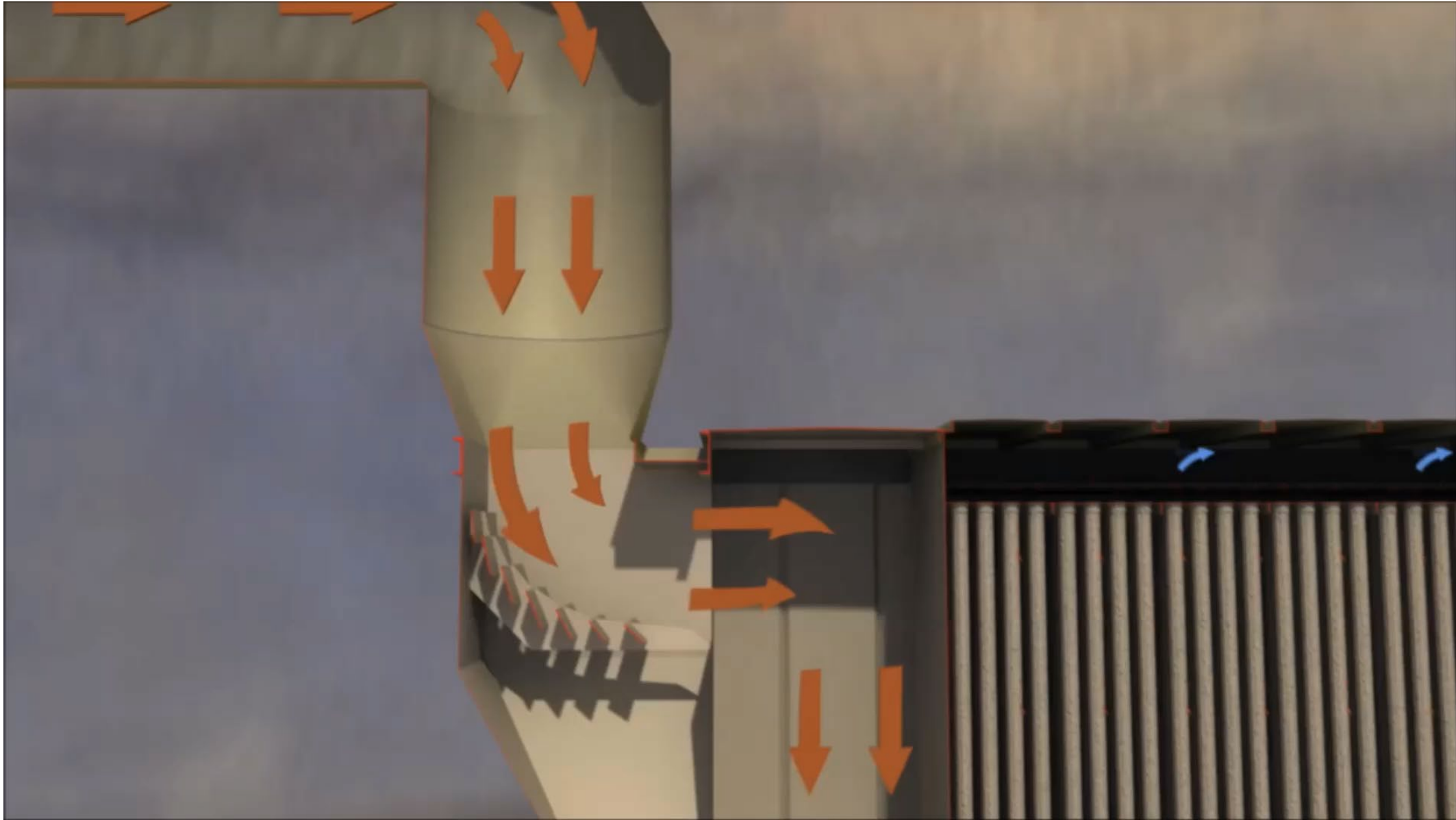
**GRAIN: UNIT OF WEIGHT EQUAL TO 1/7000 OF A POUND**

**INTERSTITIAL VELOCITY: UPWARD GAS VELOCITY BETWEEN BAGS MEASURED AT BOTTOM OF BAGS**

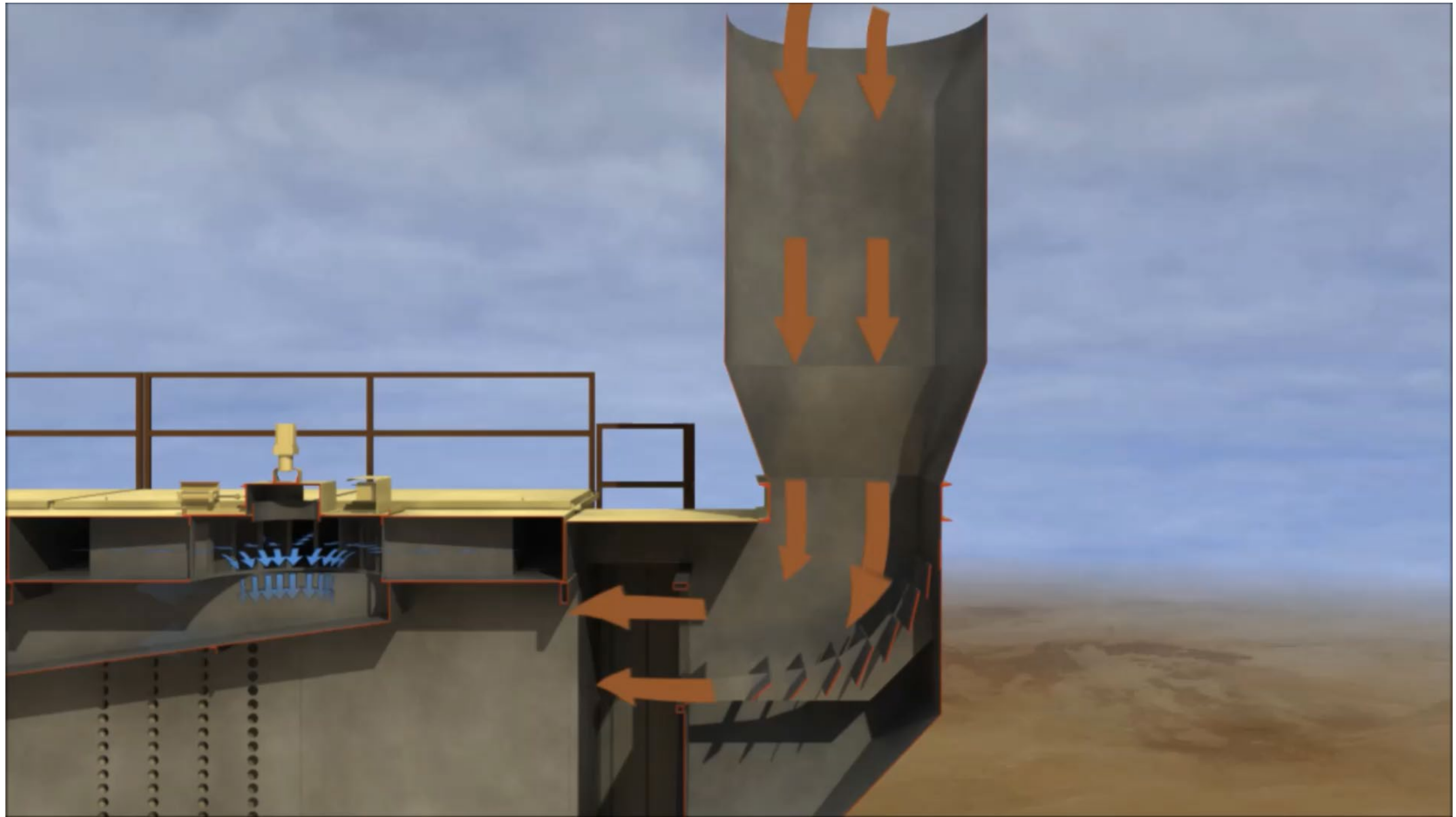
**RE-ENTRAINMENT: RE-DEPOSITING OF DUST ONTO ADJACENT BAG AFTER PULSING**



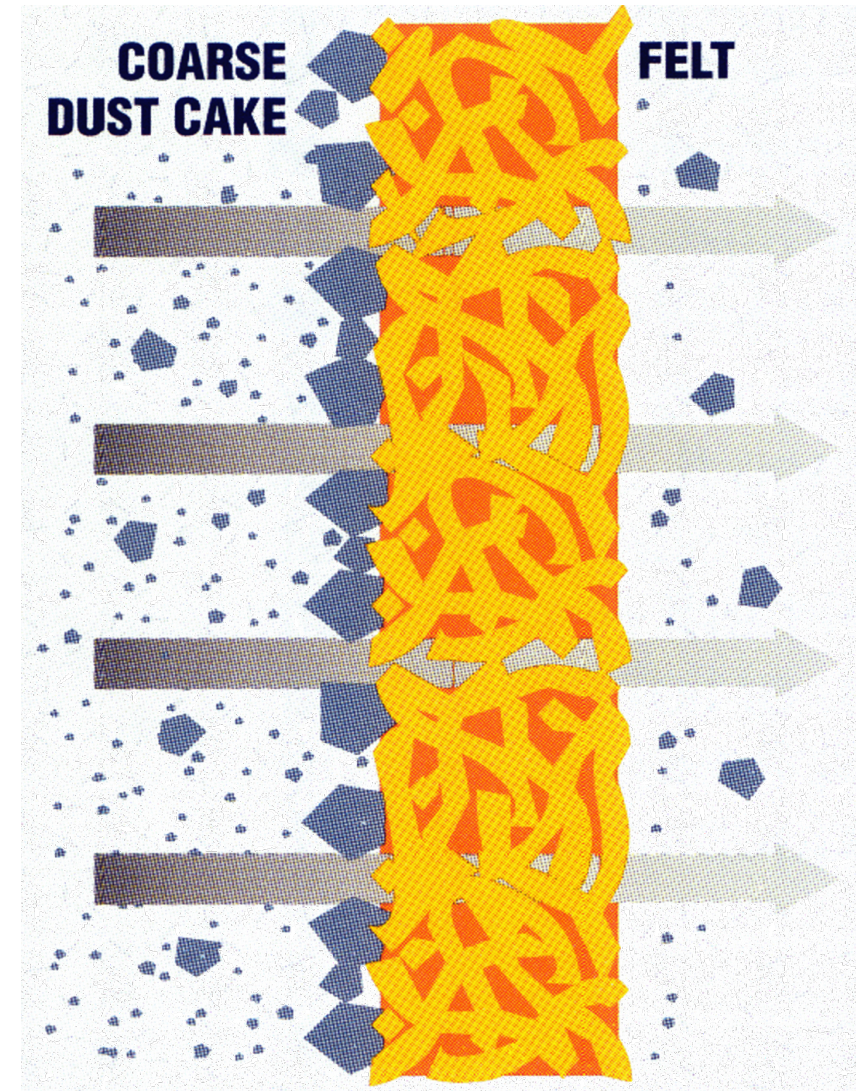
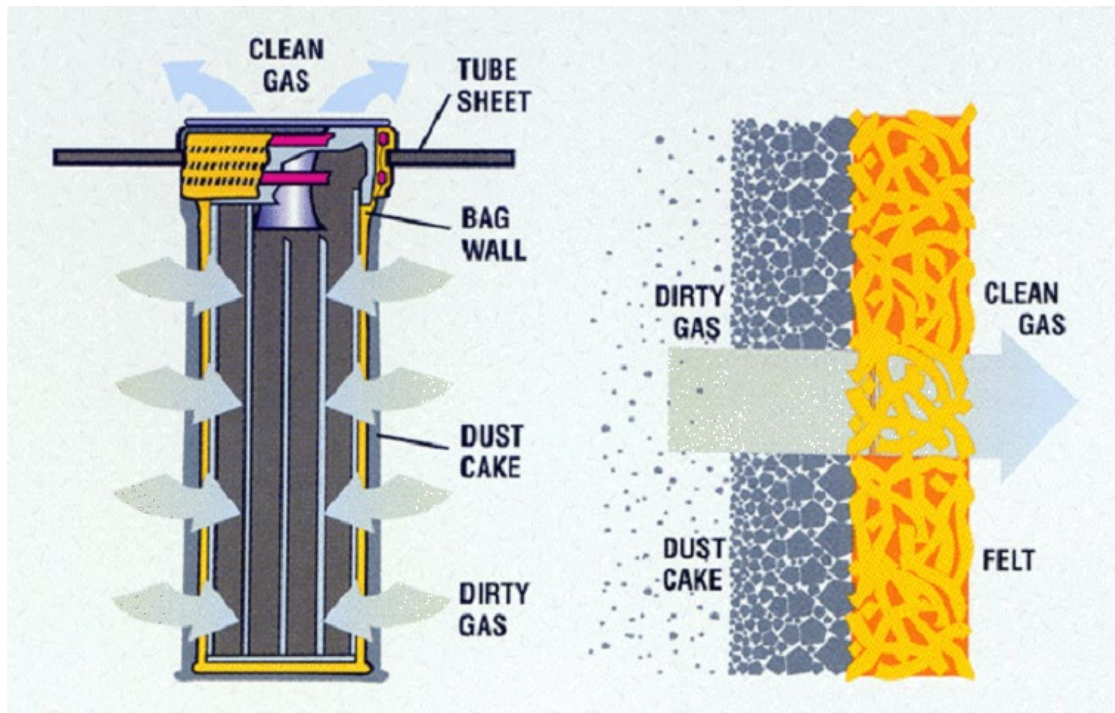
# Pulse Jet Baghouse Operation



# Reverse Pulse Baghouse Operation



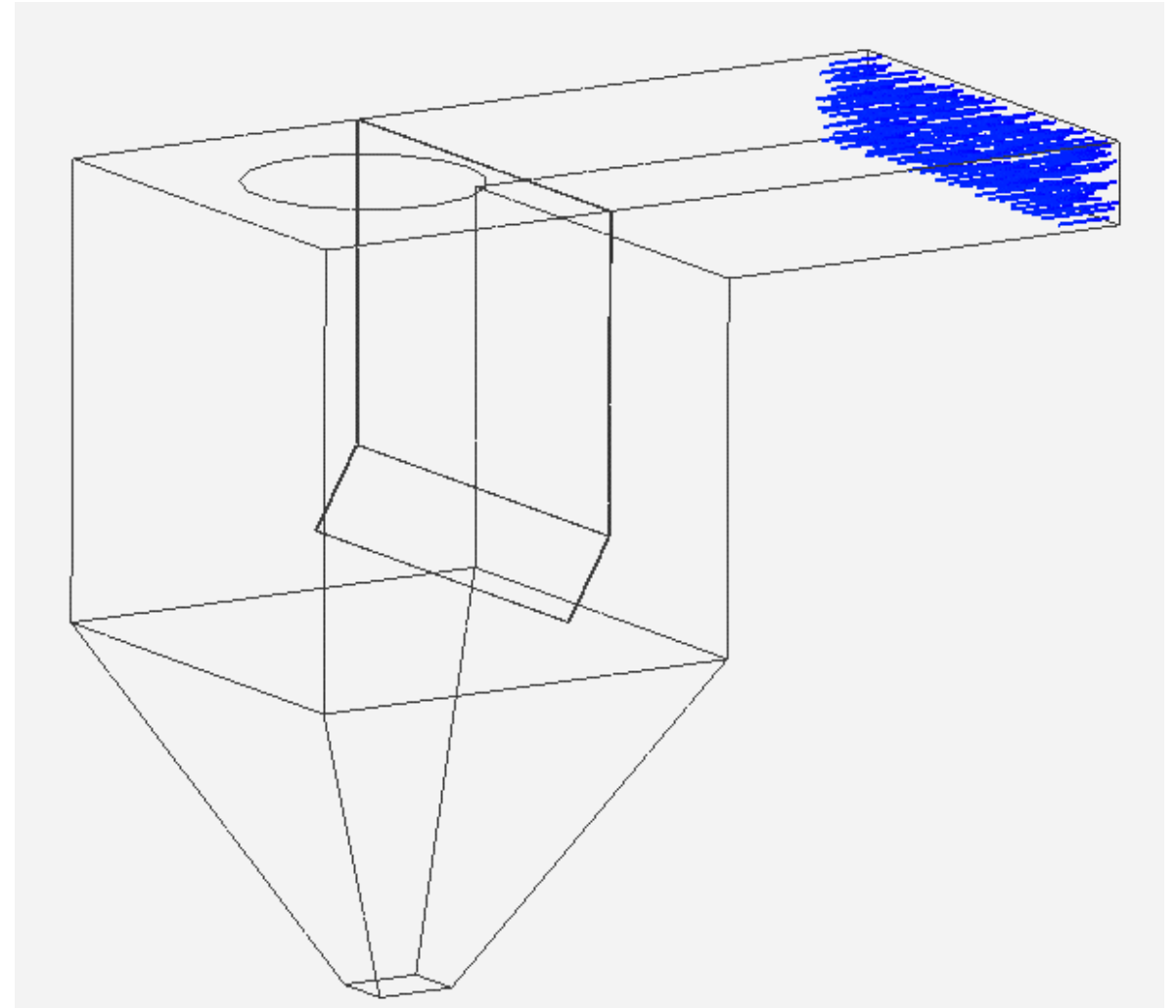
# DUST CAKE FUNCTION



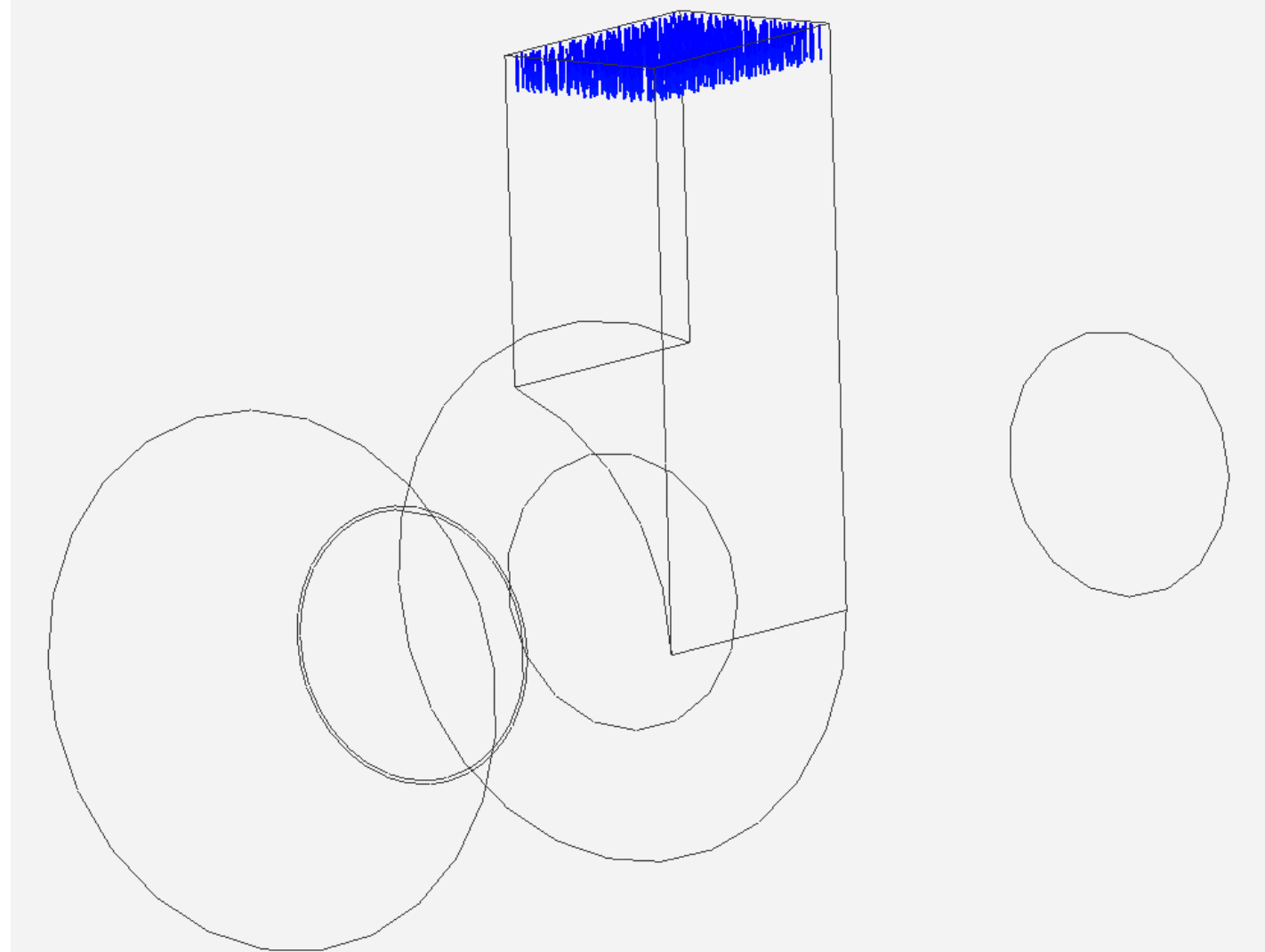
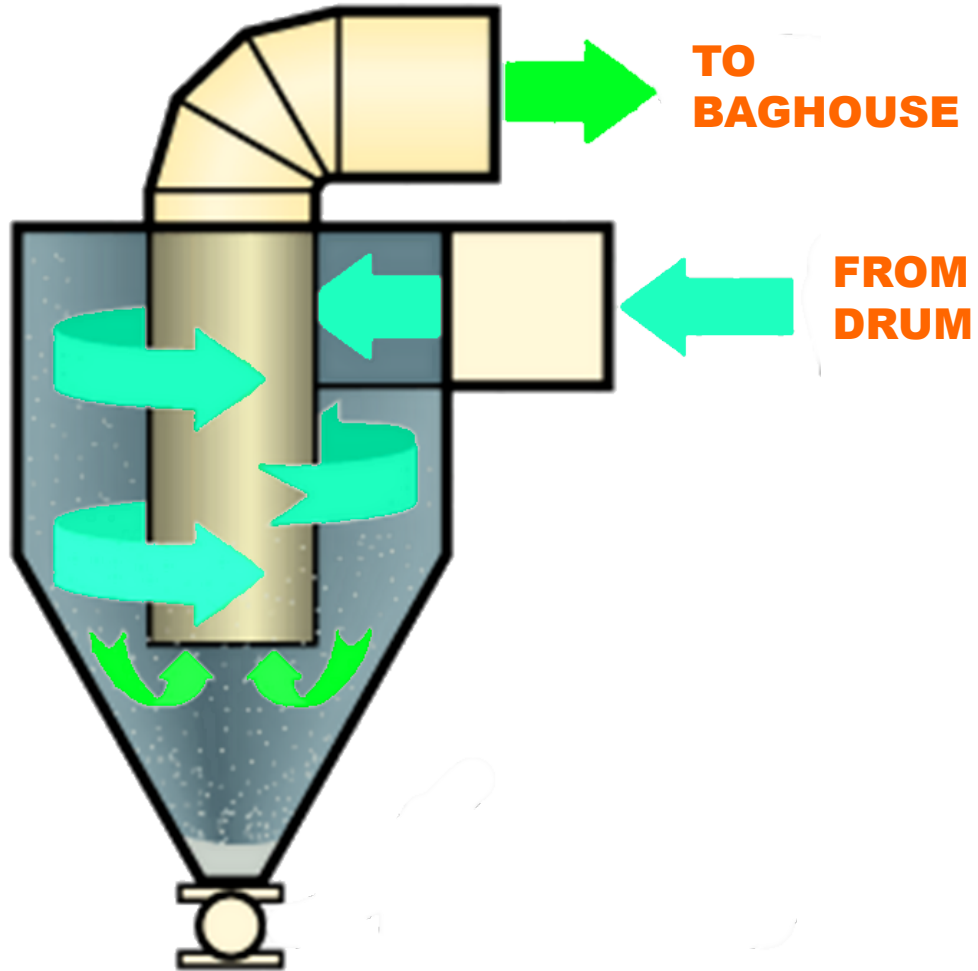
# Primary Collectors: Knockout Box



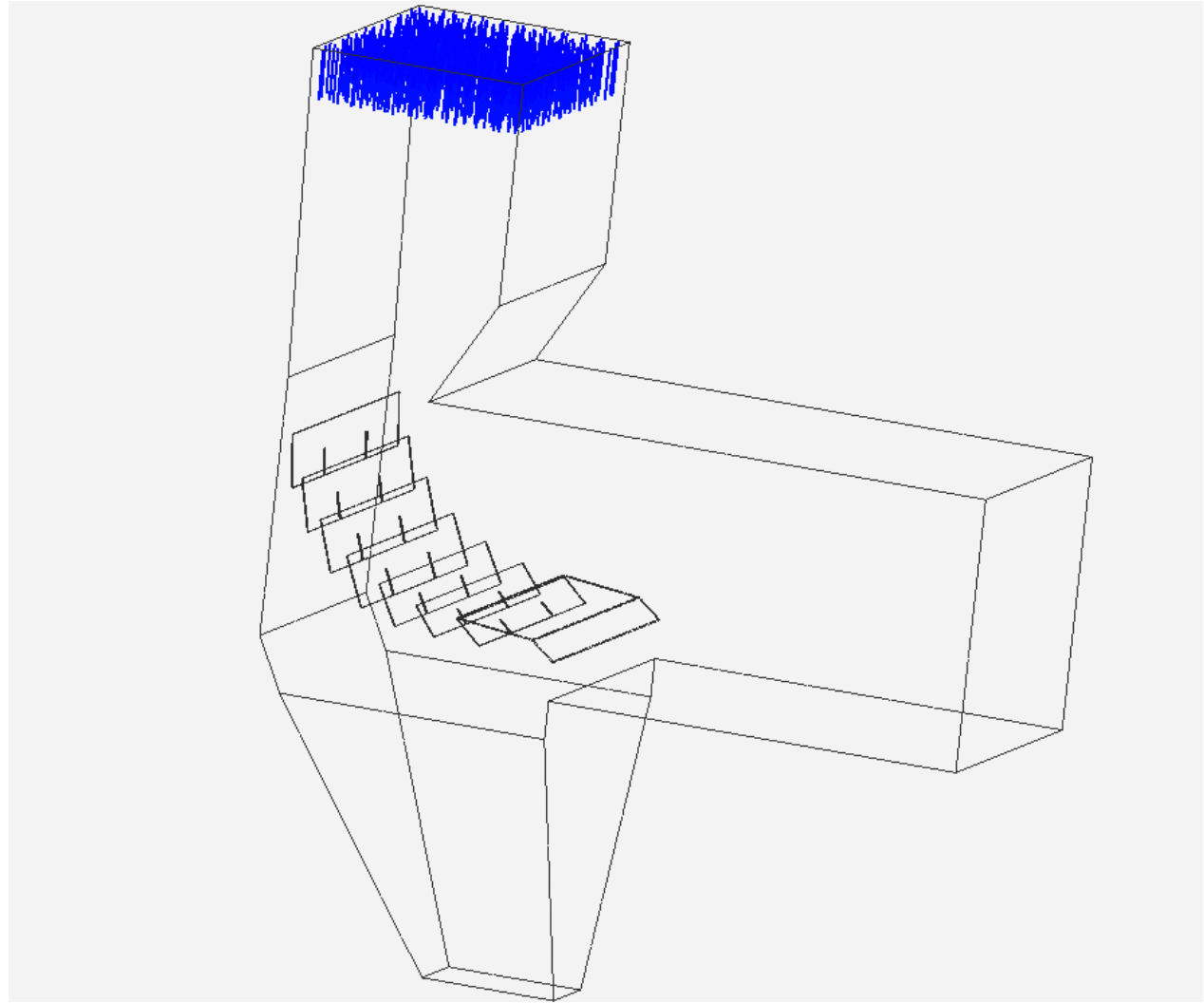
- Low internal gas velocities
- Effective for removal of large particles only
- May have baffle plate to enhance particle removal



# Primary Collectors: Cyclones



# Primary Collectors: Inertial Separator



# Let's Talk Felts...



Dust carryout:  
up to **10%** of  
production rate!

**What's the big  
deal?**

**BAGHOUSE  
PERFORMANCE!**

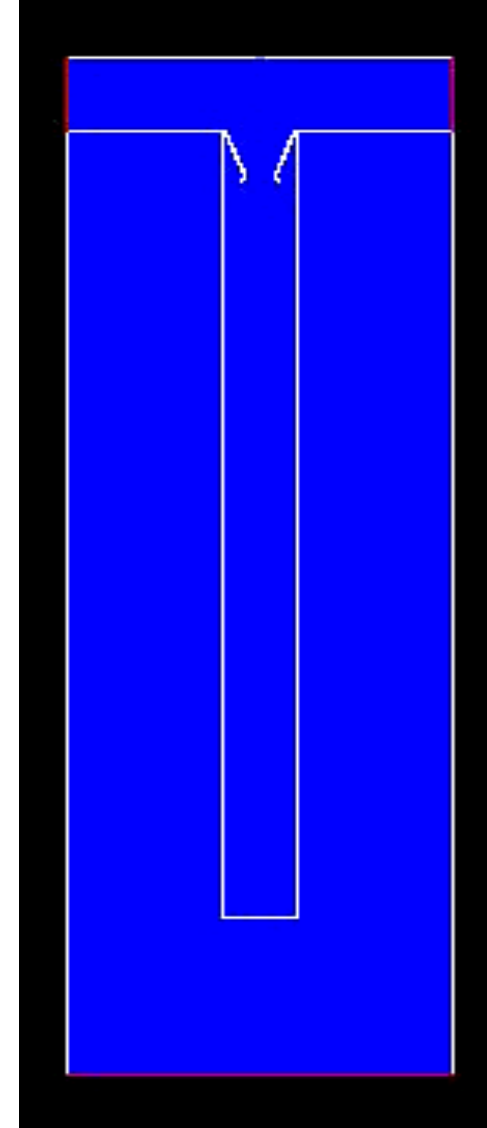


# Let's Talk Felts...

**When in doubt... Keep it low!**

- Over-cleaning reduces bag life !**
- Aggressive pulsing breaks up dust cake**
- Maintain adequate dust cake thickness: 3-5inWC**

**It's better to pulse more often at a lower pressure!**



# Let's Talk Cleaning...



- **Blowpipes must properly align with the bags**
- **Inspect holes annually for deformation**
- **Use only dry, compressed air**

# Mudballs



- **High Baghouse  $\Delta P$**
- **Low Exhaust Temps**

**BAD  
DAY!!!**

# HYDROCARBON CONTAMINATION



LIQUIDS DON'T BURN – ONLY  
VAPORS BURN.



# BLINDED BAGS

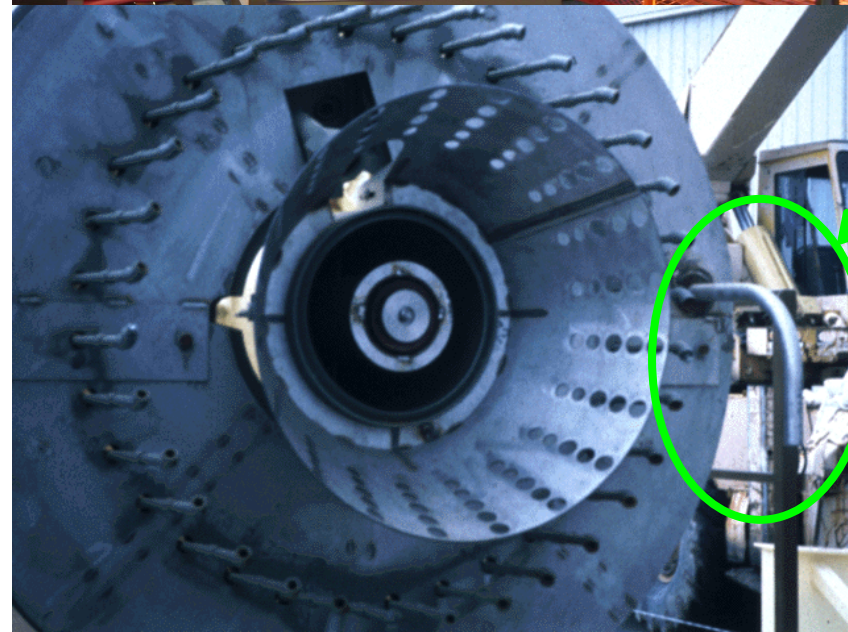
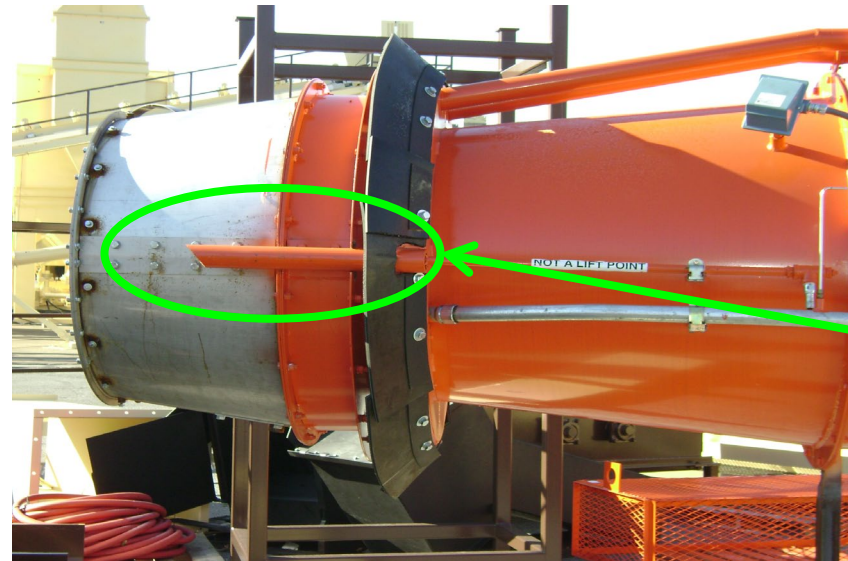


## CRITERIA:

- BAG WEIGHT *DOUBLE* THAT OF NEW FELT AFTER CLEANING
- *PERMEABILITY* < 2 CFM AT 0.5 INWC
- *DUST PENETRATION* > 50% THROUGH FELT

# BURNER SUCTION

Rule of Thumb  
Burner Suction  
Set Point



# Assessing Evidence of Corrosion



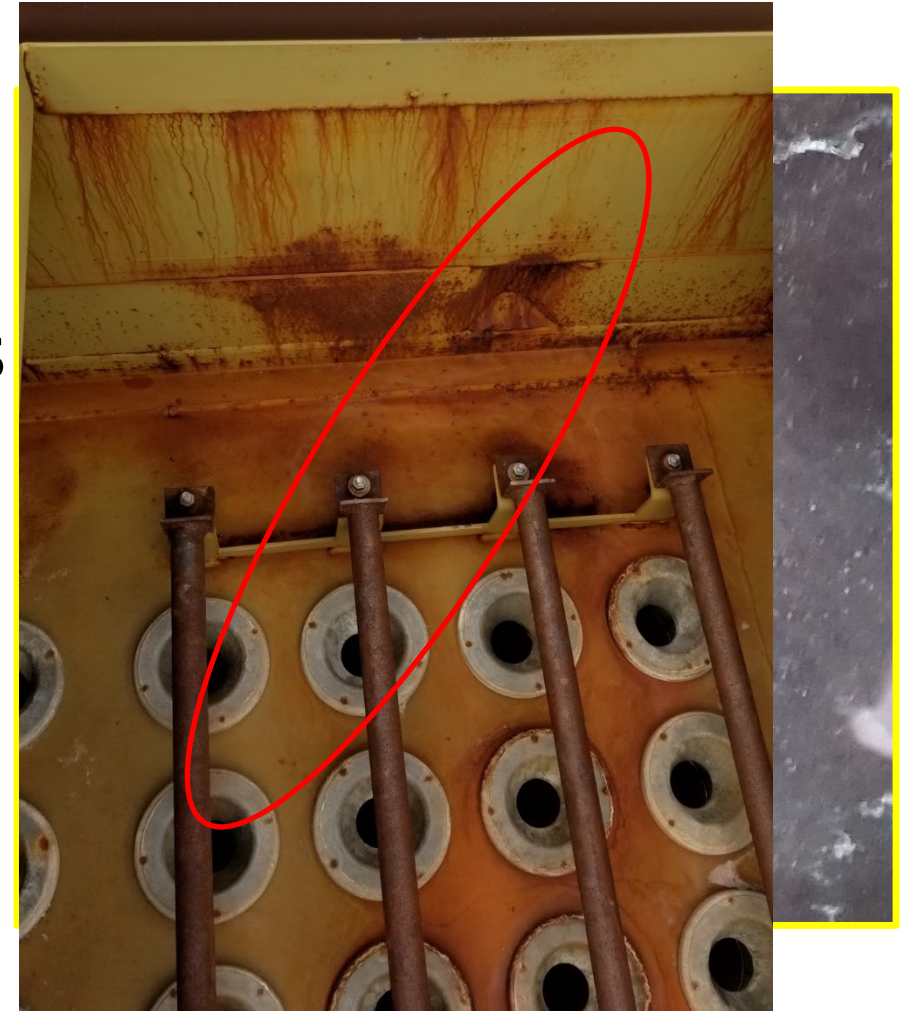
**Non-Critical**  
But how do we  
know which is  
which?  
**Critical Corrosion**



# Differences in Corrosion Severity



What differences do you see with these two photos?



# Corrosive Residues

**Sulfur** residues have a similar, but yellow appearance  
Chloride residues have a chalk white appearance



# Non-Critical Corrosion



- Typically has causes that are *more* easily fixed such as:
  - Low stack temperatures
  - Baghouse leaks in the form of:
    - Deteriorated Door Seals
    - Broken or cracked welds
- The corrosion in the baghouse shown here was solved by removing flights in the drum, and increasing the temperature in the baghouse by roughly 30 degrees.
  - The customer typically saw aggregate moistures near 8-10%

# Critical Corrosion



- Typically has causes that originate from somewhere other than the baghouse itself.
  - Corrosive compounds from various sources:
    - Asphalt Cements
    - Aggregates
    - RAP
    - Additives
    - Fuels
- White / Yellow residues are a tell-tale sign of critical corrosion.
- Critical corrosion needs to be solved at the source of the corrosion, not by simply modifying baghouse temperature.

# Abrasion



# Severe bag leaking



This should  
throw a **RED**  
flag.

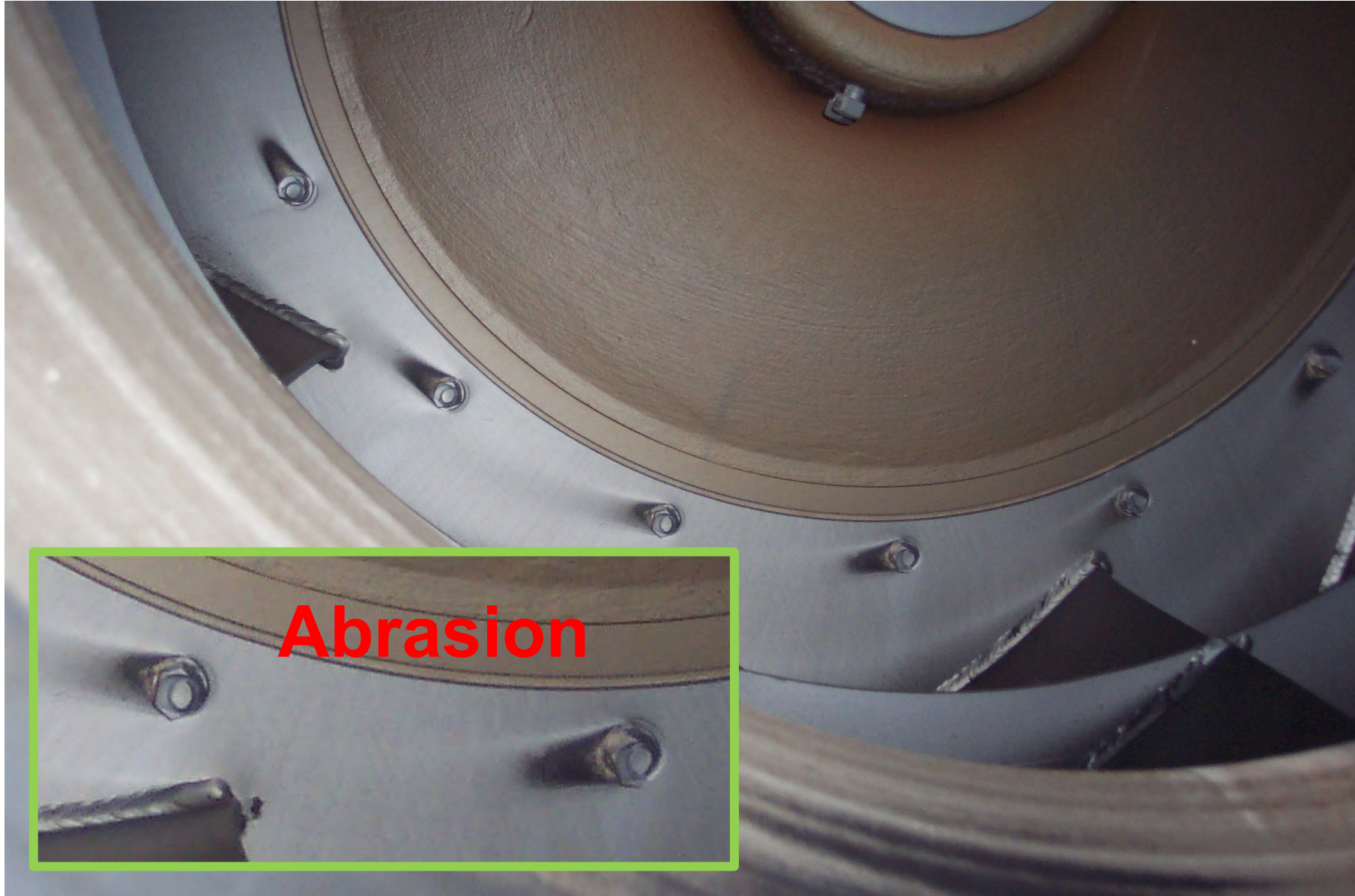
What else  
should you  
inspect?

# Severe bag leaking



Inspect  
the  
Fan  
Wheel!

# Severe bag leaking





# Dust Control Options

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BUILT TO **CONNECT**

Lafarge Seminar  
May 16-17, 2022



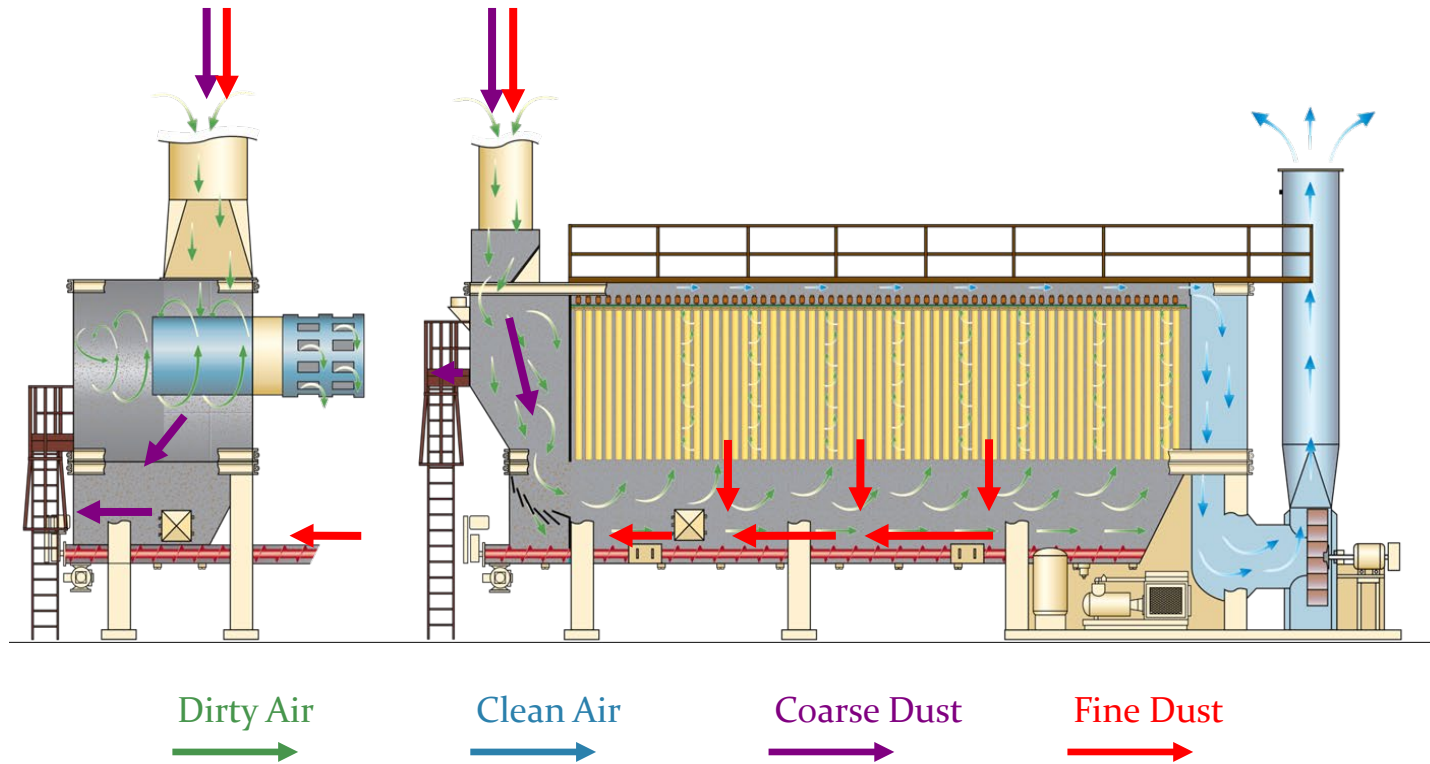


## Available Options

Astec currently offer six distinct dust control scenarios:

- Automatic Control
- Split Return with Weigh Pot
- Split Return
- Split Return with Surge Pot
- Return All with Surge Pot
- Return All

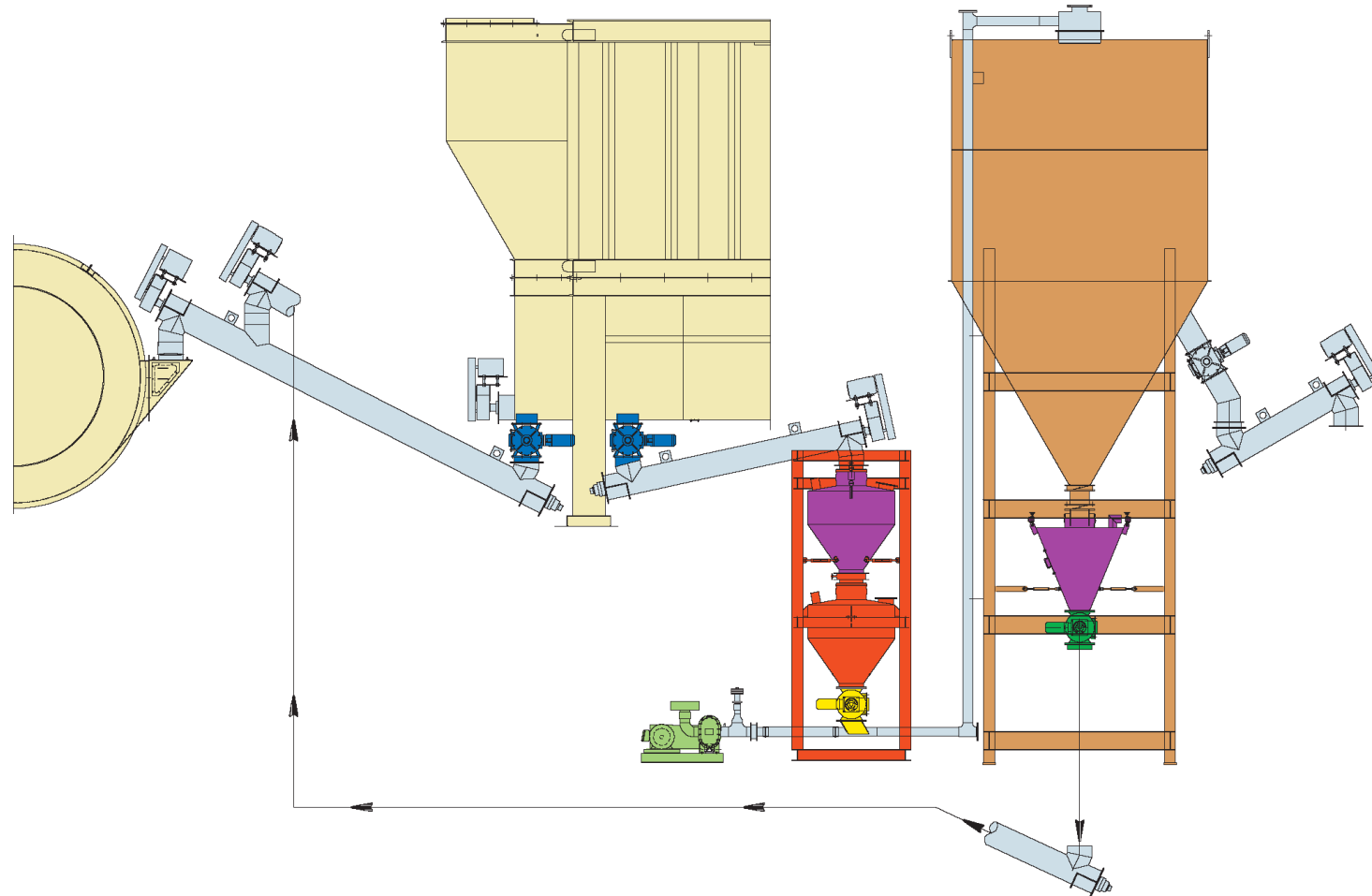
# General Airflow and Dust Flow



# Option 1 – Automatic Control



Commonly referred to as “Illinois run-around System”



# Option 1 – Automatic Control

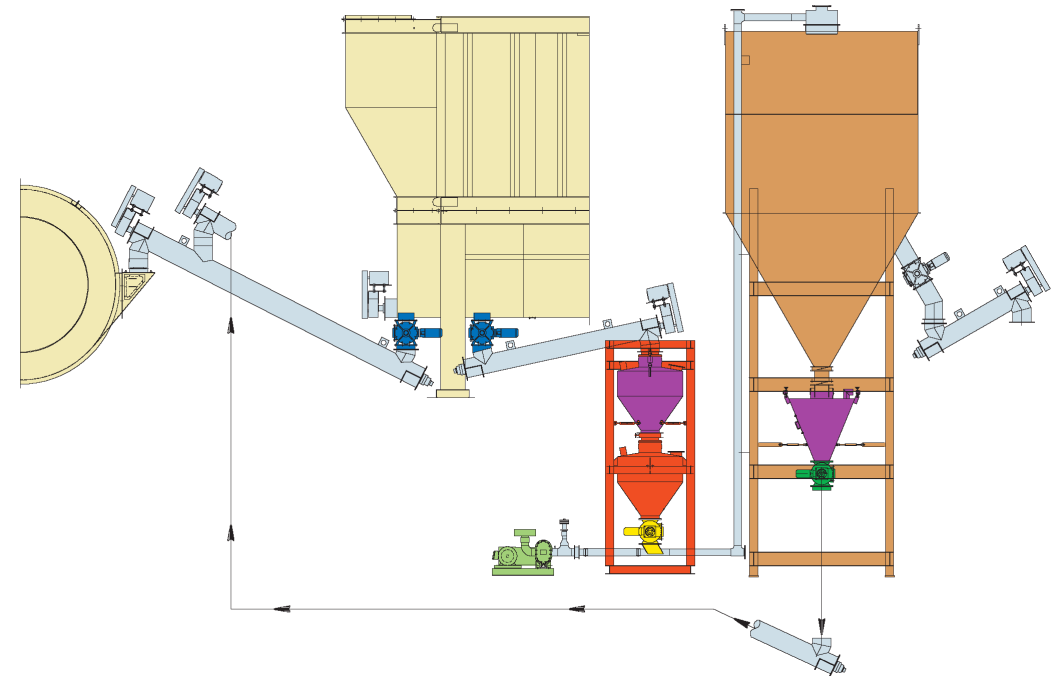


## Advantages

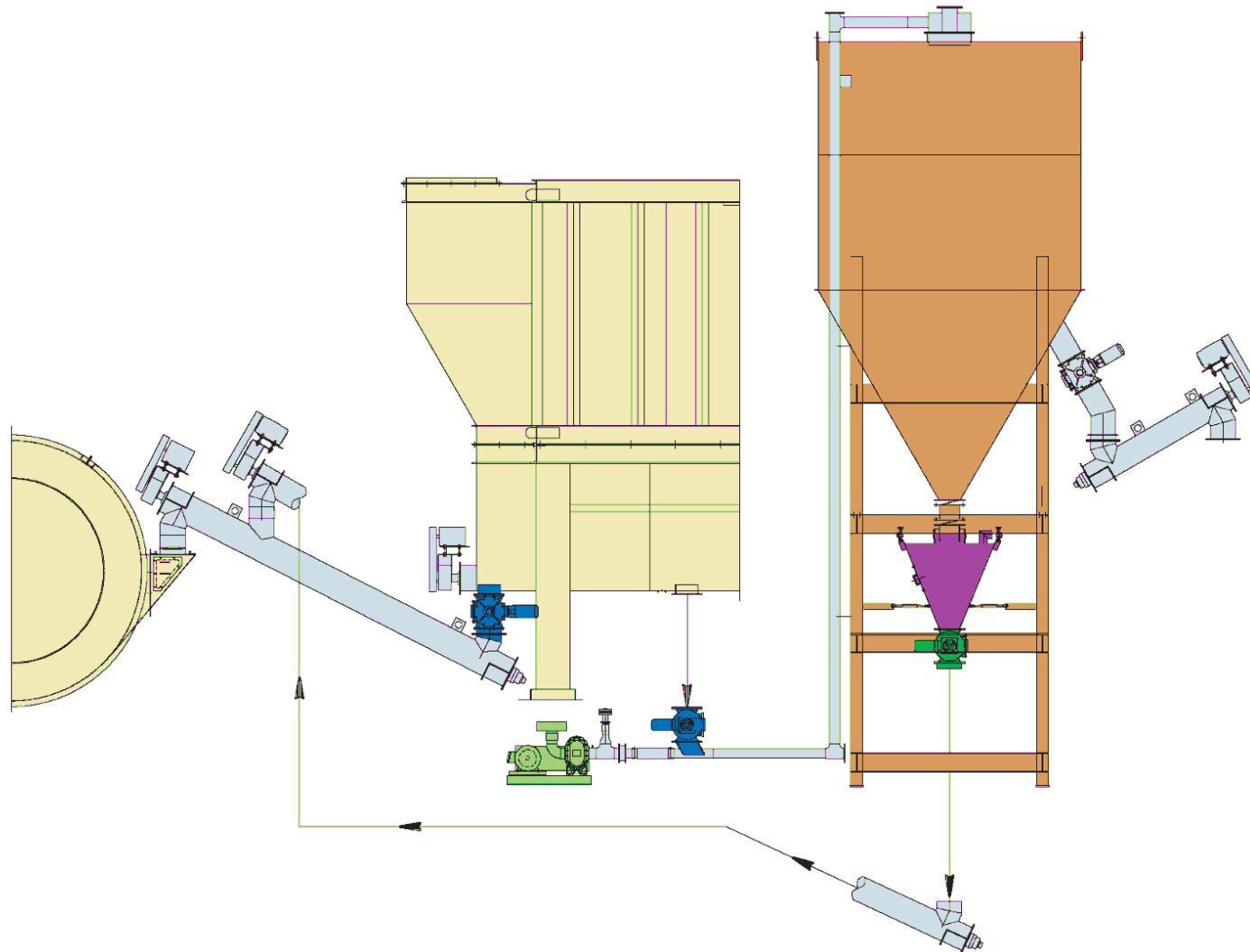
- Only system that ACCOUNTS for ALL dust in system to automatically calculate required AC content
- Weighing of fine dust leaving baghouse provides amount of fine dust needed for return
- AC flow is automatically adjusted based on measured change in fine dust component
- More dust can be added than is removed, if needed, because of silo
- Ensures steady dust flow from baghouse at start up and mix design transitions

## Disadvantages

- Highest cost
- Most complex



# Option 2 – Split Return w Weigh Pot



# Option 2 – Split Return w Weigh Pot



## Advantages

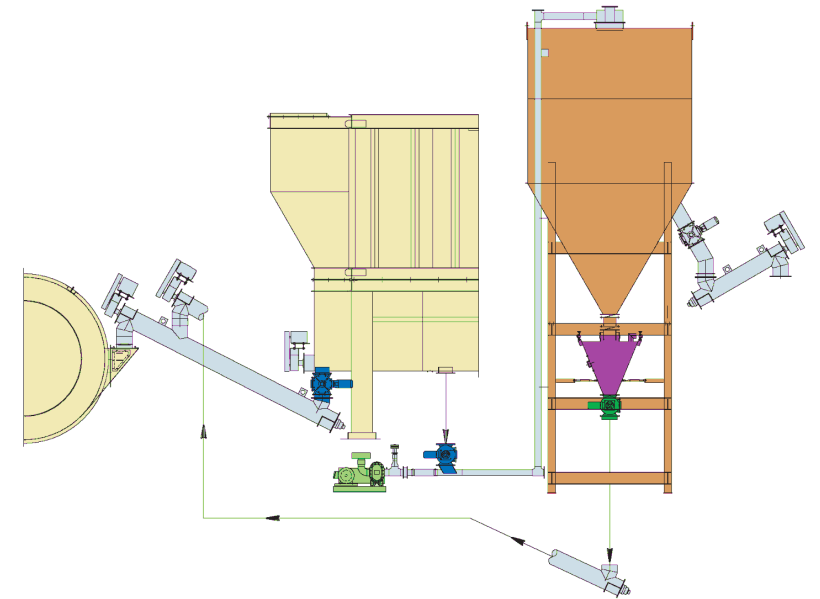
- Allows for wasting of dust if aggregate blend cannot meet specifications
- More dust can be added than is removed, if needed, because of silo

## Disadvantages

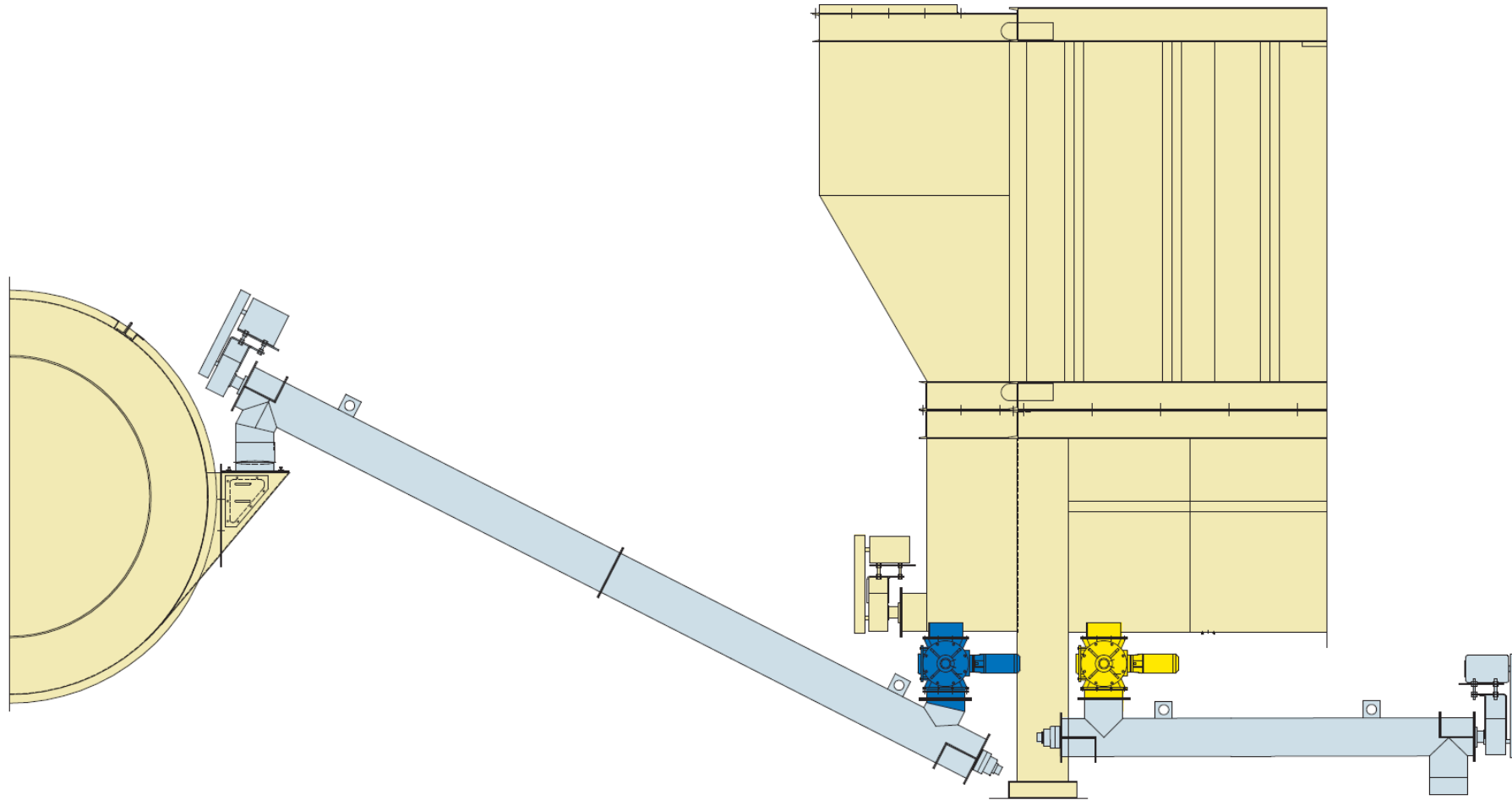
- Amount of dust moved to silo is unknown
- Amount of dust to return is trial and error
- AC flow rate is trial and error
- Since the fine dust is not metered as it leaves the baghouse, required change of AC flow is unknown

## Note:

- Most common dust control system
- Balances control, cost, and reliability



# Option 3 – Split Return



# Option 3 – Split Return

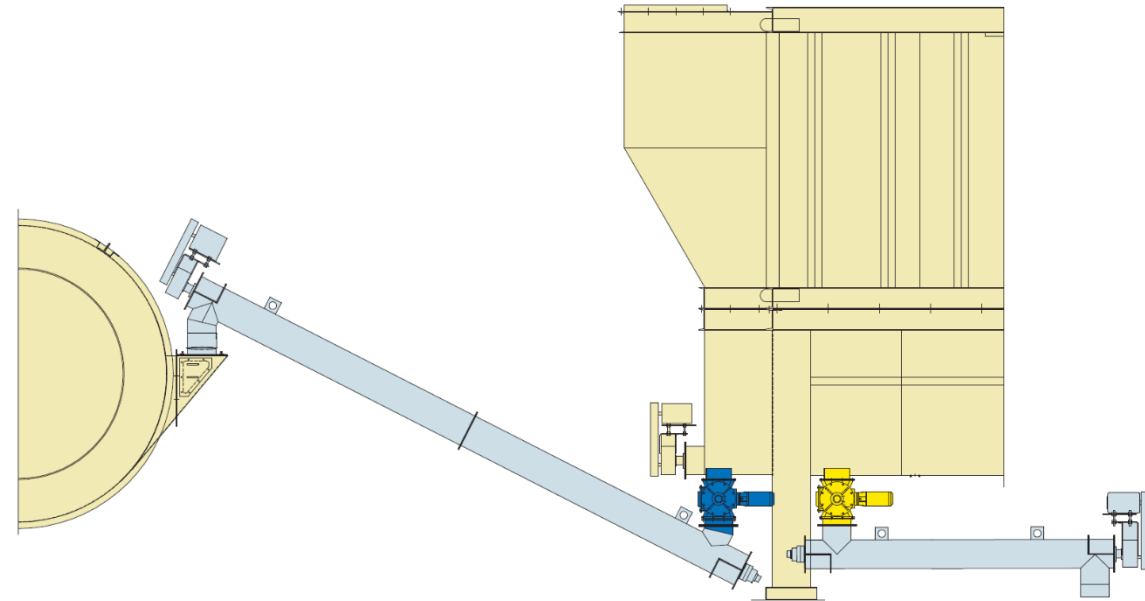


## Advantages

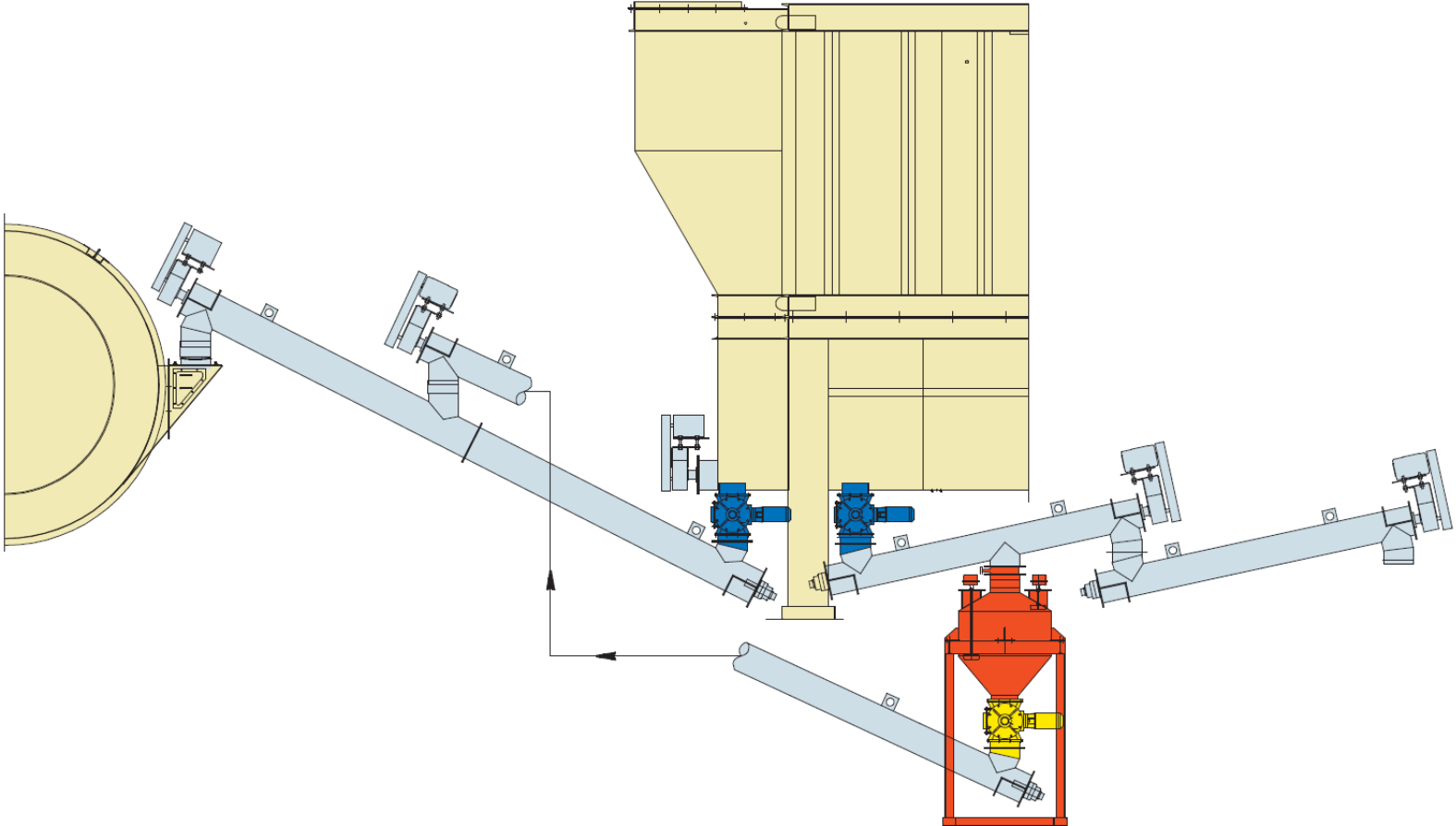
- Allows for wasting of dust if aggregate blend cannot meet spec

## Disadvantages

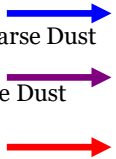
- Amount of dust to waste is trial and error
- AC flow rate is trial and error
- Since the fine dust is not metered as it leaves the baghouse, required change of AC flow is unknown



# Option 4 – Split Return with Surge Pot



- Coarse/Fine Dust Combined
- Coarse Dust
- Fine Dust



# Option 4 – Split Return with Surge Pot

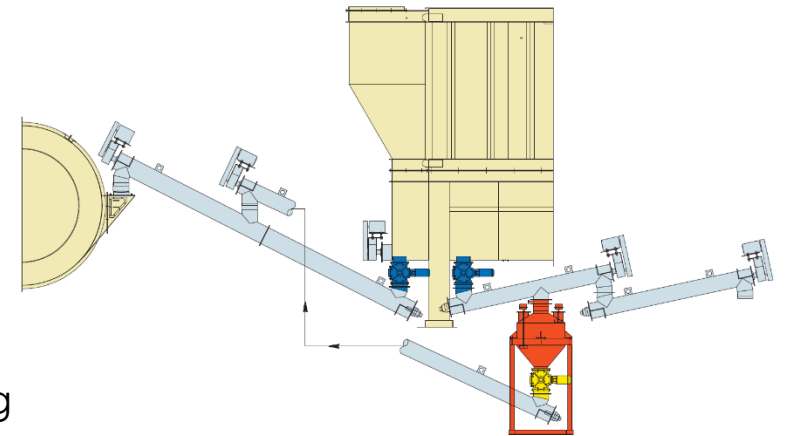


## Advantages

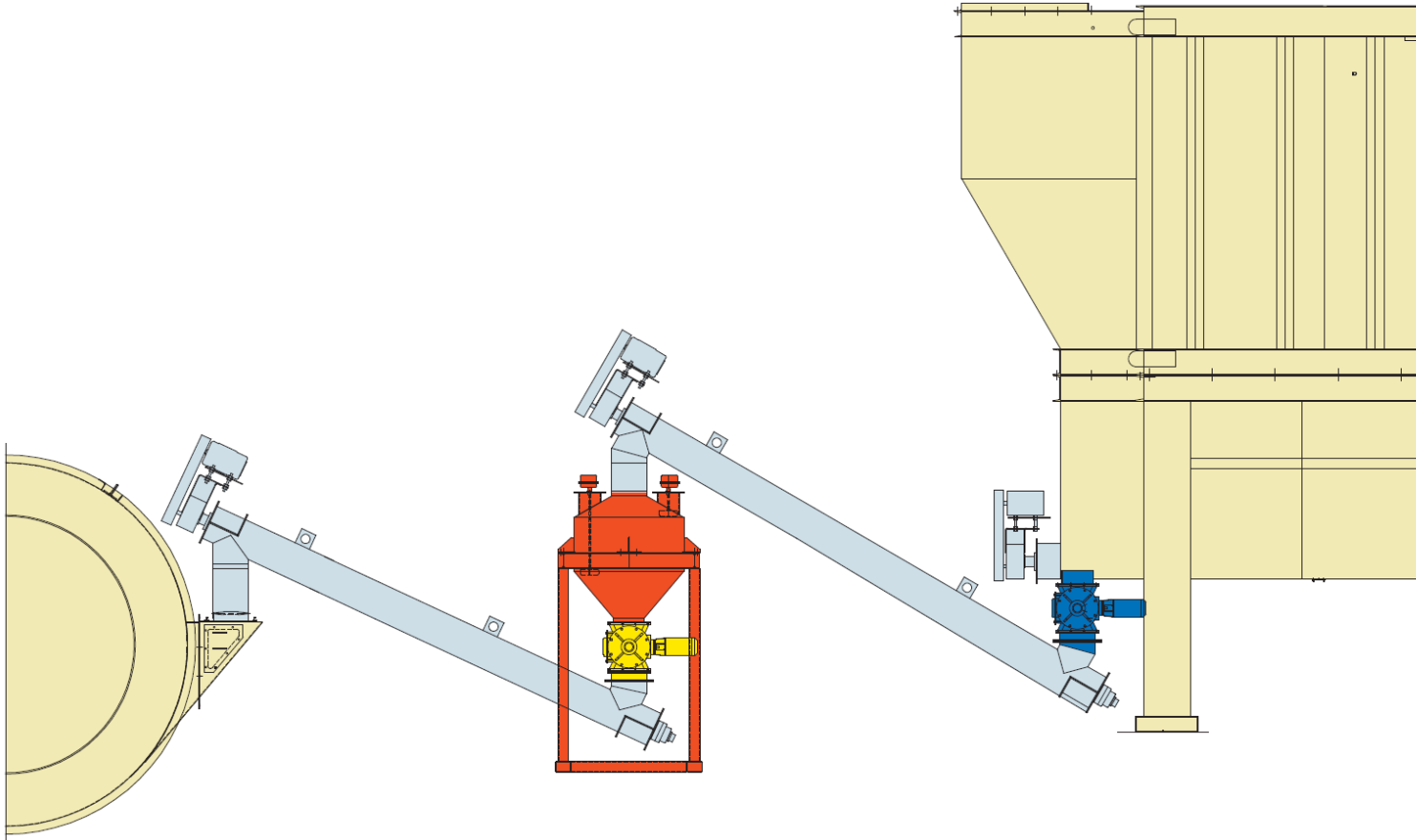
- Allows for wasting of dust if aggregate blend cannot meet spec
- Ensures steady dust flow from baghouse at start up and mix design transitions

## Disadvantages

- Amount of dust to waste is trial and error
- Cannot add dust without additional mineral feed system
- AC flow rate is trial and error
- Since the fine dust is not metered as it leaves the baghouse, required change of AC flow is unknown



# Option 5 – Return All with Surge Pot



# Option 5 – Return All with Weigh Pot

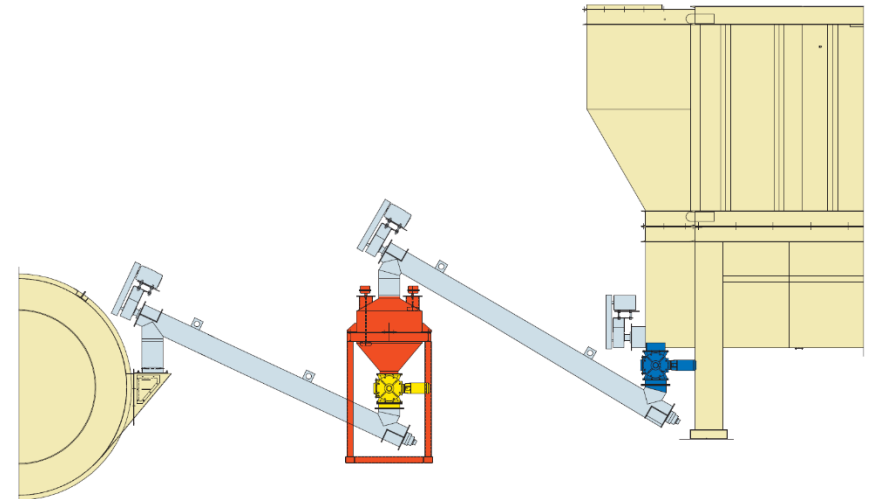


## Advantages

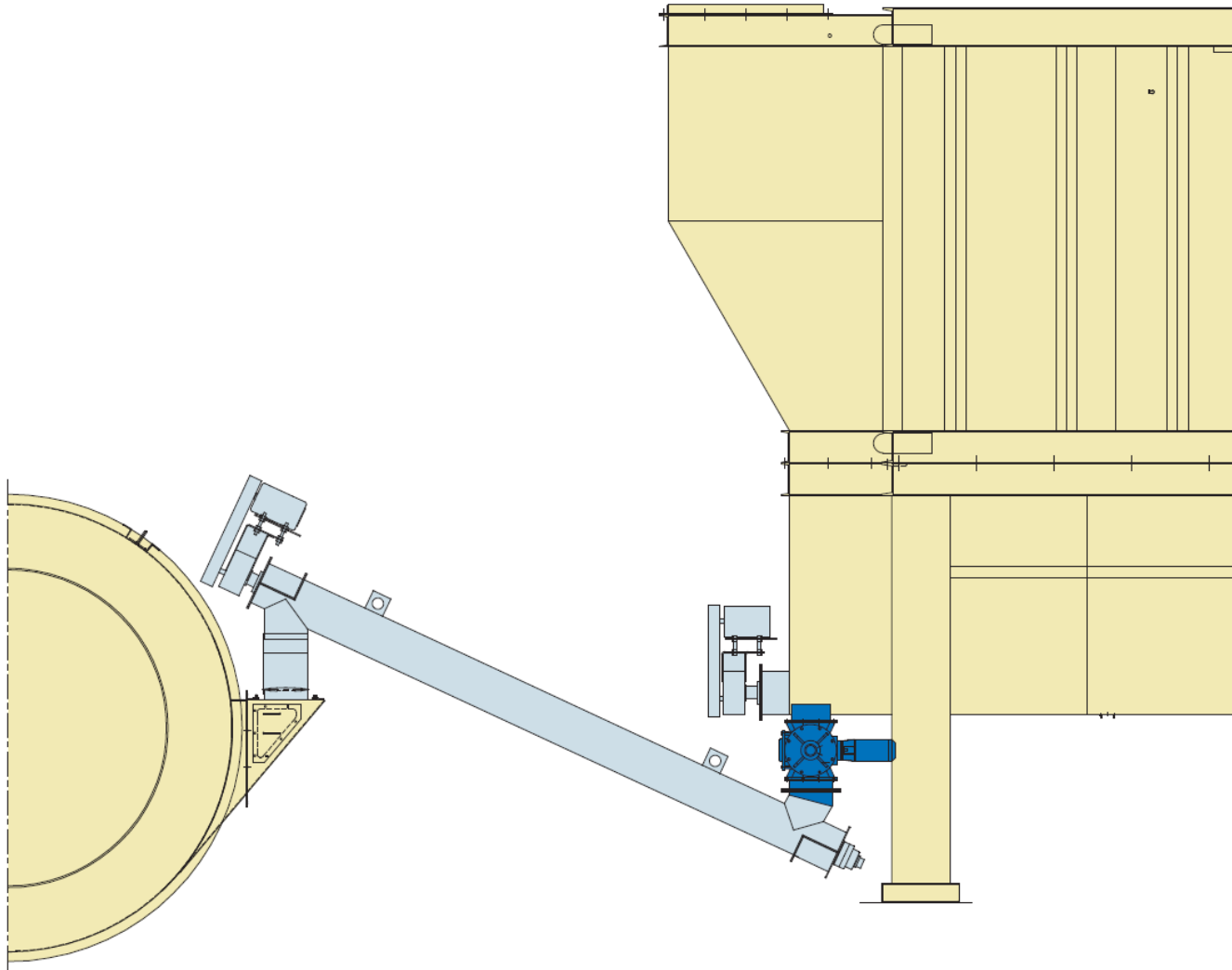
- Ensures steady dust flow from baghouse at start up and mix design transitions
- Relatively low cost

## Disadvantages

- Does not control dust in mix beyond Cold Feed Blending controls
- Surge pot control



# Option 6 – Return All



# Option 6 – Return All

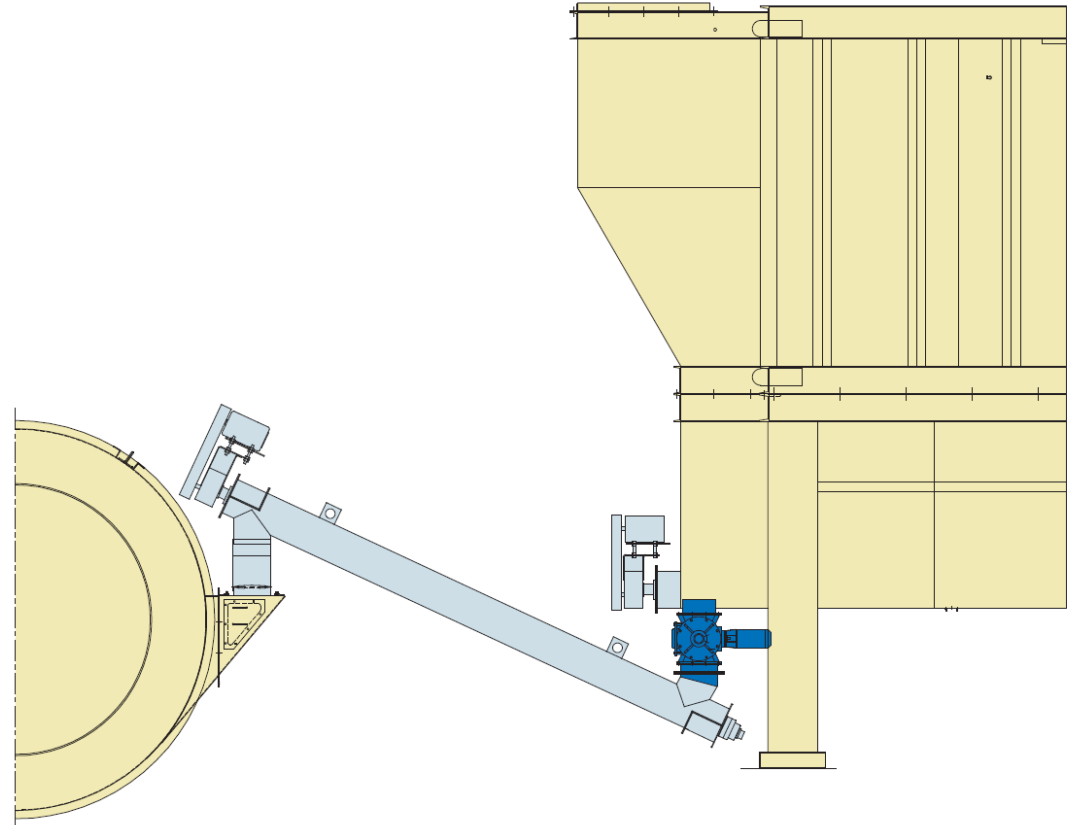


## Advantages

- Lowest cost

## Disadvantages

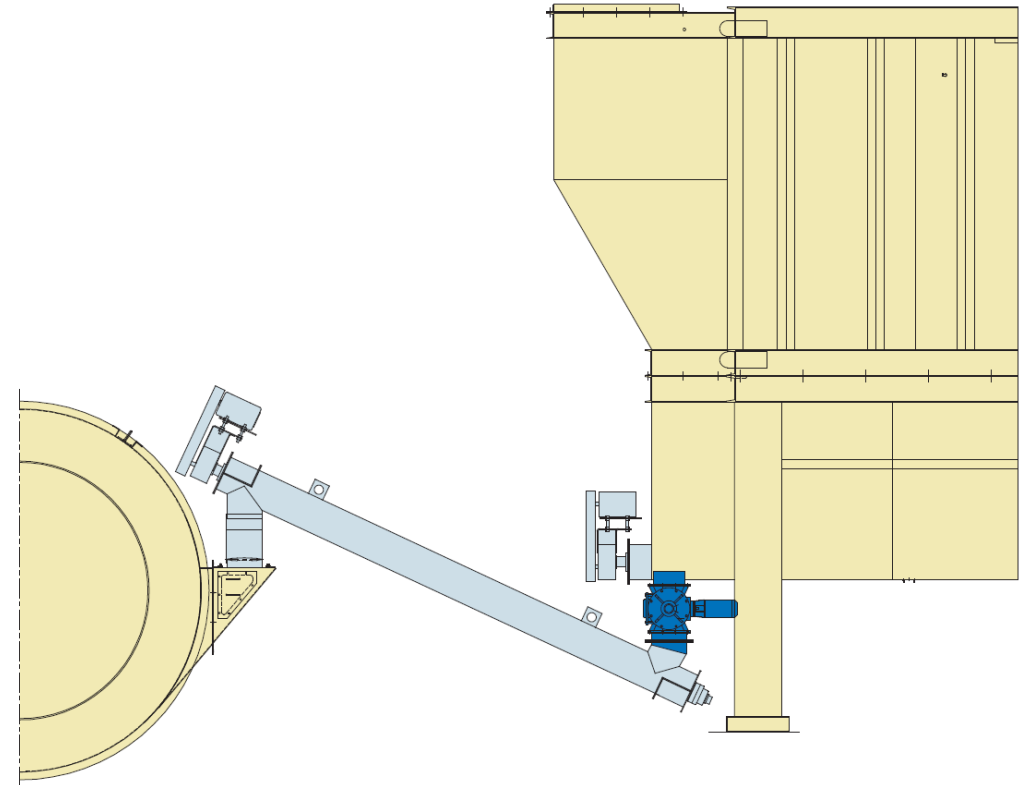
- Does not control dust in mix beyond CFB controls
- All dust collected will be returned to mix
- Cannot waste dust



# Additional discussion topics



- The dryer – exhaust system is not a classifier
- How much dust exits the drum can vary greatly
- Dust creation in the drum (1% to 4%)
- Does a mixer create dust?
- What about start-up dust flow?
- What about shut-down dust?
- How long to steady state?





Questions?